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EST



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Negative CO₂ Emissions in the Lime Production Using an Indirectly Heated Carbonate Looping Process

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300 kW_{th} IHCaL pilot
plant and corrosion
testing facility

Laboratory and
mechanic workshop

1 MW_{th} Pilot plant for
testing of CO₂-capture
und gasification

Gas cleaning pilot
plant

Fuel and chemicals
synthesis facility



Agenda



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1 Motivation

2 Indirectly Heated Carbonate Looping

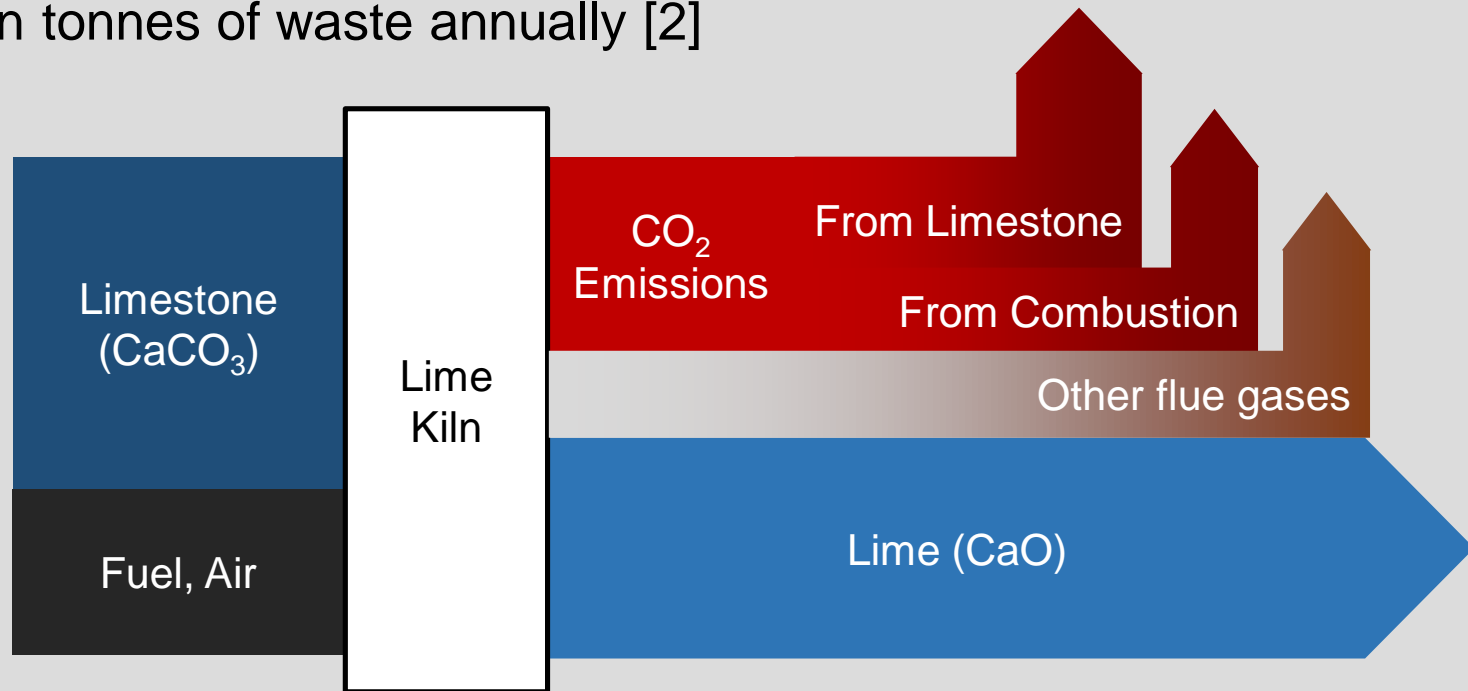
3 Methodology

4 Results

5 Summary and Outlook

1 Motivation

- 50 million tonnes CO₂ annually [1]
- 2 billion tonnes of waste annually [2]



*Mass flow diagram with data from [1]

[1] Schorcht et al. *BAT Reference Document for the Production of Cement, Lime and Magnesium Oxide* (2016)

[2] Kaza et al. *What a waste 2.0*. (2018)

