

NUMERICAL ANALYSIS OF THERMAL DISTRIBUTIONS AND
LOCALIZED MELTING IN SOLIDS

BY

WILHELM UNKELBACH

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WILHELM UNKELBACH

APPROVED:

Thesis Committee:

Major Professor Prof. Dr. David G. Taggart
Apl. Prof. Dr. Sc. Tatiana Gambaryan-Roisman
Prof. Dr.-Ing. Peter Stephan

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ABSTRACT

Analytic solutions for heat transfer problems are limited to simple geometries and boundary conditions. This thesis aims to investigate numerical methods for solving transient heat transfer problems, with particular emphasis on problems involving localized heating that can lead to phase change. Such problems are of increasing importance in modelling additive manufacturing processes. Heat transfer is present in most engineering applications. Complex problems require numerical solutions which involve complex geometries, non-uniform boundary conditions and transient temperature history. For such problems, finite difference and finite element solution techniques have been developed. This thesis introduces the basic numerical models for finite difference and finite element calculations. Then the found calculation problems are employed to solve validation problems and generic heat transfer problems. A comparison is drawn to commercial code, namely Abaqus. Finally, melting and freezing processes are modelled and evaluated.

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Numerical Analysis of Thermal Distributions and Localized Melting in Solids

Numerische Analyse von Temperaturverteilungen und
lokalem Schmelzverhalten in Feststoffen



TECHNISCHE
UNIVERSITÄT
DARMSTADT

Master-Thesis of Wilhelm Unkelbach (matriculation number: 2819914)
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Analytic solutions for heat transfer problems are limited to simple geometries and boundary conditions. Thermal analysis of complex geometries requires solution by numerical methods. This requires the investigation of numerical methods for solving transient heat transfer problems, with particular emphasis on problems involving localized heating that can lead to phase change. Such problems are of increasing importance in modelling additive manufacturing processes. Recent developments in the field of additive manufacturing, in which filaments are heated in extruders and deposited in controlled patterns or powders are melted by controlled motion of a moving heat sources, lead to complex heat transfer problems. Such problems require numerical solutions which involve complex geometries, non-uniform boundary conditions and transient temperature history. For such problems, finite difference and finite element solution techniques have been developed.

Heat transfer analysis of porous material or metal powders are complicated since the high surface area per volume leads to high heat transfer rates. Initial investigation will consider traditional heat transfer problems using Matlab and Abaqus, a commercial finite element code. Cases to be considered include 1- and 2-dimensional solid body problems with given boundary conditions. The generic problems can also include heat sources and convection. After successfully achieving realistic temperature distributions and validating the solution accuracy, the problems will incorporate either stresses or liquid elements.

task outline:

- Literature research
- Calculation of generic problems using Matlab and Abaqus
- Incorporation of phase change or stresses
- Evaluation of the simulations
- Validation using different code or experiments
- Written documentation

Apl. Prof. Dr. Sc. Tatiana Gambaryan-Roisman

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CHAPTER 1

Motivation

Heat transfer is present in most engineering applications and its investigation ranges from household appliances to combustion engines to large-scale thermal power plants. Recent developments in the field of additive manufacturing, in which filaments are heated in extruders and deposited in controlled patterns or powders are melted by controlled motion of a moving heat sources, lead to complex heat transfer problems. Such problems require numerical solutions which involve complex geometries, non-uniform boundary conditions and transient temperature histories. For such complex problems, numerical finite difference and finite element solution techniques can be applied. Many of these techniques have been incorporated into commercial software packages. Melting represents a phase change which involves absorption of energy, volumetric expansion and change in material properties. Energy absorption affects the temperature distribution and thermal expansion can induce stresses and therefore can cause deformation and possible damage. Melting can be modeled through the use of a potential function [5]. The field variables for modeling melting can also be modeled via subroutines in the commercial finite element code, Abaqus. For example Yaakoubi et al. developed an Abaqus USDFLD user subroutine for modeling melting of iron [6]. Heat transfer analysis of porous materials or metal powders are complicated since the high surface area per volume leads to high heat transfer rates [7]. Clearly, the complexity of these problems requires the development of appropriate numerical modeling techniques.

Before discussing details of this investigation, some fundamentals of heat transfer shall be reviewed. Heat conduction is governed by the general heat conduction equation.

$$\frac{dT}{dt} - \alpha \Delta T = \frac{dQ/dt}{\rho c_p} \quad (1)$$

where T is temperature, t the time, Q the heat generated within the solid, c_p the material's specific heat capacity at constant pressure, ρ its density, and α its thermal diffusivity [8]. The thermal diffusivity equals $\frac{k}{\rho c_p}$ where k is the thermal conductivity. Free and forced convection can be included using Newton's Law of cooling

$$q_h = h (T - T_\infty) \quad (2)$$

with the convection coefficient h . The term q_h is added on the right-hand side of Eq. 1. In finite element formulations, solving the heat conduction equation numerically is similar to solving stress-displacement problems [3].

In this thesis, numerical methods for 1-dimensional heat transfer problems will be developed and solved in Matlab, with validation by comparing to analytical solutions and/or solutions obtained using Abaqus, a commercial finite element code. For 2-dimensional problems, solutions will be found using Abaqus. In some cases, the boundary conditions are Dirichlet problems [6], i. e. the surface temperature is explicitly given by a function of time (and location). The generic problems can also include heat sources and convection (Neumann problems). After successfully achieving realistic temperature distributions, the solution accuracy shall be validated.

In order to compute the numerical solution to stress-strain problems and heat transfer in rigid bodies, the underlying equations shall briefly be introduced. Forces acting on a deformable body can be calculated using a global stiffness matrix which essentially models the body as a multitude of nodes connected by effective elastic springs [3]. The individual element stiffnesses are assembled to define the global stiffness matrix. Eq. 3 shows the relationship between the global force vector \tilde{F} ,

the global stiffness matrix \tilde{K} and the displacement vector d .

$$\vec{F} = \tilde{K} \vec{d}. \quad (3)$$

Heat transfer problems can be modelled very similarly. The global conduction matrix K replaces the global stiffness matrix and displacements are replaced by nodal temperatures, T . The global force vector, F , includes specified heat flux and/or convection at the surface. Therefore, the global equation for heat conduction and convection becomes

$$\vec{F} = K \vec{T}. \quad (4)$$

In order to numerically solve Eqs. 3 and 4, displacement or temperature interpolation functions, typically polynomials of linear or quadratic order, are used. For heat transfer problems, the relationship between heat flux and temperature gradients, analogous to strain and displacements relations, are defined. The conduction and convection matrices are calculated for each element. This step is analogous to the forces and displacements of each element that are calculated in case of a stress-strain problem. After formulating these equations for each discretized element, the global equations are assembled and boundary conditions are imposed. Finally, this system of global equations is solved for the nodal temperatures which yields the temperature gradients and therefore the heat flux. This step is analogous to the case of stress-strain problems, where the global equations yield the displacement of each node, which can then be used to calculate the strains and stresses. These procedures are detailed for both stress analysis and heat transfer problems in the text by Logan [3].

CHAPTER 2

Derivation of finite difference calculation schemes

2.1 Finite difference in Cartesian coordinates

The finite difference method is commonly used to solve the heat conduction equation numerically. The governing equation is simplified using a difference quotient instead of the derivative. Starting with the heat conduction equation:

$$\alpha \nabla^2 T = \dot{T}. \quad (5)$$

where α is the thermal diffusivity ($k/(\rho c_p)$), ∇^2 is the Laplacian operator, T is temperature, and \dot{T} is $\frac{dT}{dt}$. In Cartesian coordinates, Eq. 5 becomes

$$\alpha \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) = \frac{dT}{dt}. \quad (6)$$

In the 1-dimensional case, this simplifies to

$$\alpha \frac{\partial^2 T}{\partial x^2} = \frac{dT}{dt}. \quad (7)$$

The difference quotients can be approximated in order to calculate the partial derivatives numerically as follows

$$\frac{\partial T}{\partial x} \approx \frac{T(x + \Delta x, t) - T(x, t)}{\Delta x} \quad (8)$$

and

$$\frac{dT}{dt} \approx \frac{T(x, t + \Delta t) - T(x, t)}{\Delta t}. \quad (9)$$

In order to approximate the second derivative of Eq. (7) a central differencing scheme is used. The difference quotient can also be obtained by using the same structure as in Eq. (8) for $\partial T/\partial x$. This yields

$$\frac{\partial^2 T}{\partial x^2} \approx \frac{T(x + \Delta x, t) - 2T(x, t) + T(x - \Delta x, t)}{\Delta x^2}. \quad (10)$$

Now the spatial coordinate x shall be denoted x_i and the temporal coordinate t_j respectively. The next spatial step is $x_{i+1} = x + \Delta x$ and the time-step analogously $t_{j+1} = t + \Delta t$. Eq. (7) can be discretized in a more compact form as

$$\frac{T(x_i, t_{j+1}) - T(x_i, t_j)}{\Delta t} = \alpha \left(\frac{T(x_{i+1}, t_j) - 2T(x_i, t_j) + T(x_{i-1}, t_j)}{\Delta x^2} \right) \quad (11)$$

By introducing the variable $X_{i,j}$ for $T(x_i, t_j)$ this can be further condensed

$$\frac{X_{i,j+1} - X_{i,j}}{\Delta t} = \alpha \left(\frac{X_{i+1,j} - 2X_{i,j} + X_{i-1,j}}{\Delta x^2} \right) \quad (12)$$

Solving for the next time step yields

$$X_{i,j+1} = \alpha \Delta t \left(\frac{X_{i+1,j} - 2X_{i,j} + X_{i-1,j}}{\Delta x^2} \right) + X_{i,j} \quad (13)$$

This scheme can be applied iteratively to calculate the temperature for each consecutive time step. A code example for a later discussed problem is attached in Appendix A.

2.2 Finite difference in spherical coordinates

The same procedure as in the previous section can be employed to simplify heat conduction problems in spherical coordinates. This is helpful for problems with spherical symmetry (e.g. a heat source in the center of a solid mass). The heat conduction equation (Eq. 5) can be expressed in spherical coordinates as

$$\frac{\alpha}{r^2} \left(\frac{\partial}{\partial r} \left(r^2 \frac{\partial T}{\partial r} \right) \right) + \frac{1}{\sin(\varphi)} \frac{\partial}{\partial \varphi} \left(\sin(\varphi) \frac{\partial T}{\partial \varphi} \right) + \frac{1}{\sin^2(\varphi)} \frac{\partial^2 T}{\partial \vartheta^2} = \frac{dT}{dt} \quad (14)$$

which, for spherically symmetric problems, reduces to

$$\frac{\alpha}{r^2} \left(\frac{\partial}{\partial r} \left(r^2 \frac{\partial T}{\partial r} \right) \right) = \frac{dT}{dt} \quad (15)$$

using the identities $\frac{\partial}{\partial \varphi} = \frac{\partial}{\partial \vartheta} = 0$. This assumption means that there is no temperature dependence on coordinates φ and ϑ . Using the product rule, Eq. (15) can be discretized as

$$\alpha \left(\frac{2}{r} \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial r^2} \right) = \frac{dT}{dt} \quad (16)$$

The difference quotients can be formulated in order to calculate the partial derivatives numerically as follows

$$\frac{\partial T}{\partial r} \approx \frac{T(r + \Delta r, t) - T(r, t)}{\Delta r} \quad (17)$$

and

$$\frac{dT}{dt} \approx \frac{T(r, t + \Delta t) - T(r, t)}{\Delta t} \quad (18)$$

In order to approximate the second derivative of Eq. (16) a central differencing scheme is used. The difference quotient can also be obtained by using the same structure as in Eq. (17) for $\partial T/\partial r$. This yields

$$\frac{\partial^2 T}{\partial r^2} \approx \frac{T(r + \Delta r, t) - 2T(r, t) + T(r - \Delta r, t)}{\Delta r^2} \quad (19)$$

Now the spatial coordinate r shall be denoted r_i and the temporal coordinate t_j respectively. The next spatial step is $r_{i+1} = r + \Delta r$ and the time-step analogously $t_{j+1} = t + \Delta t$. Eq. (16) can be discretized in a more compact form as

$$\alpha \left(\frac{2}{r_i} \frac{T(r_{i+1}, t_j) - T(r_i, t_j)}{\Delta r} + \frac{T(r_{i+1}, t_j) - 2T(r_i, t_j) + T(r_{i-1}, t_j)}{\Delta r^2} \right) = \frac{T(r_i, t_{j+1}) - T(r_i, t_j)}{\Delta t} \quad (20)$$

By introducing the variable $X_{i,j}$ for $T(r_i, t_j)$ this can be further reduced to

$$\frac{X_{i,j+1} - X_{i,j}}{\Delta t} = \alpha \left(\frac{2}{r_i} \frac{X_{i+1,j} - X_{i,j}}{\Delta r} + \frac{X_{i+1,j} - 2X_{i,j} + X_{i-1,j}}{\Delta r^2} \right) \quad (21)$$

Solving for the next time step yields

$$X_{i,j+1} = \alpha \Delta t \left(\frac{1}{r_i} \frac{X_{i+1,j} - X_{i,j}}{\Delta r} + \frac{X_{i+1,j} - 2X_{i,j} + X_{i-1,j}}{\Delta r^2} \right) + X_{i,j} \quad (22)$$

This is an analogous expression to Eq. 13. The only difference is the $1/r_i$ term which stems from the product rule (Eq. 16). This equation can be used to solve 1-dimensional heat transfer problems with spherical symmetry. A code example for a later discussed problem is attached in Appendix B.

CHAPTER 3

Finite element formulation

3.1 Introduction

The general form of the heat equation can be expressed as

$$\rho c_p \frac{\partial T}{\partial t} = \nabla \cdot (k \nabla T) + Q \quad (23)$$

where T is the temperature, t is the time, ρ is the density, c_p is the specific heat, k is the thermal conductivity and Q is the internal heat generation. In this chapter, 1-dimensional solutions are obtained in Cartesian, cylindrical and spherical coordinates, with spatial variables defined in Figure 1.