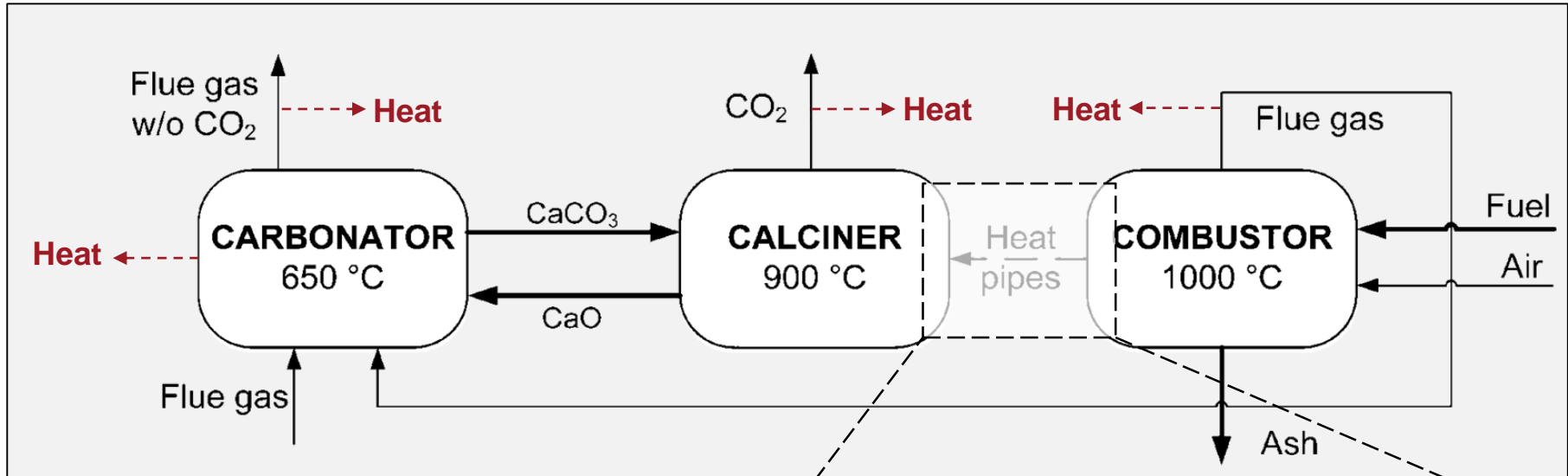
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The IHCaL Process

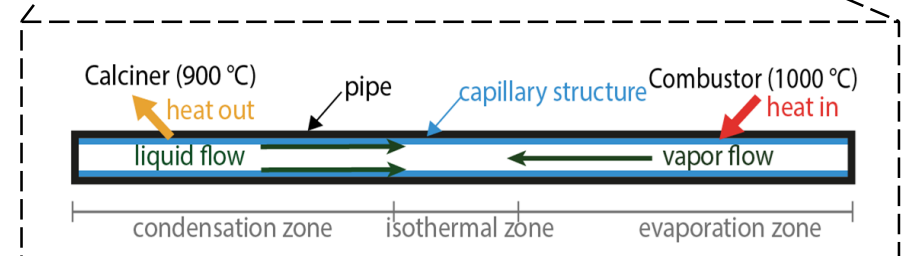
Indirectly Heated Carbonate Looping



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- Technology validated up to 0.3 MW_{th}
- Longer sorbent life
- High efficiency
- Reduced cost - no need of pure O₂
 - Oxy-fired CaL: 26.8 €/t CO₂ [3]
 - Indirectly heated CaL: 22.6 €/t CO₂ [4]



[3] Lyngfelt and Leckner, A 1000 MW_{th} Chemical-Looping Combustor for solid fuels – discussion of design and costs (2014)

[4] Junk et al., *Technical and economical assessment of the indirectly heated carbonate looping process* (2015)