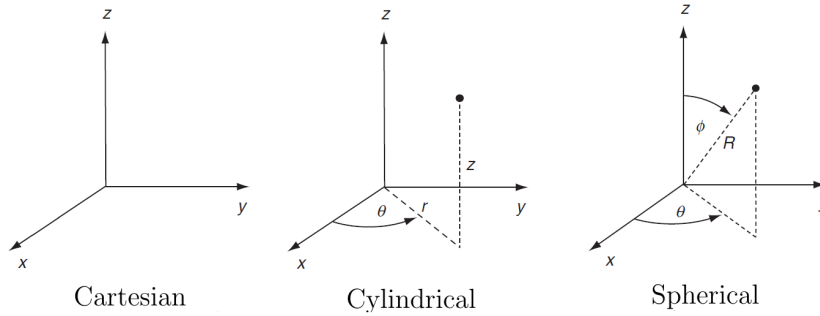


Figure 1: Cartesian, cylindrical and spherical coordinate systems (adapted from [1])

For the case of steady state heat conduction with no internal heat generation and temperature independent thermal conductivity, Eq. 23 reduces to Laplace's equation

$$\nabla^2 T = 0 \quad (24)$$

In Cartesian coordinates, if the spatial variation of temperature is limited to the x-direction, Laplace's equation becomes

$$\nabla^2 T = \frac{d^2 T}{dx^2} = 0 \quad (25)$$

In cylindrical coordinates, if the spatial variation of temperature is limited to the r-direction, Laplace's equation becomes

$$\nabla^2 T = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{dT}{dr} \right) = 0 \quad (26)$$

In spherical coordinates, if the spatial variation of temperature is limited to the R-direction, Laplace's equation becomes

$$\nabla^2 T = \frac{1}{R^2} \frac{\partial}{\partial R} \left(R^2 \frac{dT}{dR} \right) = 0 \quad (27)$$

3.2 Derivation of 1-dimensional equations

A brief derivation of application of Galerkin's method for developing 1-dimensional finite element equations is discussed below. Starting with Fourier's Law of Heat Conduction, which is defined as

$$q = -k \frac{dT}{dx} \quad (28)$$

where k is the thermal conductivity, q is the heat flux and T is the temperature, which is assumed to depend only on the spatial direction x , the energy balance on a control volume for steady conduction leads to

$$\frac{d}{dx} \left(k \frac{dT}{dx} \right) + Q = 0. \quad (29)$$

In the case of constant thermal conductivity and no heat sources or sinks, Eq. 29 can be further simplified to

$$k \frac{d^2 T}{dx^2} = 0. \quad (30)$$

In weighted residual methods (see Logan [3]), $\frac{d^2 T}{dx^2}$ is multiplied by a weighting function and integrated over the length of the element. In Galerkin's method, the weighting function is taken to be the finite element temperature interpolation functions, N_i as follows

$$\int_0^L k \left(\frac{d^2 T}{dx^2} \right) N_i(x) dx = 0 \quad (31)$$

where $i = 1, 2$, $N_1 = 1 - x/L$ and $N_2 = x/L$. This expression can be simplified by using integration by parts as follows

$$\int uv' = uv - \int u'v \quad (32)$$

where $u = N_i$, $u' = du/dx = dN_i/dx$, $v' = dv/dx = kd^2T/dx^2$ and $v = kdT/dx$. With these substitutions, Eq. 31 can be simplified as follows

$$\int_0^L k \left(\frac{d^2T}{dx^2} \right) N_i dx = N_i \left(\frac{dT}{dx} \right) \Big|_0^L - \int_0^L k \left(\frac{dT}{dx} \right) \left(\frac{dN_i}{dx} \right) dx = 0. \quad (33)$$

Using

$$T(x) = N_1(x)T_1 + N_2(x)T_2 \quad (34)$$

and

$$\frac{dT}{dx} = \frac{dN_1}{dx}T_1 + \frac{dN_2}{dx}T_2 = \begin{pmatrix} -1/L & 1/L \end{pmatrix} \begin{pmatrix} T_1 \\ T_2 \end{pmatrix} \quad (35)$$

Eq. 33 (for $i = 1$) can be simplified to

$$\int_0^L Ak \frac{dN_1}{dx} \frac{dT}{dx} dx = Ak \int_0^L (-1/2) \begin{pmatrix} -1/L & 1/L \end{pmatrix} \begin{pmatrix} T_1 \\ T_2 \end{pmatrix} dx = \frac{Ak}{L} \begin{pmatrix} 1 & -1 \end{pmatrix} \begin{pmatrix} T_1 \\ T_2 \end{pmatrix}. \quad (36)$$

Defining $f_{1x} = N_1 \left(\frac{dT}{dx} \right) \Big|_0^L$ gives the result

$$f_{1x} = \frac{Ak}{L} \begin{pmatrix} 1 & -1 \end{pmatrix} \begin{pmatrix} T_1 \\ T_2 \end{pmatrix}. \quad (37)$$

A similar expression for f_{2x} , defined as $N_2 \left(\frac{dT}{dx} \right) \Big|_0^L$, can be obtained, leading to element equations

$$K \vec{T} = \frac{Ak}{L} \begin{pmatrix} 1 & -1 \\ -1 & 1 \end{pmatrix} \begin{pmatrix} T_1 \\ T_2 \end{pmatrix} = \begin{pmatrix} f_{1x} \\ f_{2x} \end{pmatrix} = \vec{F} \quad (38)$$

where the 2x2 matrix on the left hand side that multiplies the nodal temperatures is the element conductivity matrix, K . This matrix is analogous to the element stiffness matrix in structural problems.

The global conductivity matrix can be assembled using element conductivity terms a_{ii} , a_{ij} , a_{ji} and a_{jj} for element i which lies between nodes i and j . In the case of a 1-dimensional model, the global conductivity matrix becomes a band matrix with entries on the diagonal of width 2. An example is presented in the next chapter to illustrate the finite element calculation for transient problems and is compared to a finite difference calculation for validation purposes.

In addition to 1-dimensional problems in Cartesian coordinates, it is of interest to develop a finite element formulation for 1-dimensional problems in cylindrical and spherical coordinates. In cylindrical coordinates, when the integrand depends only on the radial coordinate r , integration over the element volume is given by

$$\iiint_V f(r) dV = 2\pi h \int_{r_1}^{r_2} r f(r) dr \quad (39)$$

where r_1 and r_2 are the inner and outer radii of the element, respectively, and h is the element's height in z -direction. In spherical coordinates, when the integrand depends only on the radial coordinate R , integration over the element volume is given by

$$\iiint_V f(R) dV = 4\pi \int_{R_1}^{R_2} R^2 f(R) dR \quad (40)$$

where R_1 and R_2 are the inner and outer radii of the element, respectively.

For axisymmetric problems where the solution depends only on the radial coordinate r , Laplace's equation in cylindrical coordinates reduces Eq. 26. Analogously, for spherically symmetric problems where the solution depends only on the radial coordinate R , Laplace's equation reduces to Eq. 27. Applying Galerkin's method using these forms of Laplace's equations leads to the following element conductivity matrices. For 1-dimensional axisymmetric problems, the element conductivity matrix is given by

$$K = \frac{\pi k (r_1 + r_2) h}{L} \begin{bmatrix} 1 & -1 \\ -1 & 1 \end{bmatrix} \quad (41)$$

For spherically symmetric problems

$$K = \frac{4\pi k (R_1^2 + R_1 R_2 + R_2^2)}{3L} \begin{bmatrix} 1 & -1 \\ -1 & 1 \end{bmatrix} \quad (42)$$

Also, it should be noted here that in formulating transient problems, the term on the left hand side of Eq. 23 leads to definition of an element mass matrix. For 1-dimensional transient problems in Cartesian coordinates, the element mass matrix is given by (see Chapter 4 for derivation).

$$M = \frac{\rho c_p AL}{6} \begin{bmatrix} 2 & 1 \\ 1 & 2 \end{bmatrix} \quad (43)$$

For 1-dimensional axisymmetric problems M, is given by

$$M = 2\pi\rho c_p h \begin{bmatrix} \left(\frac{r_1}{4} + \frac{r_2}{12}\right) & \left(\frac{r_1}{12} + \frac{r_2}{12}\right) \\ \left(\frac{r_1}{12} + \frac{r_2}{12}\right) & \left(\frac{r_1}{12} + \frac{r_2}{4}\right) \end{bmatrix}. \quad (44)$$

For spherically symmetric problems

$$M = 4\pi\rho c_p \begin{bmatrix} \left(\frac{R_1^2}{5} + \frac{R_1 R_2}{10} + \frac{R_2^2}{30}\right) & \left(\frac{-3R_1^5 + 5R_1^4 R_2 - 5R_1 R_2^4 + \frac{3R_1^5}{5}}{60 (R_2 - R_1)^3}\right) \\ \left(\frac{-3R_1^5 + 5R_1^4 R_2 - 5R_1 R_2^4 + \frac{3R_1^5}{5}}{60 (R_2 - R_1)^3}\right) & \left(\frac{R_1^2}{30} + \frac{R_1 R_2}{10} + \frac{R_2^2}{5}\right) \end{bmatrix}. \quad (45)$$

3.3 Validation problems

To validate expressions derived in Section 3.2, a series of problems are considered where the 1-dimensional finite element solutions are compared to known exact solutions. In some cases, the exact solutions are based on analytic solutions. In other cases, the 1-dimensional solutions are compared to solutions obtained using the commercial general purpose code Abaqus. The 1-dimensional finite element equations are implemented in Matlab scripts given in the Appendices.

To validate the derived equations in Cartesian, cylindrical and spherical coordinates, three type of problems are considered. To validate the conductivity matrices, steady state conduction problems are solved and compared to known solutions. A mesh convergence study was performed for every Abaqus solution that

served as a validation for the used Matlab code. Here, the mesh size was refined until the solution converged. This ensured the mesh is adequately refined.

Figures 2 - 4 show that the finite element results match the known solutions for 1-dimensional Cartesian (Figure 2), cylindrical (Figure 3) and spherical (Figure 4) problems.

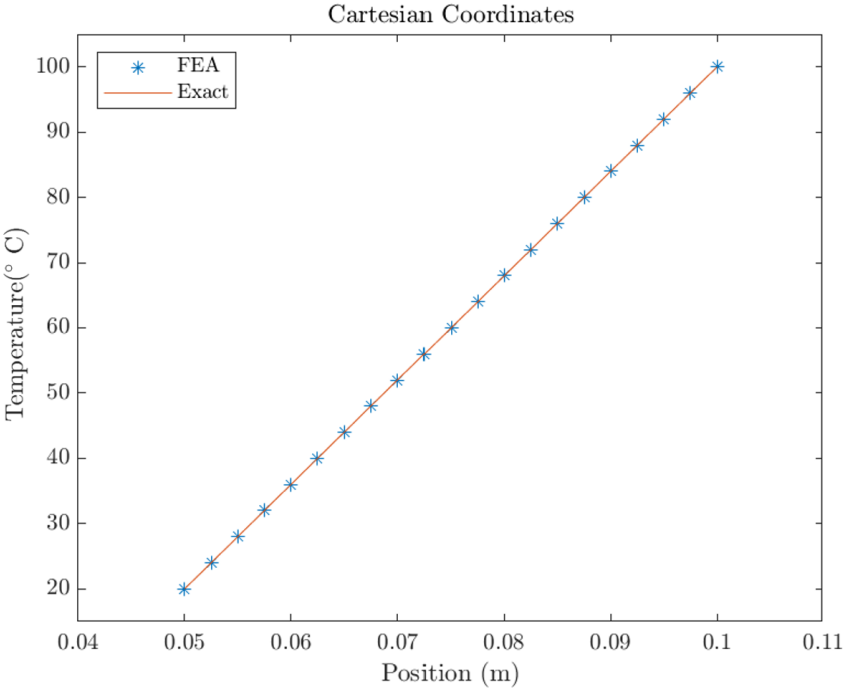


Figure 2: Cartesian Validation Case - Temperature Boundary Conditions

To validate transient problems involving convection boundary conditions, three additional problems are considered. To validate the Cartesian equations, the "Mill's" problem [2] discussed in Chapter 4 is considered. Results for this problem are shown in Figure 5. For the cylindrical formulation, a hollow cylinder is subjected to convection boundary conditions at the inner radius and is insulated at the outer radius. The temperature history at the inner and outer surfaces of the cylinder are shown in Figure 6. Evaluation of the spherically symmetric formula-

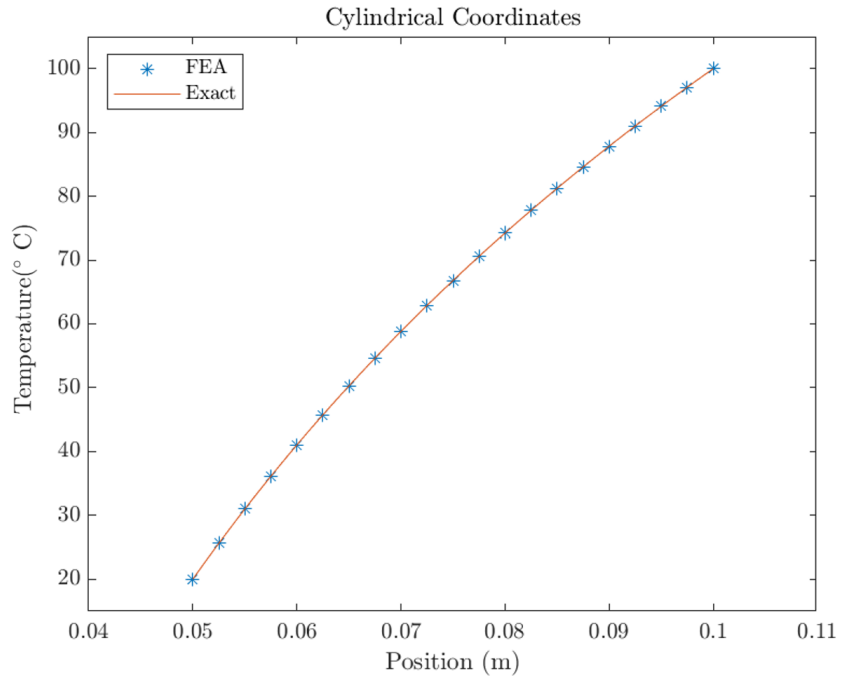


Figure 3: Cylindrical Validation Case - Temperature Boundary Conditions

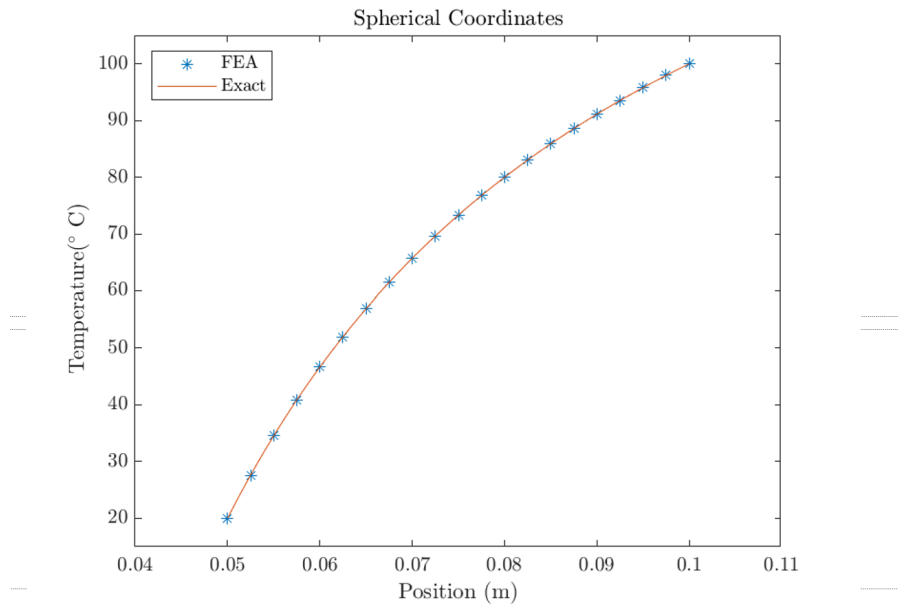


Figure 4: Spherical Validation Case - Temperature Boundary Conditions

tion is obtained using the "boiling egg" problem discussed in Chapter 5. Figure 7 shows that the center of the egg reaches 70 °C in 863 seconds, consistent with the known solution.