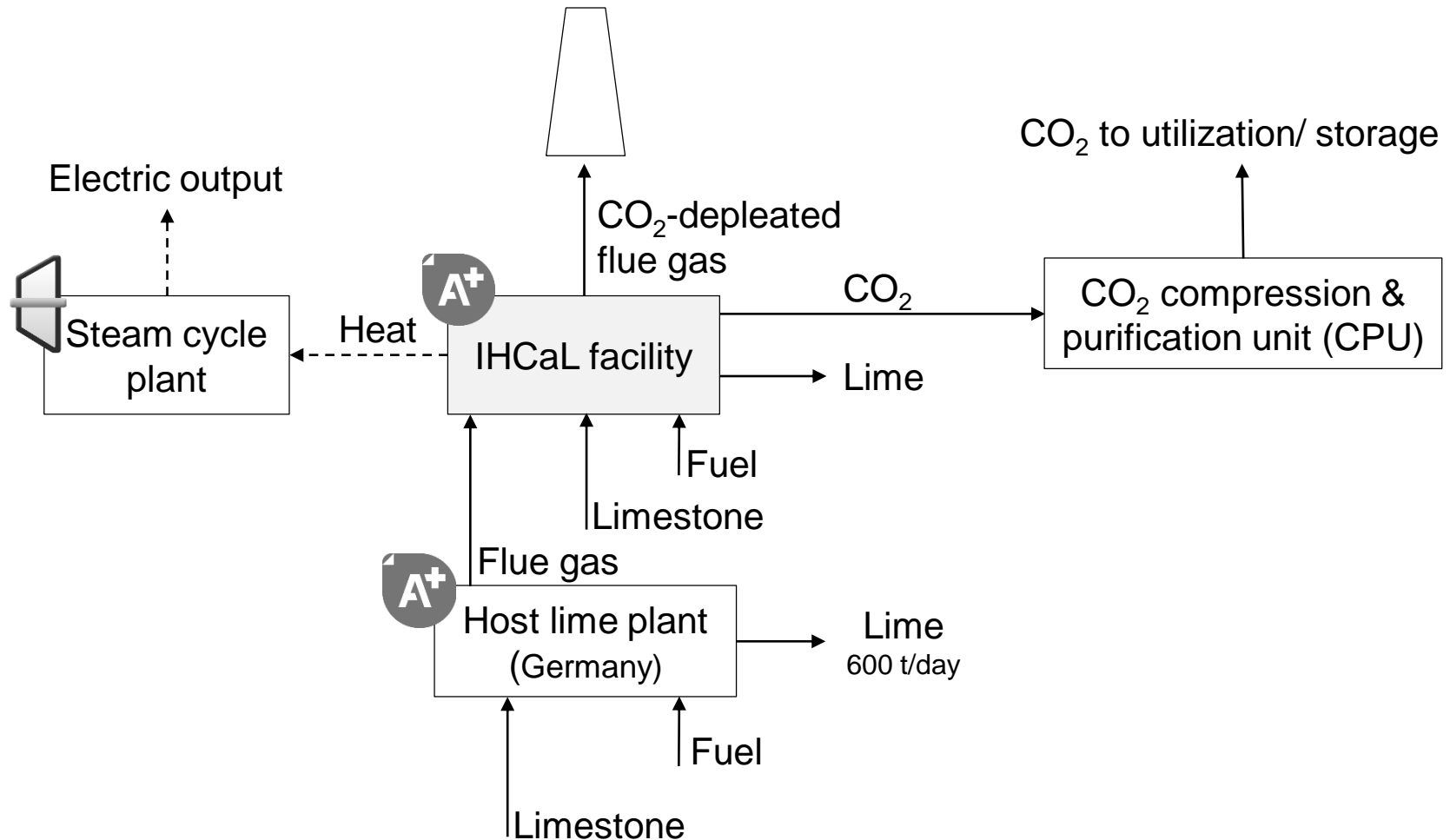
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Methodology

System Overview



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Dried Lignite

- $LHV_{wet} = 21.5 \text{ MJ/kg}$
- $96.7 \text{ gCO}_2/\text{MJ}_{LHV}$; $x_{bio} = 0\%$



Refuse-Derived Fuel (RDF) Pellets

- $LHV_{wet} = 19.6 \text{ MJ/kg}$
- $92.8 \text{ gCO}_2/\text{MJ}_{LHV}$; $x_{bio} = 51\%$
- Pilot testing



Solid Recovered Fuel (SRF)

- $LHV_{wet} = 15.7 \text{ MJ/kg}$; $x_{bio} = 65\%$
- $88.7 \text{ gCO}_2/\text{MJ}_{LHV}$



Municipal Solid Waste (MSW)

- $LHV_{wet} = 10.0 \text{ MJ/kg}$; $x_{bio} = 65\%$
- $106.0 \text{ gCO}_2/\text{MJ}_{LHV}$



IHCaL Key Performance Indicator

- Carbon capture efficiency:

$$E = \frac{F_{CO_2}^{captured}}{F_{CO_2}^{total}} = 90\%$$

Thermodynamic Key Performance Indicators

- Net direct CO₂ avoided: (influence of biogenic fraction)

$$AC_{net} = 1 - \frac{e_{CO_2} - e_{CO_2,capt,bio}}{e_{CO_2,ref}}$$

- Specific primary energy consumption per kg of CO₂ avoided (SPECCEA)

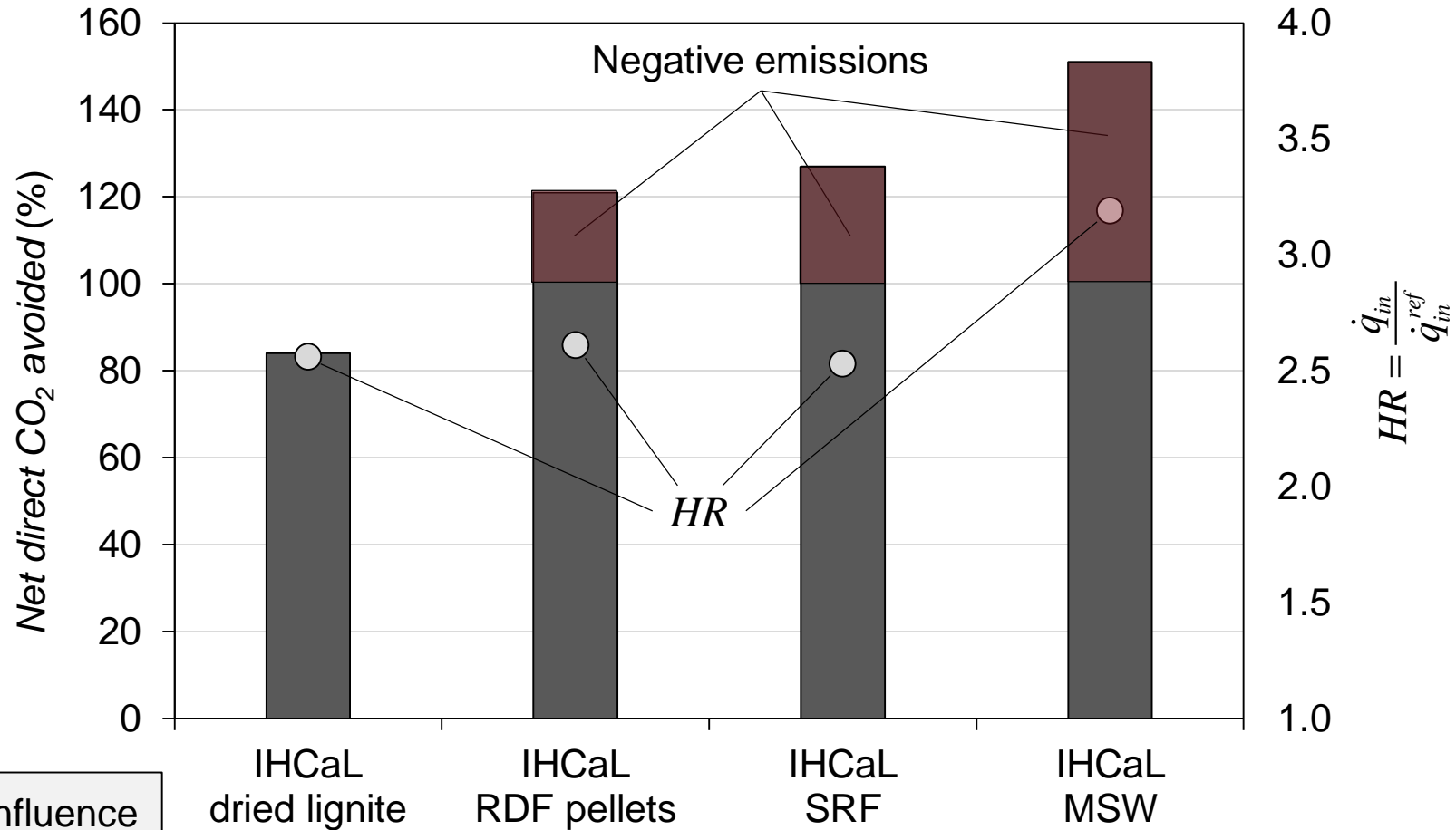
$$SPECCEA = \frac{q_{eq} - q_{eq,ref}}{e_{CO_2,ref} - e_{CO_2}}$$