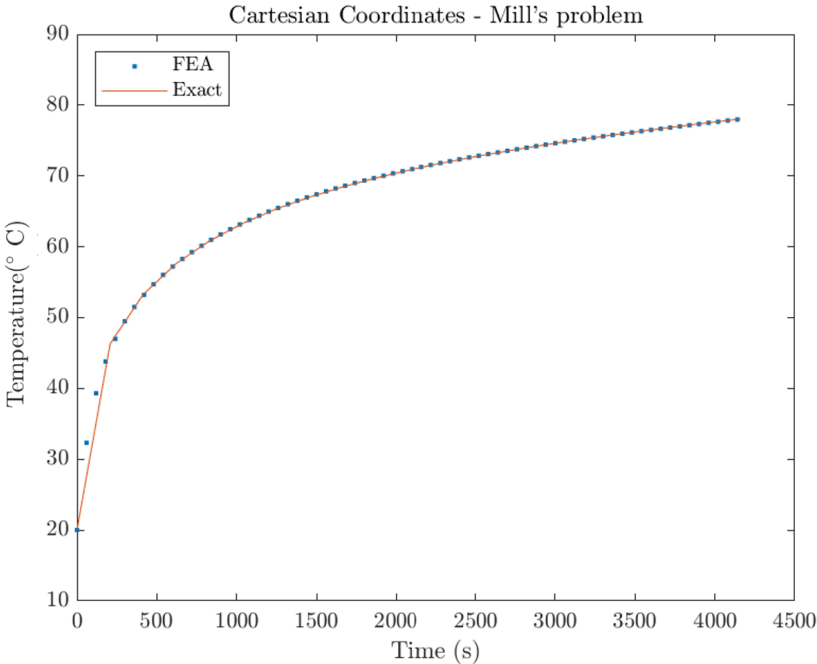


Figure 5: Cartesian Validation Case - Convection Boundary Conditions

To validate transient problems involving specified surface heat flux, three problems are considered. For Cartesian coordinates, the geometry and properties for examining melting of a PLA cylinder (see Chapter 6) are considered here, while ignoring the effects of latent heat of melting, which is considered in Chapter 6. Note that ignoring the effect of latent heat of melting results in unrealistically high temperatures. Despite being unrealistic, this case provides a problem that can be compared to a known solution. The results of this analysis are shown in Figure 8, where a temperature increase of over 3500 °C is observed in 2 seconds, in agreement with the known solution. For the cases of cylindrical and spherical coordinates, cases of a hollow cylinder and a hollow sphere are considered, with

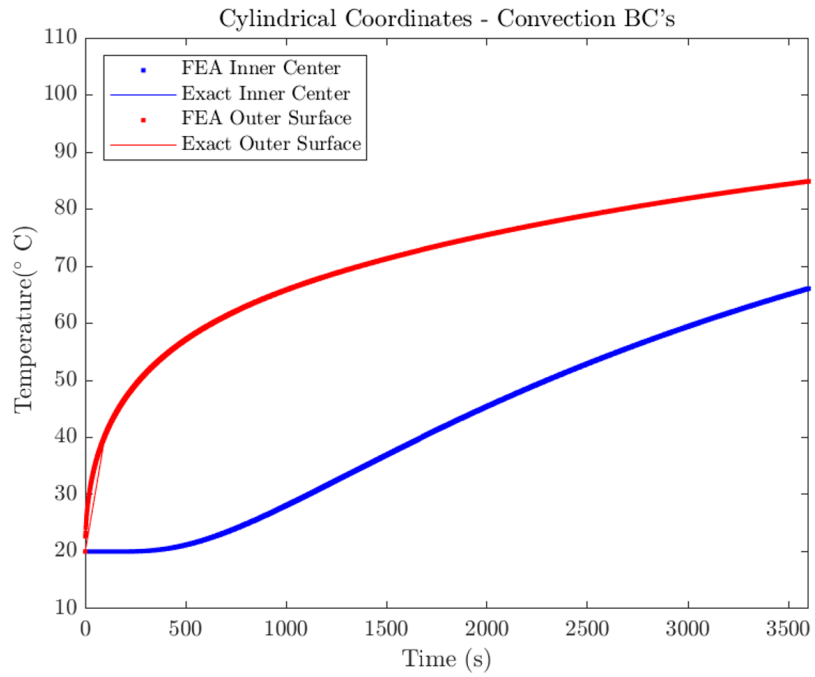


Figure 6: Cylindrical Validation Case - Convection Boundary Conditions

a specified heat flux at the inner radius and insulated boundary conditions at the outer radius. As shown in Figures 9 and 10, the temperature histories at the inner and outer radii match the known solutions.

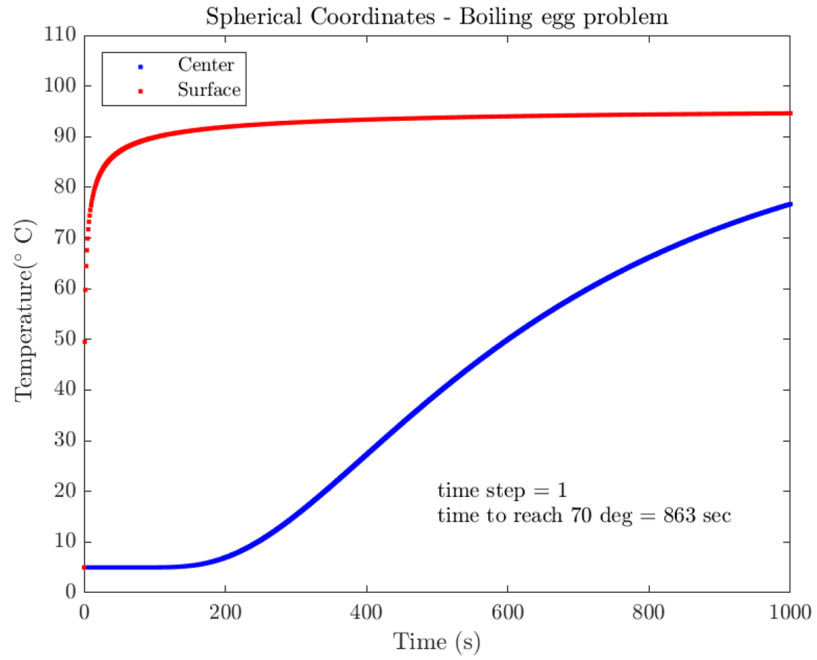


Figure 7: Spherical Validation Case - Convection Boundary Conditions

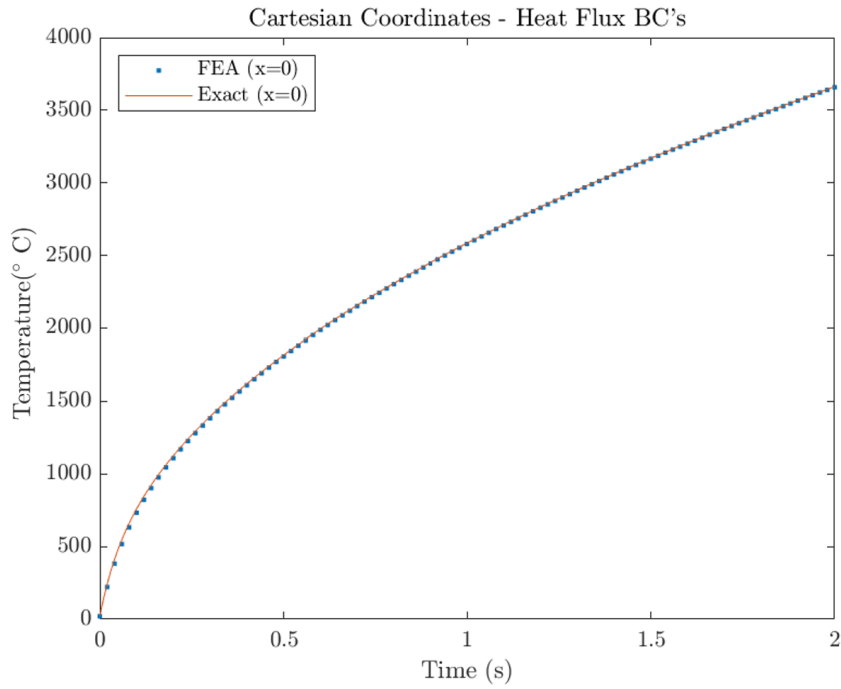


Figure 8: Cartesian Validation Case - Heat Flux Boundary Conditions

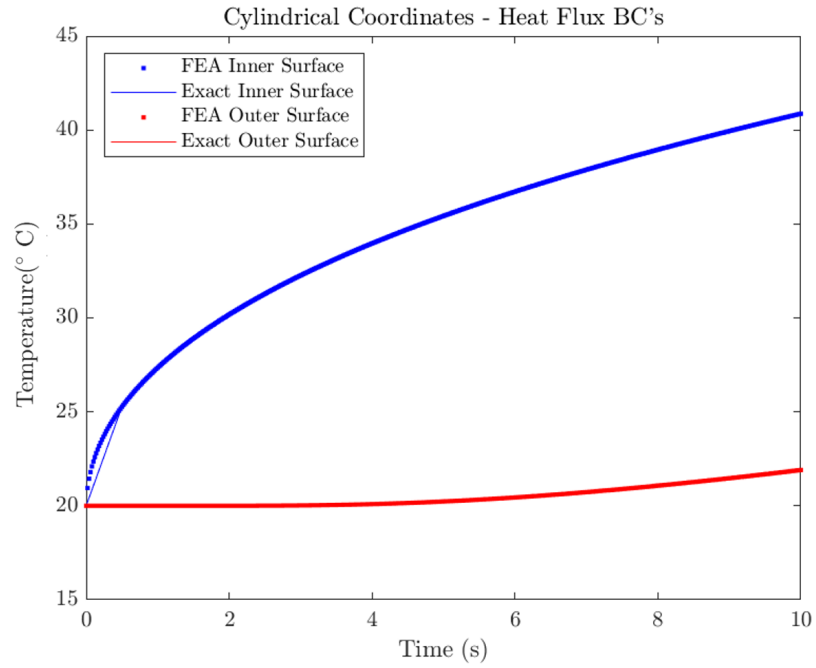


Figure 9: Cylindrical Validation Case - Heat Flux Boundary Conditions

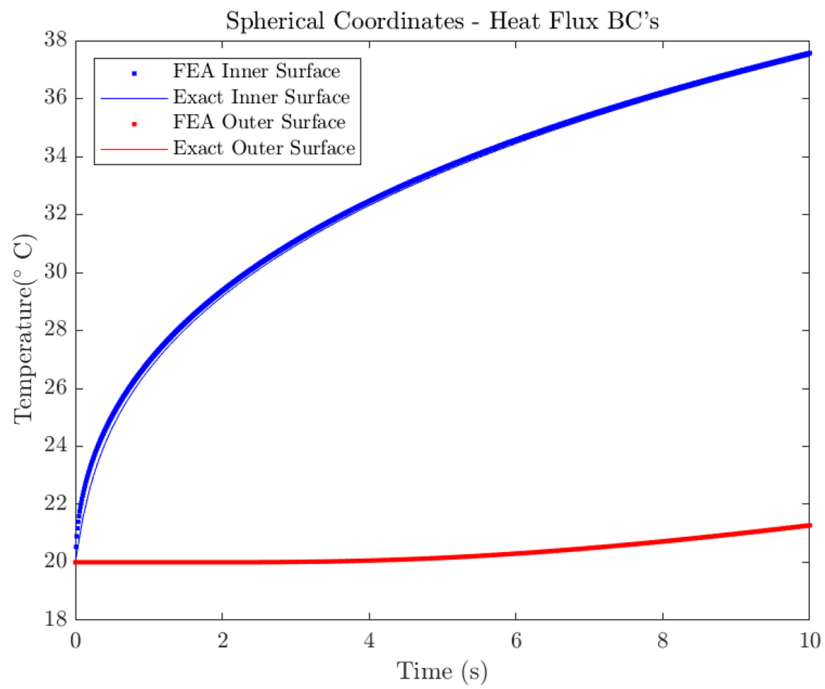


Figure 10: Spherical Validation Case - Heat Flux Boundary Conditions

CHAPTER 4

Convection boundary condition test case

A convective boundary finite difference calculation can be obtained by equating the internal increase in energy with the volumetric conduction as well as the convection across the boundary. The surrounding temperature T_∞ forms a heat sink for the internal temperatures at two consecutive nodes T^i and T^{i+1} . This leads to Eq. 46 [2]:

$$\rho c_p \frac{\Delta x}{2} (T_0^{i+1} - T_0^i) = k \frac{T_1^i - T_0^i}{\Delta x} \Delta t + h (T_\infty^i - T_0^i) \Delta t. \quad (46)$$

It is useful to non-dimensionalize Eq. 46 and solve for T_0^{i+1} similar to the procedure explained in the previous chapter:

$$T_0^{i+1} = 2Fo(T_1^i + BiT_\infty^i) + (1 - 2Fo - 2FoBi)T_0^{i+1} \quad (47)$$

where the Fourier number is defined as $Fo = \alpha \Delta t / \Delta x^2 = k \Delta t / c_p \rho \Delta x^2$ and the Biot number is defined as $Bi = h \Delta x / k$ [9]. This method has been implemented in the Matlab code shown in Appendix D and results are compared to finite element results below.

Alternatively, the finite element method can be adapted to include the temperature change vector \dot{T} . The structure of the following equation is similar to Eq. 38. For transient heat transfer problems the discretized energy balance is given by

$$K \vec{T} + M \dot{\vec{T}} = \vec{f}_Q + \vec{f}_q + \vec{f}_h \quad (48)$$

with the stiffness matrix K , mass capacitance matrix M , temperature vector T , temperature change vector \dot{T} and force vectors f_Q , f_q , f_h for internal heat sources, heat flux and convection, respectively. Considering the example of a slab of temperature T_0 which is heated by an air stream of temperature T_∞ , Eq. 48 simplifies

to

$$K\vec{T} + M\vec{T} = \vec{f}_h. \quad (49)$$

A visualization of a slab which is convectively heated is shown in Figure 11. The

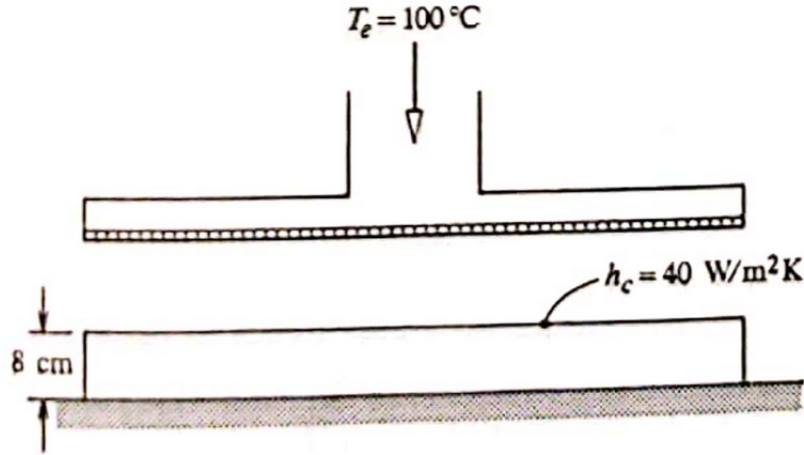


Figure 11: Convectively heated slab (adapted from [2])

stiffness matrix K can be calculated according to the derivation in Chapter 1 (See Eqs. 28 and following), where it is shown

$$K = \int_V B^T D B dV = Ak \int_0^L \begin{pmatrix} -1/L \\ 1/L \end{pmatrix} \begin{pmatrix} -1/L & 1/L \end{pmatrix} dx = \frac{Ak}{L} \begin{pmatrix} 1 & -1 \\ -1 & 1 \end{pmatrix}. \quad (50)$$

For the case of a convection boundary condition, the conductivity matrix K is modified due to the nature of Eq. 38. The convection coefficient h multiplies the temperature difference $\Delta T = T_\infty - T_{w(all)}$. In Eq. 38 the force vector F is on the right hand side and does not contain the temperature vector T . Therefore this equation is modified, so \vec{T} can be included on the left hand side of Eq. 38. The modified conductivity matrix K_h is defined as follows for a convection boundary condition acting on the first node:

$$K_h = K + \tilde{K}_h = \frac{Ak}{L} \begin{pmatrix} 1 & -1 \\ -1 & 1 \end{pmatrix} + \begin{pmatrix} hA & 0 \\ 0 & 0 \end{pmatrix}. \quad (51)$$

The mass capacitance matrix M is defined as

$$M = \int_V c_p N^T N dV \quad (52)$$

with the specific heat capacity at constant pressure c_p . For our problem this yields

$$M = \int_V c_p N^T N dV = A c_p \int_0^L \begin{pmatrix} 1 - x/L \\ x/L \end{pmatrix} \begin{pmatrix} 1 - x/L & x/L \end{pmatrix} dx = \frac{c_p A L}{6} \begin{pmatrix} 2 & 1 \\ 1 & 2 \end{pmatrix}. \quad (53)$$

The force vector \vec{f}_h is applied on the outside surface S_1 . The right hand side of Eq. 49 therefore yields

$$\vec{f}_h = \int_{S_1} N^T h T_\infty dS = \frac{A h T_\infty L}{2} \begin{pmatrix} 1 \\ 0 \end{pmatrix}. \quad (54)$$

Following the procedure outlined by Logan [3], the iteration for a future time step of the temperature vector \vec{T}_{i+1} can be obtained implicitly according to

$$\left(\frac{1}{\Delta t} M + K \right) \vec{T}_{i+1} = \left(\frac{1}{\Delta t} M - (1 - \beta) K \right) \vec{T}_i + (1 - \beta) \vec{F}_i + \beta \vec{F}_{i+1} \quad (55)$$

using a weighting factor β . For $\beta = 0.5$ this is called the Crank-Nicholson procedure [10]. Using $\beta = 0$ makes the calculation explicit, which improves calculation time but can cause unstable solutions which may diverge. The implicit calculation is guaranteed to always converge.

Results obtained using the finite difference and finite element codes given in Appendices D and E were compared to the commercial finite element code Abaqus. The case considered was defined by Mills [2], with the following problem parameters: $T_0 = 20^\circ\text{C}$, $T_\infty = 100^\circ\text{C}$, $h = 40 \text{ W/m}^2 \text{ K}$, $\rho = 2600 \text{ kg/m}^3$, $c_p = 800 \text{ J/kg K}$, $k = 1 \text{ W/K}$, $N = 5$ nodes and $\Delta t = 60 \text{ s}$. All three models used the same spatial discretization, with $N=41$ nodes or 40 elements. An exact solution also exists for this problem and can be found in [2]. The Abaqus simulation was done using the mesh depicted in Figure 12. The final temperature distribution computed by Abaqus after 60 minutes is depicted in Figure 13.

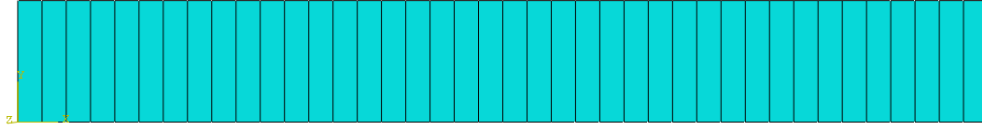


Figure 12: Mesh for Abaqus simulation

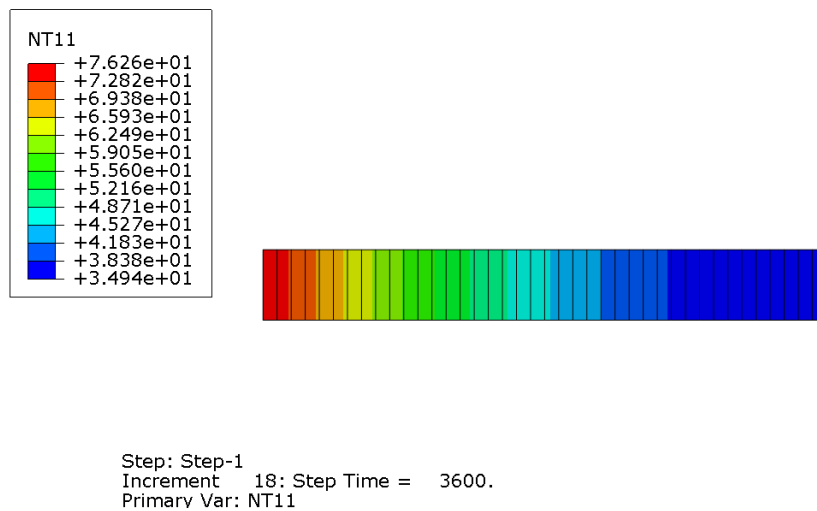


Figure 13: Temperature distribution at $t = 3600 \text{ s} = 60 \text{ min}$ from Abaqus simulation

Comparison of the Abaqus simulation and the finite difference code is shown in Figure 14. The Abaqus temperature distribution in Figure 13 is that same as that plotted in Figure 14. The temperature near the boundary is expectedly high and slowly decreases over the length of the body. As conduction is the only mode of heat transfer within the solid, even after one hour the temperature is only $35 \text{ }^\circ\text{C}$ at the end of the heated body. The curve in Figure 15 shows the temperature history at the surface exposed to convective heating. As time increases, this surface temperature increases more slowly as it approaches the convective fluid temperature, $T_\infty = 100^\circ\text{C}$. All calculations agree very well. The comparison between the

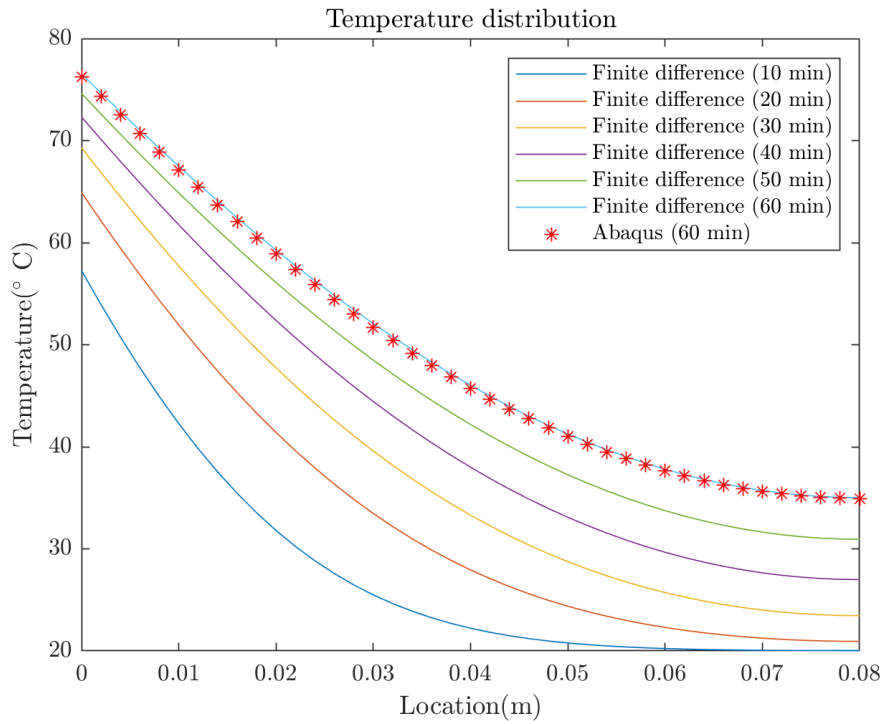


Figure 14: Temperature distribution in Finite Difference calculation and Abaqus simulation

Abaqus simulation and the 1-dimensional finite element code is shown in Figure 15. Here the finite element solution matches the exact solution. In conclusion, for this case of convection boundary conditions, both the 1-dimensional finite difference and finite element methods agree with the Abaqus analysis and the exact solution provided by Mills [2].

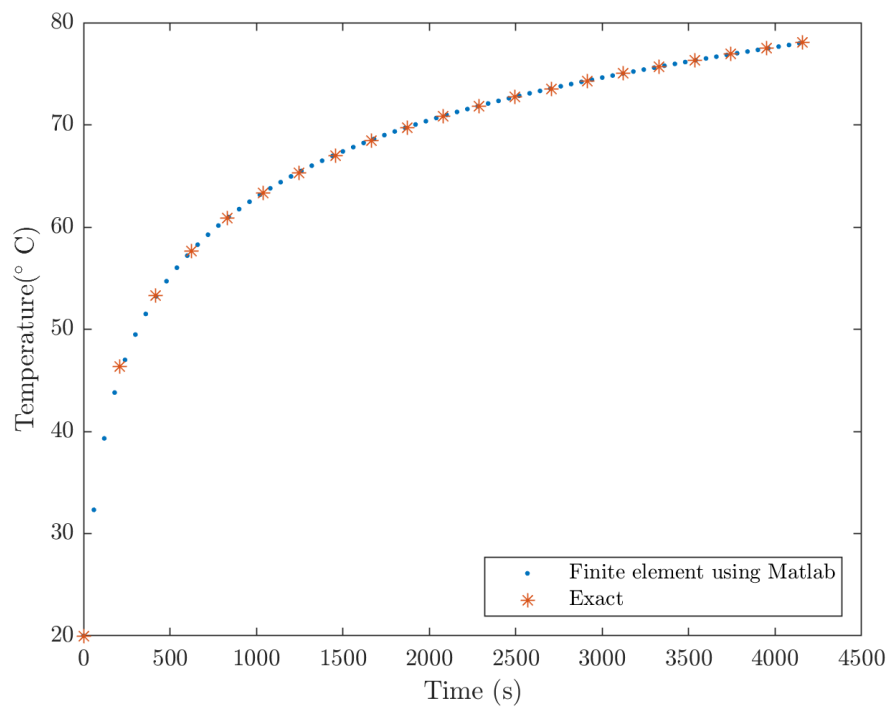


Figure 15: Trend for surface temperature in Finite Element Analysis and exact solution

CHAPTER 5

Solution of various heat transfer problems

5.1 Heated spherical body

The finite difference code for spherically symmetric problems which has been developed in Chapter 2 shall now be employed to calculate the time a sphere takes to heat up when exposed to a higher temperature environment. This problem was solved using a Matlab routine based on Eq. 22, an Abaqus simulation which employs finite element calculations as described in Chapter 2 and compared to the COMSOL solution which is available online [11]. The code used for the Matlab simulation is attached in Appendix B. The radius of the sphere is $r = 2.5$ cm and the initial temperature $T_0 = 5^\circ\text{C}$. The calculation was done using both a convection boundary condition and a temperature boundary condition. The wall temperature was $T_w = 95^\circ\text{C}$. For the convection boundary condition a convective film coefficient of $h = 1200\text{ W/m}^2\text{ K}$ was used.

The other constants are density, $\rho = 993.05\text{ kg/m}^3$, and specific heat capacity at constant pressure, $c_p = 4178.5\text{ J/kg K}$ and thermal conductivity $k = 0.627\text{ W/m K}$. A transient heat transfer analysis with Abaqus used a time step size of $\Delta t = 1$ s, while the Matlab code used $\Delta t = 0.05$ s. Both calculations and the COMSOL solution agree as can be seen in Figure 16. Both simulations calculate the time until the outer boundary of the sphere reaches $T_w = 70^\circ\text{C}$. COMSOL calculates $t_{final} = 860$ s while the finite difference code determined the time required to be $t_{final} = 875.05$ s.

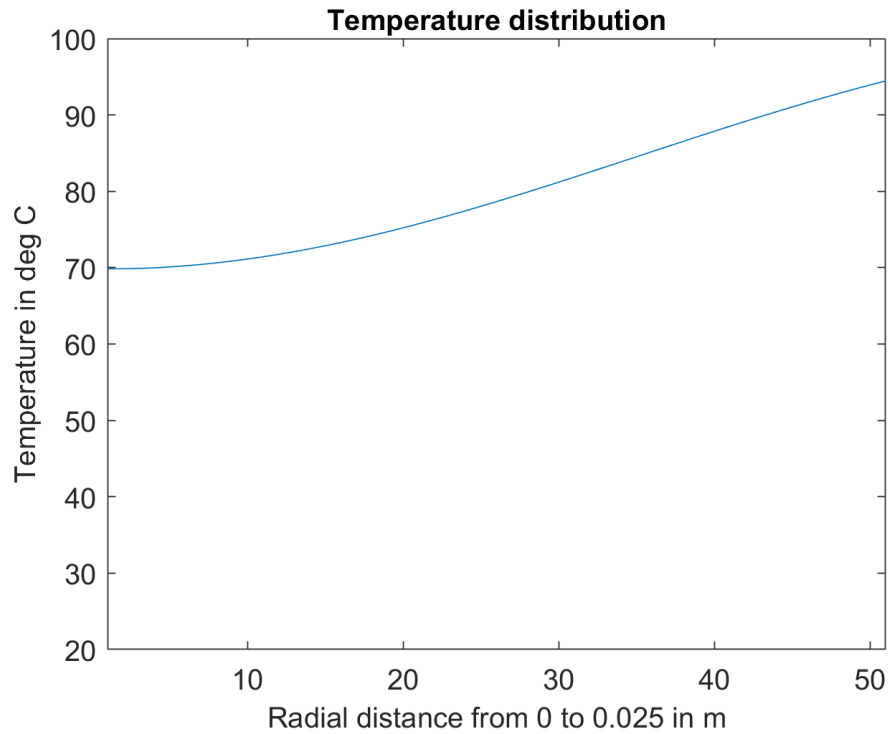


Figure 16: Temperature distribution in finite difference analysis at $t_{final} = 875$ s

5.2 Cooling of insulated rod

The next problem is the steady-state finite element analysis of an insulated rod which has the material properties as delineated in Table 1. The code can be seen in Appendix F.1.