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Results

Direct Fossil CO₂

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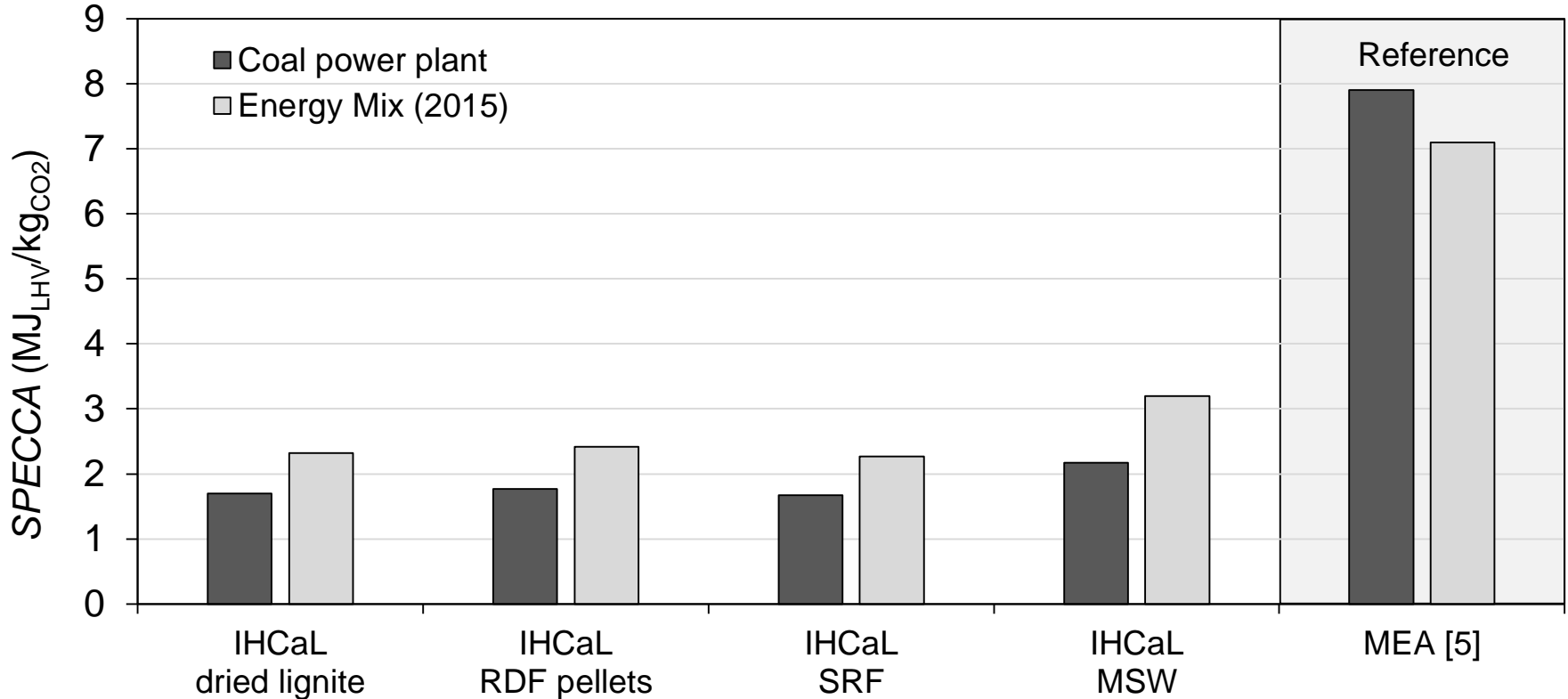
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Results

SPECCA



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Influenced
by P_{el}

[5] M. Voldsund et al. *D4.6 CEMCAP comparative techno-economic analysis of CO₂ capture in cement plants* (2019)

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Summary and Outlook



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- Potential for IHCaL
 - Negative emissions
 - Low SPECCA
 - Sorbent integration



Samples from the pilot testing at 300 kW_{th} scale. © EST Institute, TU Darmstadt.

- Pilot-testing ongoing [6]
 - Pilot (300 kW_{th}) & Long-term (≈ 15 days)
 - Real flue gas and circulation conditions
 - Different sorbents and fuels (SRF)

- Outlook
 - Plant size
 - CAPEX



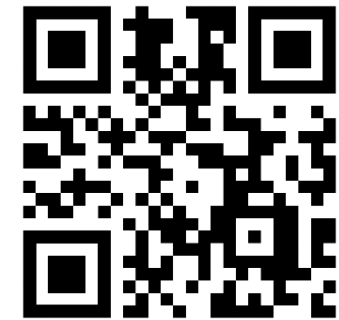
300 kW_{th} IHCaL pilot testing facility scale. © EST Institute, TU Darmstadt.

[6] C. Hofmann et al. *Adaption of a 300kW_{th} Pilot Plant for Testing the Indirectly Heated Carbonate Looping Process for CO₂ Capture from Lime and Cement Industry* (2022)

Acknowledgements



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<https://act-anica.eu/>

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Thank you for your attention!



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