Table 1: Material properties and geometry of insulated rod

T_0	100 °C
T_∞	10 °C
h	10 W/(m ² K)
k	0.627 W/(m K)
Δx	5/6 m
L	10/3 m

The steady-state solution of this problem leads to a temperature profile of $T_1 = 100$ °C as defined by boundary condition, $T_2 = 85.93$ °C, $T_3 = 71.87$ °C,

$T_4 = 57.81 \text{ }^\circ\text{C}$ and $T_5 = 43.75 \text{ }^\circ\text{C}$ for a spacing of $\Delta x = 5/6 \text{ m}$.

5.3 Cooling of rod with free convection

A similar problem to the before discussed one is the cooling of a rod which is now considered with free convection on its perimeter. The material properties are displayed in Table 2. The Matlab code for this problem is shown in Appendix F.2.

Table 2: Material properties and geometry of rod

T_0	200 $^\circ\text{C}$
T_∞	20 $^\circ\text{C}$
h	1 W/(m ² K)
k	3 W/(m K)
Δz	3 m
L	9 m
radius, r	2 m
area, A	12.56 m ²
perimeter, P	12.56 m ²

The free convection now results in the term $f_i = h T_\infty PL/2$ for both components of the force vector. This leads to a final temperature distribution of $T_1 = 200 \text{ }^\circ\text{C}$ at the boundary and $T_2 = 42.86 \text{ }^\circ\text{C}$, $T_3 = 22.92 \text{ }^\circ\text{C}$ and $T_4 = 20.49 \text{ }^\circ\text{C}$ at the nodes.

5.4 Transient insulated fin

Now a non-steady state problem shall be discussed. Similarly to Chapter 3 Eq. 55 is used to calculate the temperature increase over a rod which is heated on one end. A model of the rod with two elements is shown in Figure 17. The material and geometric parameters for this problem are given in Table 3. The Matlab code to solve this problem is attached in Appendix F.3.

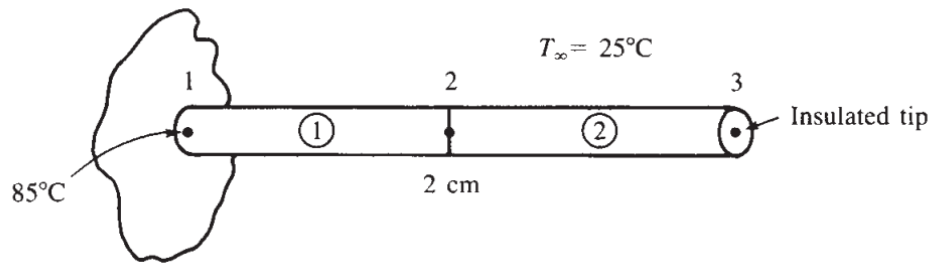


Figure 17: Transient fin with convection (adapted from [3])

Table 3: Material properties and geometry of fin

T_0	25 °C
T_∞	25 °C
T_1	85 °C
h	150 W/(m ² K)
k	400 W/(m K)
Δx	0.01 m
L	0.02 m
radius, r	2 mm
area, A	12.56 mm ²
perimeter, P	12.56 mm

The calculated temperature distribution can be seen in Fig. 18. A slow increase from 25 °C to 70 °C can be observed. As expected, the further node heats up more slowly. A saturation effect similar to the problem discussed in Chapter 4 can be observed. In this case, both nodes tend towards the boundary temperature T_1 .

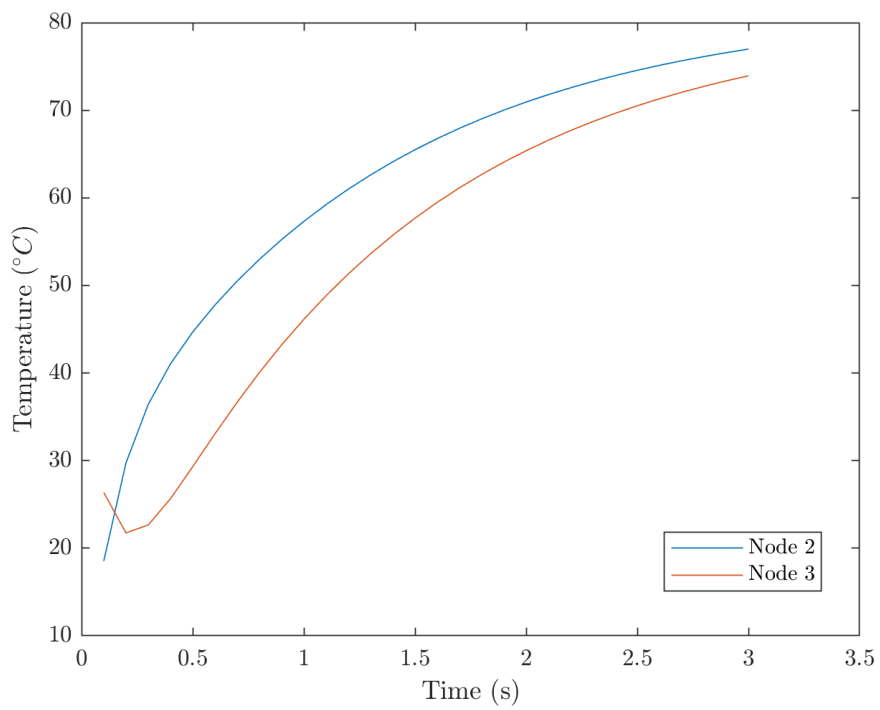


Figure 18: Temperature plot for transient fin for nodes 2 and 3

CHAPTER 6

Heat transfer problems involving phase change

6.1 Freezing problem

This problem was simulated to reproduce the findings of [11]. The problem was considered by performing an Abaqus simulation to verify the literature. A liquid probe is cooled down which leads to freezing from the top of the probe downwards. Points A and B are within the probe and represent different locations. Point A has coordinates $(1, -7)$ and B $(2, -7)$. The freezing boundary condition applies on every edge of a 2-dimensional square with dimensions 8×8 . The simulation uses non-dimensionalized units and uses $\rho = c_p = 1$, $k = 1.08$ and a latent heat of $h_{fs} = 70.26$. The location of points A and B as well as the boundary conditions is shown in Figure 19.

The decline in temperature is depicted in Figure 20 and shows good agreement between the Abaqus simulations (for coarse and fine meshes) and the literature solution by [11]. Additionally, Figures 21 to Figures 29 show the growth of the freeze front as well as the temperature distributions at time instants $t_i = \{0, 1, 2, 3, 4, 5\}$. Abaqus used automatic time stepping which determines the time step size according to the residual of a previous iteration. This leads to irregularly spaced time increments which is also depicted in the figures below. The temperature distribution for $t = 0$ s is depicted in Figure 24.

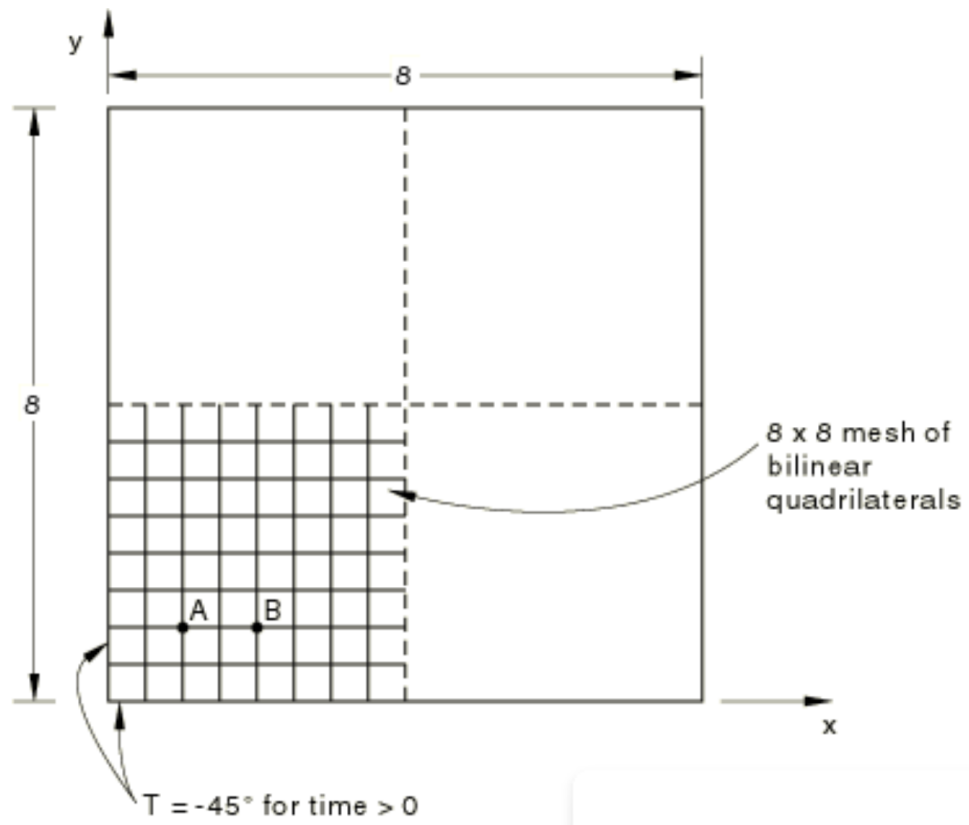


Figure 19: Square plate freezing with points A and B (adapted from [4])

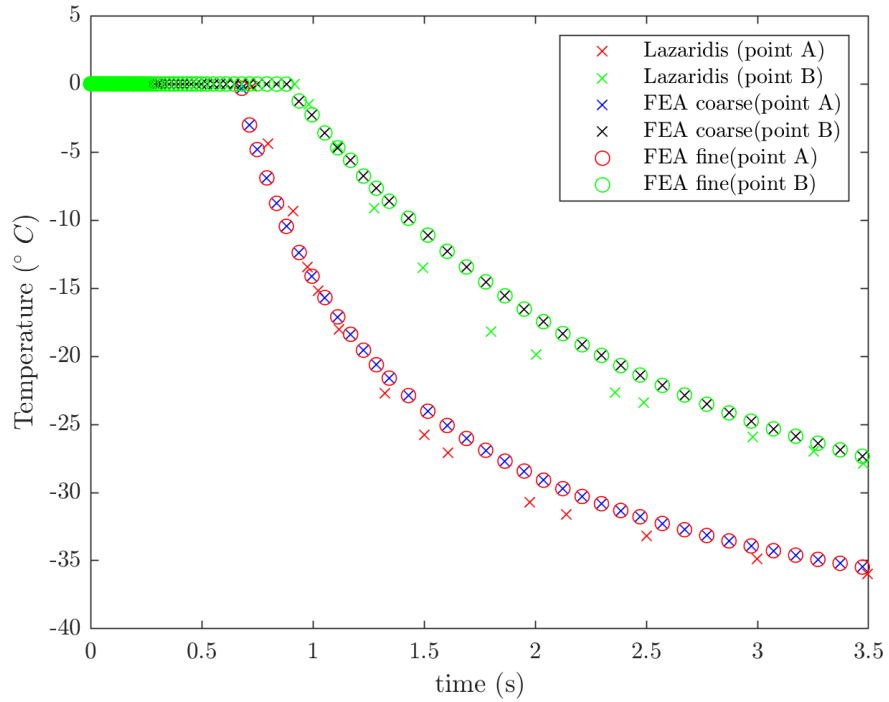


Figure 20: Temperature plot for freezing problem at points A and B

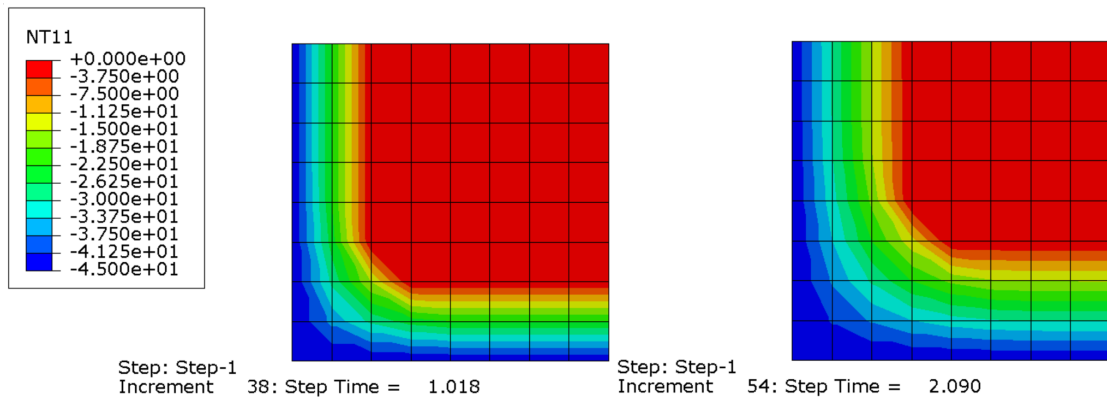


Figure 21: Temperature distribution of freezing problem at $t = 1$ s, $t = 2$ s

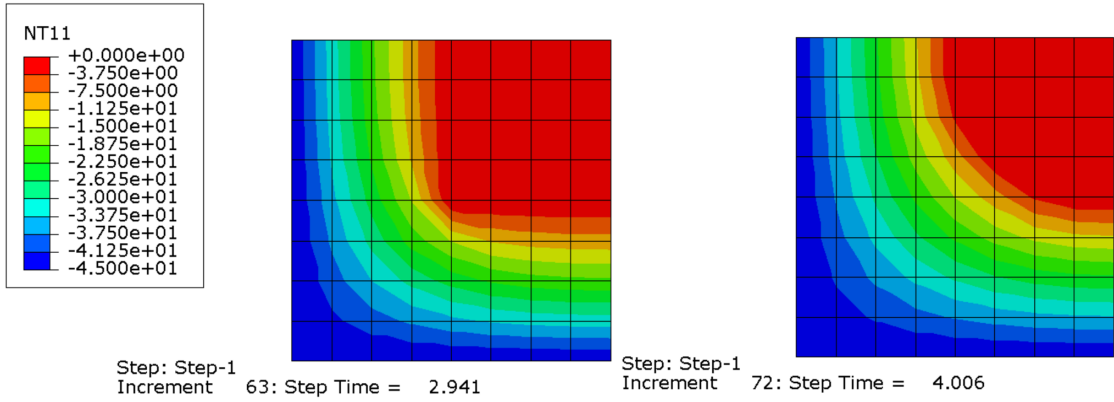


Figure 22: Temperature distribution of freezing problem at $t = 3 s$, $t = 4 s$

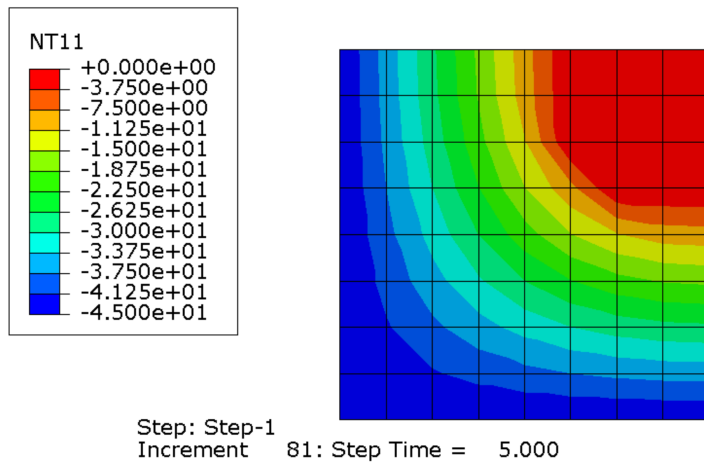


Figure 23: Temperature distribution of freezing problem at $t = 5 s$

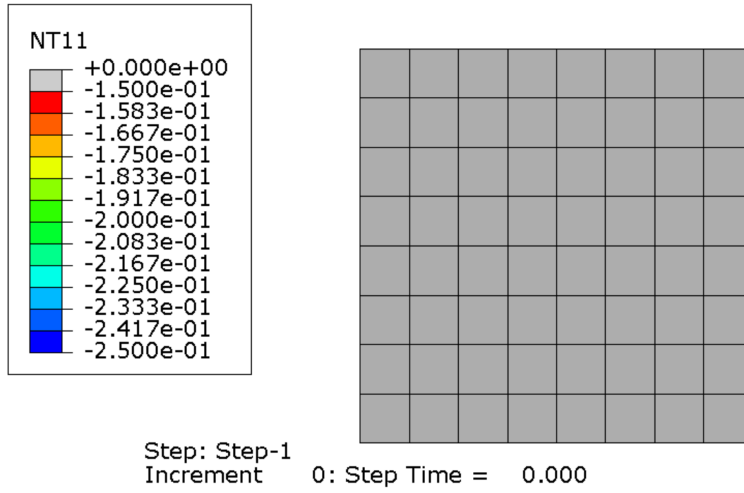


Figure 24: Temperature distribution at $t = 0$ s

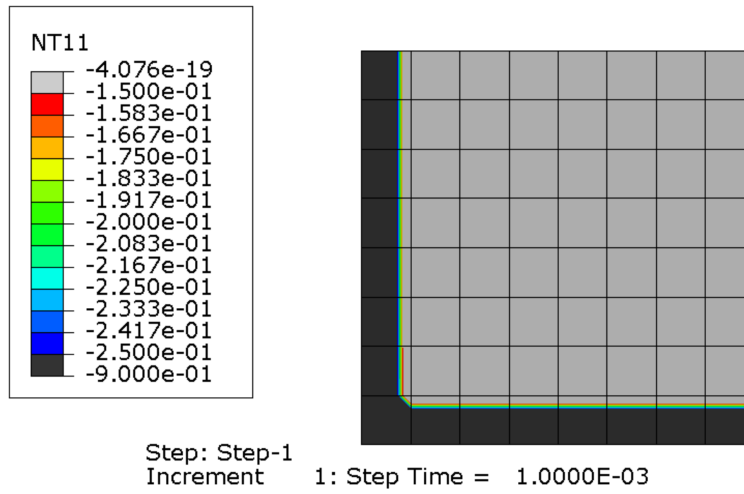


Figure 25: Growth of freeze front (grey to black) at t_1

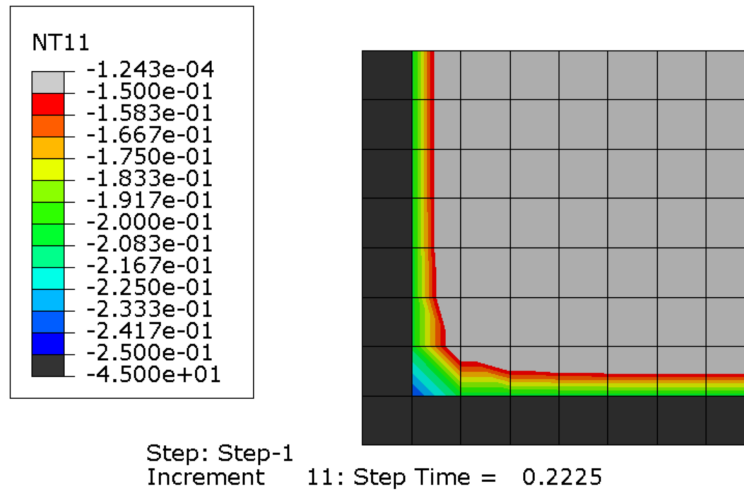


Figure 26: Growth of freeze front (grey to black) at t_2

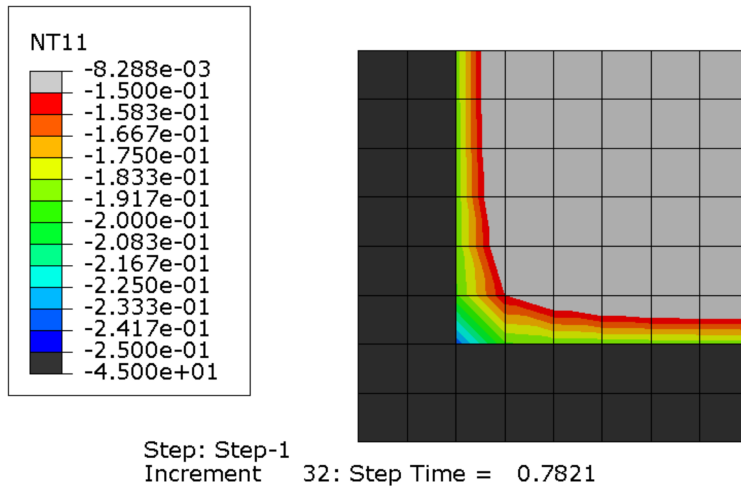


Figure 27: Growth of freeze front (grey to black) at t_3

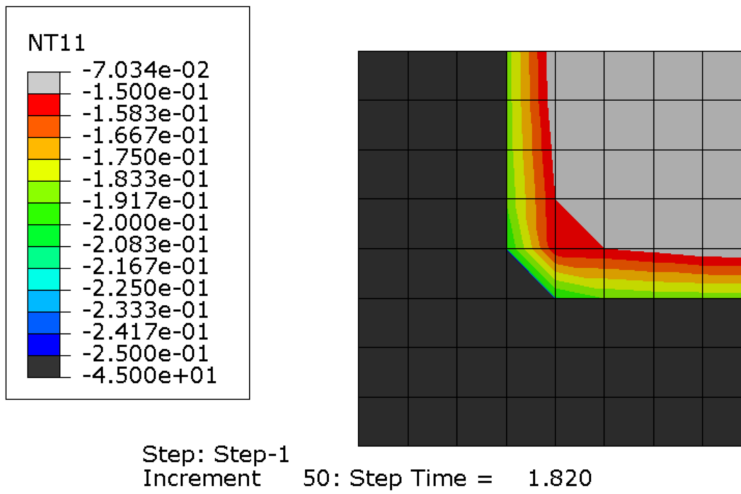


Figure 28: Growth of freeze front (grey to black) at t_4

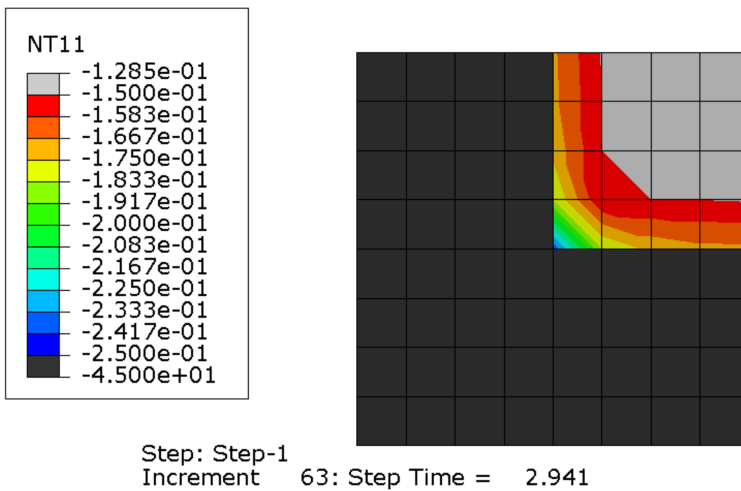


Figure 29: Growth of freeze front (grey to black) at t_5

6.2 1-dimensional phase change with latent heat in force vector

In one approach to modeling phase change, an altered force vector associated with heat released or absorbed can be included in finite element simulations. The liquidus and solidus temperatures define the temperature range over which heat is absorbed or released during the phase change. The solidus temperature is the highest temperature where the material is completely solid and the liquidus temperature is the lowest temperature where the material is completely liquid ($T_S > T_L$). To model phase change for 1-dimensional elements, force vectors can be defined which depend on the temperature distribution within each element.

Within each element, the assumed linear interpolation for the temperature distribution between two nodes with temperatures T_i and T_{i+1} can be expressed as

$$T(x) = \left(1 - \frac{x}{L} \quad \frac{x}{L}\right) \begin{pmatrix} T_i \\ T_{i+1} \end{pmatrix} \quad (56)$$

where x is the position ($0 \leq x \leq L$) and L is the element length. The force vector associated with internal heat generation due to phase change is found by integrating over the values of x for which the temperature is between the solidus and liquidus temperatures:

$$\{f_Q\} = \begin{Bmatrix} f_{Q1} \\ f_{Q2} \end{Bmatrix} = \begin{Bmatrix} h_{fs} A \int_{x_{lower}}^{x_{upper}} \left(1 - \frac{x}{L}\right) dx \\ h_{fs} A \int_{x_{lower}}^{x_{upper}} \frac{x}{L} dx \end{Bmatrix} \quad (57)$$

where h_{fs} is the latent heat of fusion, A is the element cross-sectional area, and x_{lower} and x_{upper} are the limits of integration. The limits of integration correspond to the points where the solidus and liquidus temperatures intersect the interpolated temperature distributions within the element. For each element, depending on the relative values of the nodal temperatures T_1 and T_2 , and the solidus and liquidus temperatures, T_S and T_L , 12 possible cases can be identified. These cases are summarized in Table 4 and are illustrated in Figures 30 and 31. The dashed blue line represents T_S and the orange one T_L respectively.

Table 4: Types of element temperature distributions

Type	T_1 vs. T_2	T_1	T_2	x_{lower}	x_{upper}
1	$T_1 > T_2$	$T_1 \leq T_S$	$T_2 \leq T_S$	-	-
2	$T_1 > T_2$	$T_1 > T_S, T_1 \leq T_L$	$T_2 \leq T_S$	0	$\frac{(T_1 - T_S)L}{(T_1 - T_2)}$
3	$T_1 > T_2$	$T_1 > T_S, T_1 \leq T_L$	$T_2 > T_S$	0	L
4	$T_1 > T_2$	$T_1 > T_L$	$T_2 < T_S$	$\frac{(T_1 - T_L)L}{(T_1 - T_2)}$	$\frac{(T_1 - T_S)L}{(T_1 - T_2)}$
5	$T_1 > T_2$	$T_1 > T_L$	$T_2 \leq T_L$	$\frac{(T_1 - T_L)L}{(T_1 - T_2)}$	L
6	$T_1 > T_2$	$T_1 > T_L$	$T_2 > T_L$	-	-
7	$T_2 > T_1$	$T_1 < T_S, T_1 \leq T_L$	$T_2 \leq T_S$	-	-
8	$T_2 > T_1$	$T_1 \leq T_S$	$T_2 > T_S, T_2 \leq T_L$	$\frac{(T_S - T_1)L}{(T_2 - T_1)}$	L
9	$T_2 > T_1$	$T_1 \leq T_S$	$T_2 > T_S, T_2 \leq T_L$	0	L
10	$T_2 > T_1$	$T_1 \leq T_S$	$T_2 > T_L$	$\frac{(T_S - T_1)L}{(T_2 - T_1)}$	$\frac{(T_L - T_1)L}{(T_2 - T_1)}$
11	$T_2 > T_1$	$T_1 > T_S, T_1 \leq T_L$	$T_2 > T_L$	0	$\frac{(T_L - T_1)L}{(T_2 - T_1)}$
12	$T_2 > T_1$	$T_1 > T_L$	$T_2 > T_L$	-	-

For elements where the temperature profile is characterized by types 1, 6, 7 and 12, the element temperatures are either below the solidus temperature or above the liquidus temperature and hence no internal heat is absorbed or released. For the other temperature distribution types, f_Q can be evaluated analytically to compute nodal force values for each element. The resulting nodal force vectors for each case are given in Table 5.

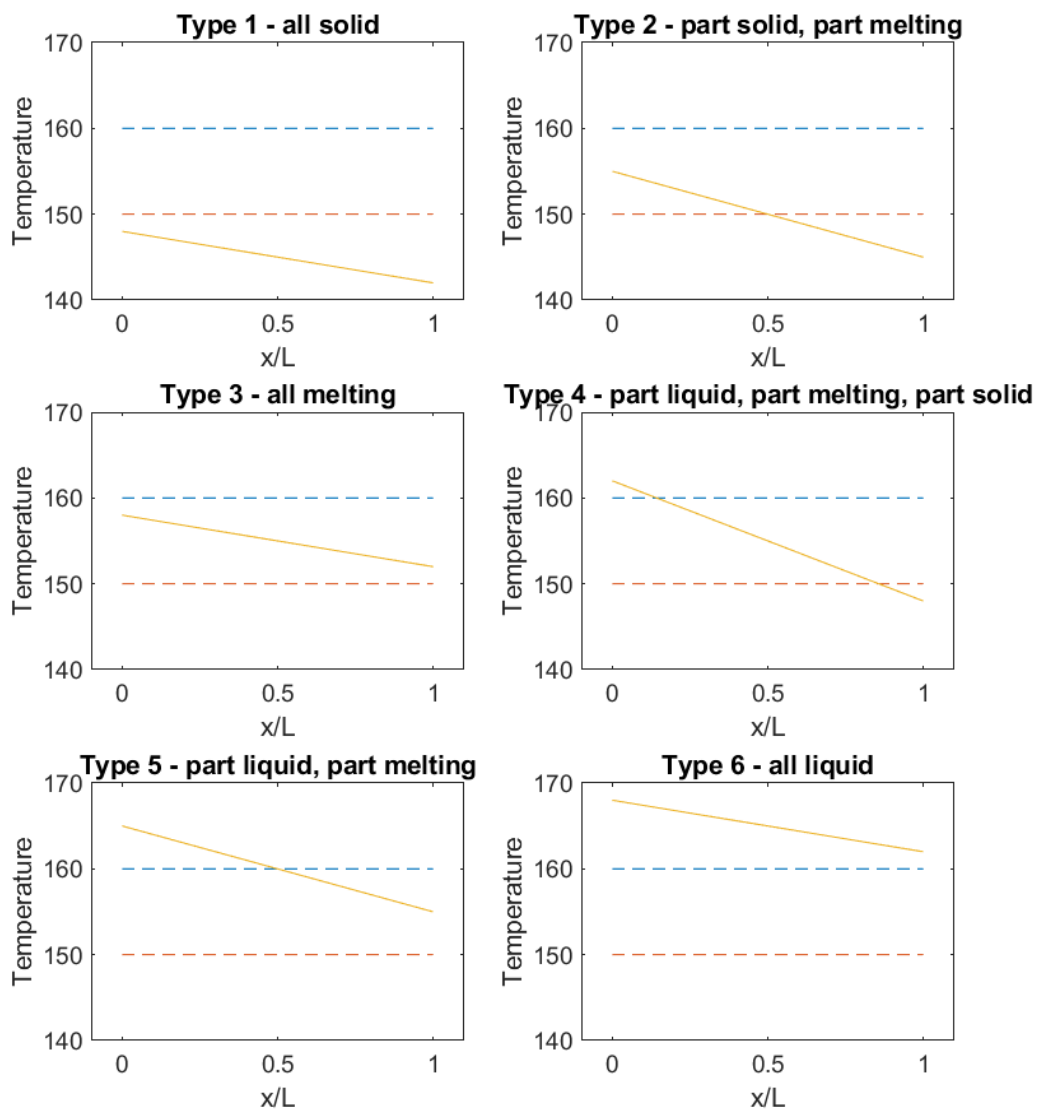


Figure 30: Element temperature distribution types 1-6

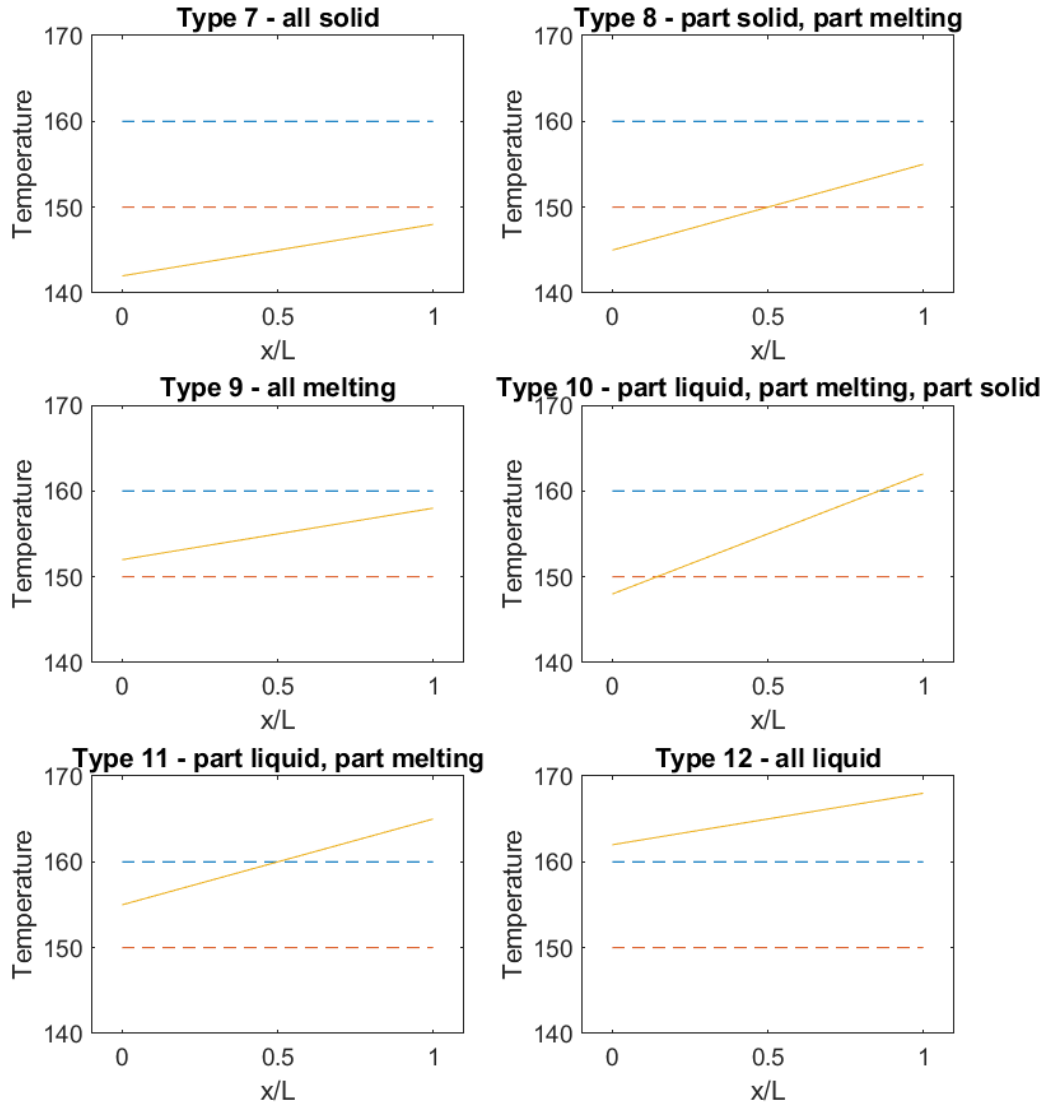


Figure 31: Element temperature distribution types 7-12

Table 5: Element force vectors

Type	$\{f_Q\}$
1	$\begin{Bmatrix} 0 \\ 0 \end{Bmatrix}$
2	$\frac{h_{fs}AL}{2(T_1 - T_2)^2} \begin{Bmatrix} (T_1 - T_S)(T_1 - 2T_2 + T_S) \\ (T_1 - T_S)^2 \end{Bmatrix}$
3	$\frac{h_{fs}AL}{2} \begin{Bmatrix} 1 \\ 1 \end{Bmatrix}$
4	$\frac{h_{fs}AL}{2(T_1 - T_2)^2} \begin{Bmatrix} (T_L - T_S)(T_L - 2T_2 + T_S) \\ (T_L - T_S)(T_L - 2T_1 + T_S) \end{Bmatrix}$
5	$\frac{h_{fs}AL}{2(T_1 - T_2)^2} \begin{Bmatrix} (T_2 - T_L)^2 \\ (T_1 - T_2)^2 - (T_1 - T_L)^2 \end{Bmatrix}$
6	$\begin{Bmatrix} 0 \\ 0 \end{Bmatrix}$
7	$\begin{Bmatrix} 0 \\ 0 \end{Bmatrix}$
8	$\frac{h_{fs}AL}{2(T_1 - T_2)^2} \begin{Bmatrix} (T_2 - T_S)^2 \\ (T_1 - T_2)^2 - (T_1 - T_S)^2 \end{Bmatrix}$
9	$\frac{h_{fs}AL}{2} \begin{Bmatrix} 1 \\ 1 \end{Bmatrix}$
10	$\frac{h_{fs}AL}{2(T_1 - T_2)^2} \begin{Bmatrix} (T_L - T_S)(T_L - 2T_2 + T_S) \\ (T_L - T_S)(T_L - 2T_1 + T_S) \end{Bmatrix}$
11	$\frac{h_{fs}AL}{2(T_1 - T_2)^2} \begin{Bmatrix} (T_1 - T_L)(T_1 - 2T_2 + T_L) \\ (T_1 - T_L)^2 \end{Bmatrix}$
12	$\begin{Bmatrix} 0 \\ 0 \end{Bmatrix}$

6.3 1-dimensional phase change with modified specific heat

An alternative model for the melting phenomenon can be found in [12]. It incorporates the latent heat as a different specific heat at constant pressure c_p within the melting range which is in between T_S and T_L . The latent heat h_{fs} leads to the following expression within the melting range

$$c_p^* = \frac{h_{fs}}{T_L - T_S} + c_p \quad (58)$$

Using a simple if-alternative this can be incorporated into the melting code which was formulated in Matlab and compared to Abaqus results. The next section deals with the force vector approach and the specific heat approach.

6.4 Extension to cylindrical and spherical coordinates

In order to model 3-dimensional problems with the developed methods, different coordinate systems can be used and simplified using symmetry relations. Therefore a 3-dimensional calculation may only depend on the radial coordinate r . Fig. 32 shows a semi-infinite plane with a surface heat flux in its center. For a punctual heat flux such as a laser even a small pin can be modeled as a semi-infinite plane. Then this is evaluated in spherical coordinates using a symmetry plane which is placed in the same location as the outer surface. This calculation in spherical coordinates allows more problems to be analyzed than just the 1-dimensional Cartesian case. In the following subsection both cylindrical and spherical coordinates are used for the governing numerical equations. The conductivity matrix K and the mass matrix M can be seen in Chapter 3 (Eqs. 41 and 43)

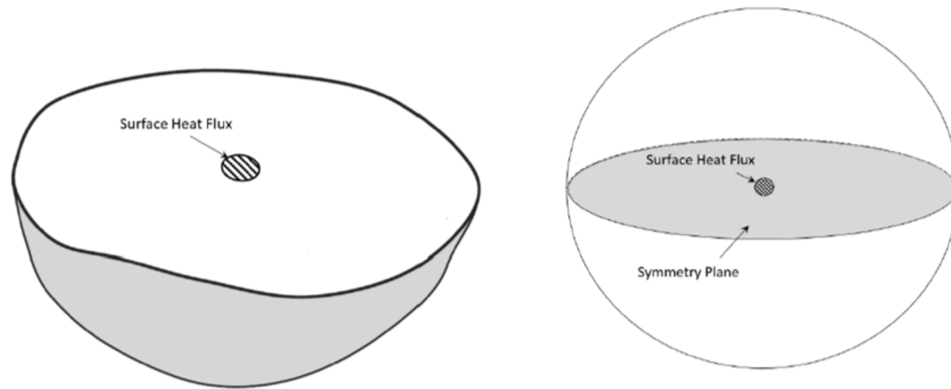


Figure 32: Localized heating of semi-infinite domain modelled as spherically symmetrical

6.5 1-dimensional melting problem

To evaluate the 1-dimensional phase change equations, transient heat transfer with melting is considered. A cylinder of radius r and length L is initially at temperature T_0 . At time $t = 0$ the left end $x = 0$ temperature is set to T_1 . The problem's dimensions and thermal properties are given in Table 6.

Table 6: Material properties and geometry for 1-dimensional cylinder melting

T_0	100 °C
T_1	200 °C
T_S	150 °C
T_L	160 °C
h_{fs}	3e6 W/(m ² K)
k	0.195 W/(m K)
c_p	0.195 J/(kg K)
Δx	0.06 mm
L	6 mm
radius, r	1 mm
area, A	3.142 mm ²

The Matlab implementation of the latent heat force vector approach given in section 6.2 can be found in Appendices C and H. The computed temperature distri-

butions at times $t = 10$ s, 50 s and 100 s are shown in Figure 33 and are compared to results obtained using Abaqus. Although the overall temperature distributions correlate reasonably well, the Matlab code does not accurately track the location of the melt front. Further investigation is required to understand this discrepancy.

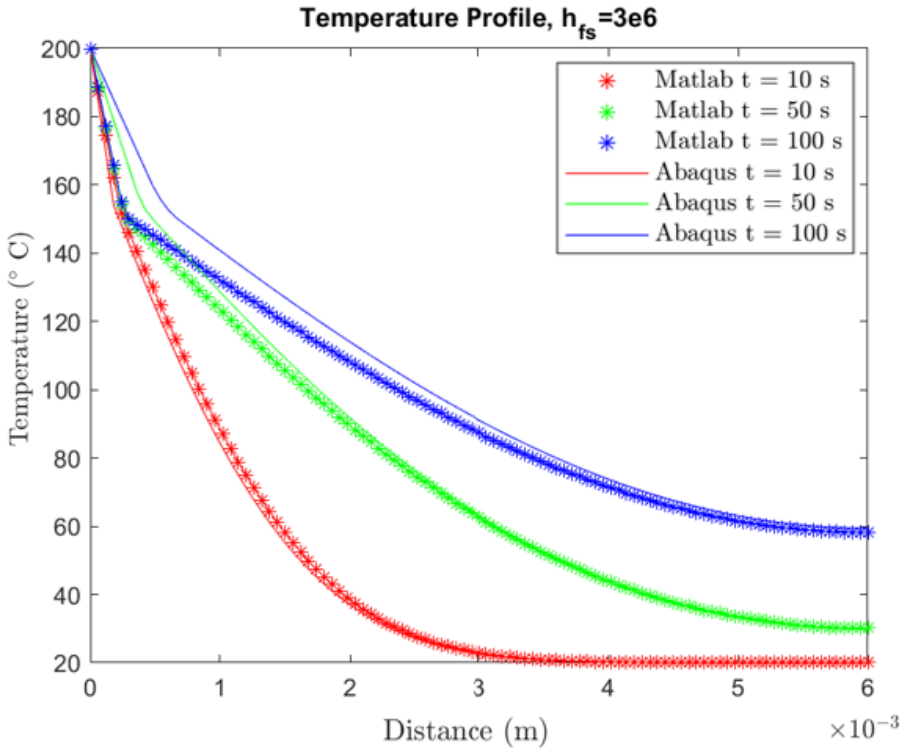


Figure 33: 1-dimensional melting with temperature boundary conditions

Now the specific heat approach is compared to the Abaqus results. The Abaqus simulation was done using Cartesian, cylindrical and spherical coordinates. The resulting temperature distributions for Cartesian, cylindrical and spherical coordinate systems over the depth of the cylinder are shown in Fig. 34 to 36. Additionally the growth of the melt front can be seen in Fig. 37. This depiction is similar to the freeze front which was shown in Fig. 24 to 29. The melt front grows

over the different finite elements. This leads to equidistant column heights which slowly grow at a slower rate because the penetration of the melt zone slows down. The used code can be found in Appendix I. The Abaqus data can be shared upon request.

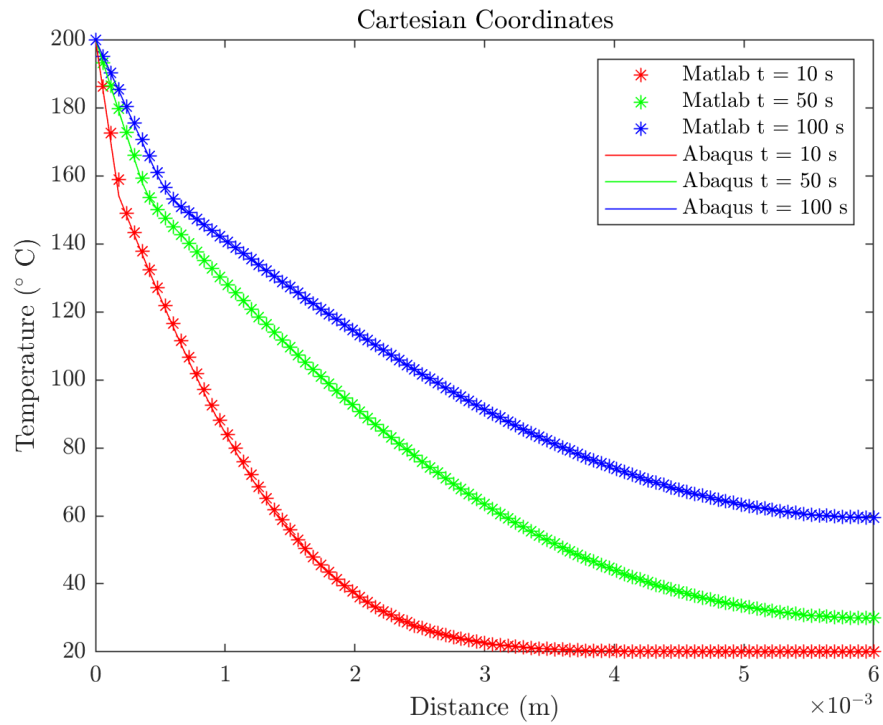


Figure 34: 1-dimensional melting in Cartesian coordinate system

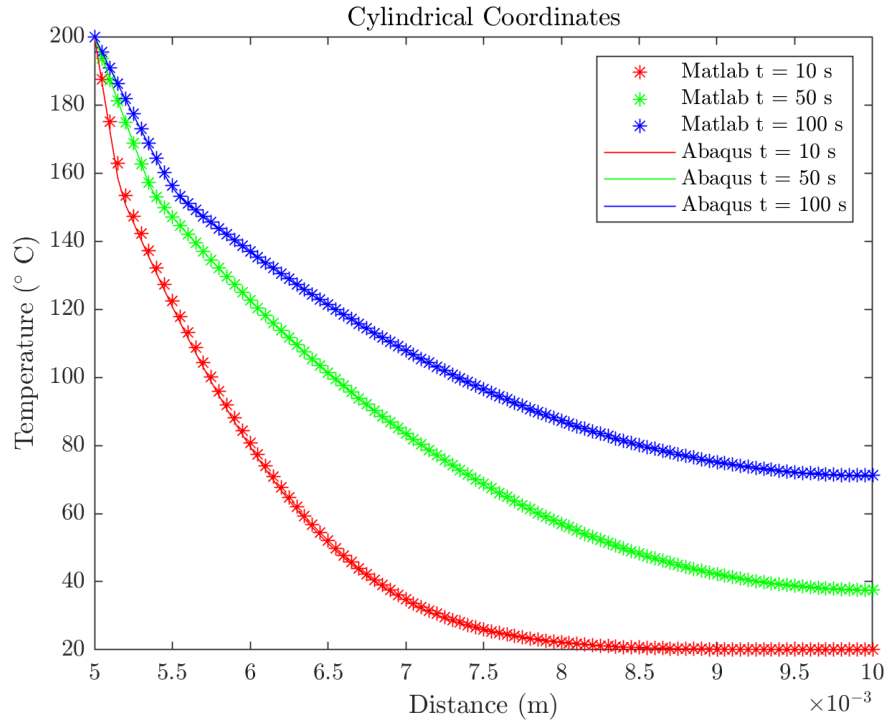


Figure 35: 1-dimensional melting in cylindrical coordinate system

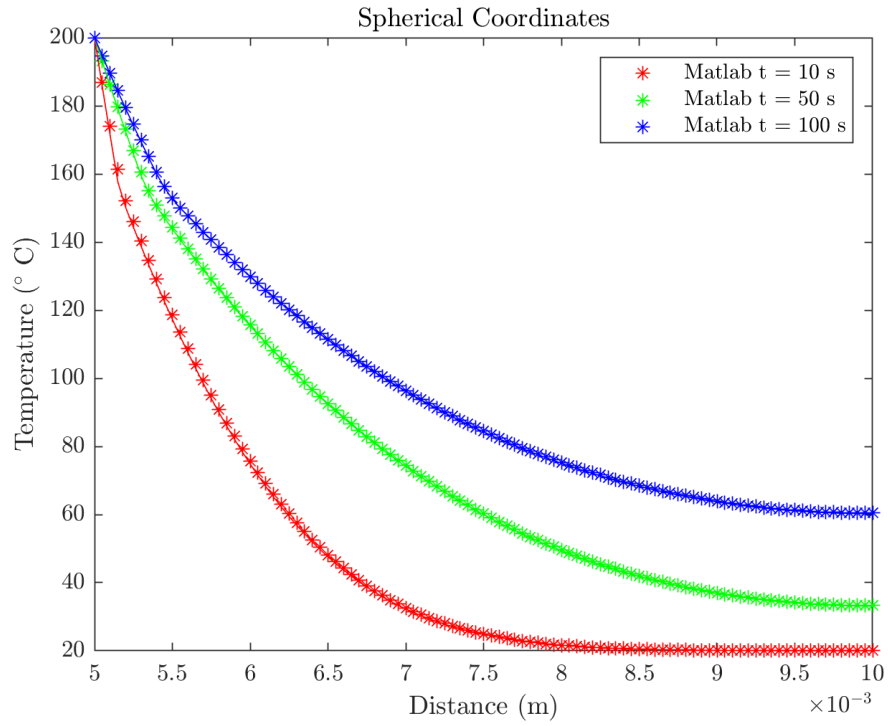


Figure 36: 1-dimensional melting in spherical coordinate system

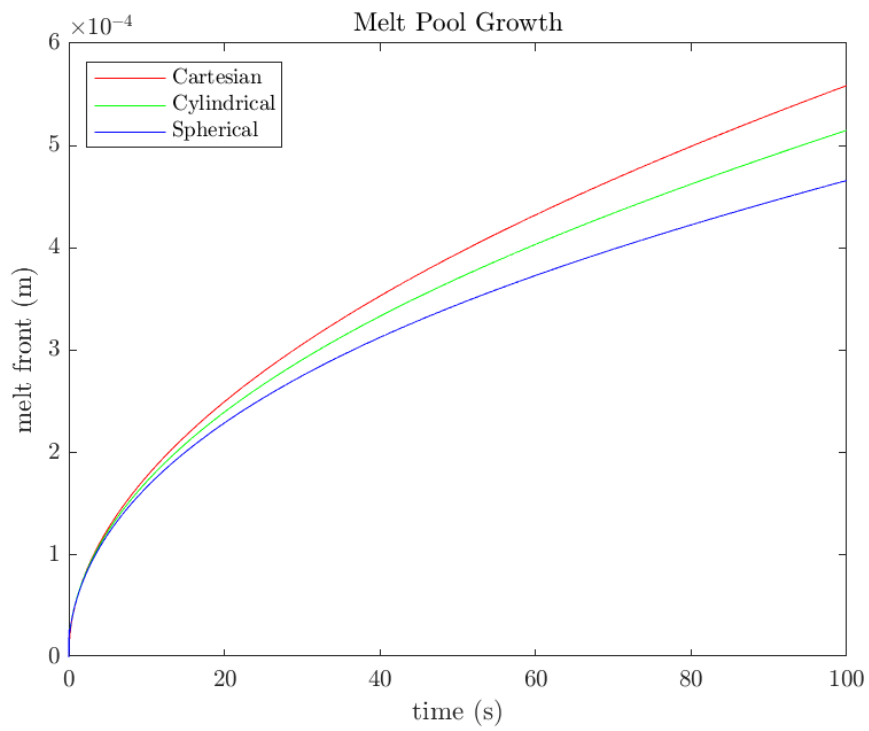


Figure 37: 1-dimensional melting in different coordinate systems

CHAPTER 7

Conclusion

Different heating problems were simulated using commercial software and self-written code. Various numerical approximation schemes were used and compared. Finally a finite element code for melting was compared to commercial software for two different latent heat models. A 1-dimensional Cartesian model was adapted for spherically symmetric melting, where a melt zone grows radially from the center of the domain. This can solve 3-dimensional problems with spherical symmetry. A laser melting a pin can be assumed to be a semi-infinite sphere. Such a solution is a computationally efficient estimate of melt zone growth in the vicinity of a focused heat source on the surface of a semi-infinite domain. This modeling capability could prove to be valuable in studying additive manufacturing processes.

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APPENDIX A

Matlab script for 1-dimensional finite difference method in Cartesian coordinates

```
% Heat Conduction Equation in one dimension
% Solves  $dT/dt = a * ( d^2T/dx^2 + 2 dT/(dx^2 * r) )$ 

clc;
close all;
clear all;

%dimensions
N = 51;

Dx=0.0005; % step size
Nx=0.025;
X=0:Dx:Nx;
k = 0.627; % thermal conductivity in W / (m K)
rho = 993.95; %denisty in kg/m^3
cp = 4178.5; %specific heat at const. press. in J / (kg K)
a=1; % arbitrary thermal diffusivity
a = k / (rho*cp);
h = 1200; %W/ m deg C
Tinf = 95;
Bi = h * Dx / k;

%boundary conditions
T(1:N) = 5 ;
T(N) = 95; %temp bound. cond.
T(N) = (2*T(N-1) + Bi*Tinf)/(2+Bi);

%%
%initial condition
Tmax=max(T);

DT = 0.05;
%DT = DR^2/(2*a); % time step
M = 20000; % maximum number of allowed iteration

%finite difference scheme

fram=0;
Ncount=0;
loop=1;

while loop==1;
    ERR=0;
    T_old = T;

    for i = 2:N-1

        Residue=(DT*((T_old(i+1)-2*T_old(i)+T_old(i-1))/Dx^2 ...
                    + 2*(T_old(i+1) - T_old(i))/(Dx^2 * i))...
                + T_old(i))-T(i);

        T_old(1) = T_old(2);
        ERR = ERR+abs(Residue);
        T(i) = T(i)+Residue*a;
        T(1) = T(2);
        T(N) = (T(N-1) + T_old(N) + Bi*Tinf)/(2+Bi);

    end

    if (ERR>=0.000001*Tmax) % allowed error limit is 1%
        loop=0;
    end
end
```

```

% of maximum temperature
Ncount=Ncount+1;
    if (mod(Ncount,50)==0) % displays movie
        % frame every 50 time steps
        fram=fram+1;
        plot(T);
        ylim([5,95])
        axis([1 N 20 100])
        h=gca;
        get(h, 'FontSize')
        set(h, 'FontSize',12)
        xlabel('radial distance from 0 to 0.025 m',...
            'fontSize',12);
        ylabel('temperature in deg C','fontSize',...
            12);
        title('temperature distribution in egg ',...
            'fontSize',12);
        fh = figure(1);
        set(fh, 'color', 'white');
        F=getframe;
    end

% if solution do not converges
% in M time steps

    if(Ncount>M)
        loop=0;
        disp(['solution does not reach...
            steady state in ',num2str(M),...
            'time steps'])
    end

% if solution converges within x time ste
% ps

else
    loop=0;
    disp(['solution reaches steady state in ',...
        num2str(Ncount) , 'time steps'])
end
end

% display a movie of heat diffusion
movie(F,fram,1);
disp(['time elapsed:',num2str(Ncount*DT) , 's'])

```

APPENDIX B

Matlab script for 1-dimensional finite difference method in spherical coordinates

```
% Spherical Heat Conduction Equation in one dimension
% Solves  $dT/dt = a * ( d^2T/dr^2 + 2 dT/(dr^2 * r) )$ 

clc;
close all;
clear all;

%dimensions
N = 51;

DR=0.0005; % step size
Nr=0.025;
X=0:DR:Nr;
k = 0.627; % thermal conductivity in W / (m K)
rho = 993.95; %denisty in kg/m^3
cp = 4178.5; %specific heat at const. press. in J / (kg K)
a=1; % arbitrary thermal diffusivity
a = k / (rho*cp);
h = 1200; %W/ m deg C
Tinf = 95;
Bi = h * DR / k;

%boundary conditions
T(1:N) = 5 ;
T(N) = 95; %temp bound. cond.
T(N) = (2*T(N-1) + Bi*Tinf)/(2+Bi);

%for cart., works: (2*T(N-1) + Bi*Tinf)/(2+Bi);
% doesnt work:
%(T(N-1) + h*DR/k*Tinf)/(1 + h*DR/k); %convective bound cond.
% k * dT/dx = h * (T-Tinf)
%dT/dx = T(N) - T(N-1) / dx or T(N-1) - T(N) / dx
%h * (T(N) - Tinf)
%T(N) = (T(N-1) - h*dx/k*Tinf)/(1 - h*dx/k)
%%
%initial condition
Tmax=max(T);

DT = 0.05;
%DT = DR^2/(2*a); % time step
M = 20000; % maximum number of allowed iteration

%finite difference scheme

fram=0;
Ncount=0;
loop=1;

while loop==1;
    ERR=0;
    T_old = T;

    for i = 2:N-1
        Residue=(DT*((T_old(i+1)-2*T_old(i)+T_old(i-1))/DR^2 ...
            + 2*(T_old(i+1) - T_old(i))/(DR^2 * i))...
            + T_old(i))-T(i);
        T_old(1) = T_old(2);
        ERR = ERR+abs(Residue);
    end
end
```

```

T(i) = T(i)+Residue*a;
T(1) = T(2);
T(N) = (T(N-1) + T_old(N) + Bi*Tinf)/(2+Bi);
%old: (T(N-1) - h*DR/k*Tinf)/(1 - h*DR/k); %for conv. bound. cond.
end
if(ERR>=0.000001*Tmax) % allowed error limit is
% 1% of maximum temperature
Ncount=Ncount+1;
    if (mod(Ncount,50)==0)
        % displays movie frame every 50 time steps
        fram=fram+1;
        plot(T);
        ylim([5,95])
        axis([1 N 20 100])
        h=gca;
        get(h,'FontSize')
        set(h,'FontSize',12)
%
        colorbar('location','eastoutside','fontsize',12);
        xlabel('radial distance from ...
0 to 0.025 m','fontSize',12);
        ylabel('temperature in deg C','fontSize',12);
        title('temperature distribution in egg ',...
'fontSize',12);
        fh = figure(1);
        set(fh, 'color', 'white');
        F=getframe;
    end

%if solution does not converge in
% 2000 time steps

    if(Ncount>M)
        loop=0;
        disp(['solution do not...
reach steady state in ',num2str(M),...
'time steps'])
    end

% if solution converges within 2000 time steps
else
    loop=0;
    disp(['solution reaches steady state in ',...
num2str(Ncount) , 'time steps'])
end
end
% display a movie of heat diffusion
movie(F,fram,1);
disp(['time elapsed:',num2str(Ncount*DT) , 's'])

```

APPENDIX C

Matlab script for validation of 1-dimensional finite element methods

```
% 1-D conduction
clc; clear all; close all; format compact
set(groot, 'defaulttextinterpreter', 'latex');
set(groot, 'defaultAxesTickLabelInterpreter', 'latex');
set(groot, 'defaultLegendInterpreter', 'latex');
for coordtype=1:3 % (1- Cartesian, 2-Cylindrical, 3- Spherical)
    %% set constants

    h = 40; % W/m^2 K
    rho = 2600; % kg/m^3
    c = 800; % J/kg K
    k = 1; % W/m K

    %% define mesh
    x1=0.05; % left node coordinate(m)
    x2=.1; % right node coordinate (m)
    L = x2-x1; % m
    N=21; % number of nodes;
    dx=L/(N-1);
    xfea=x1:dx:x2;

    %% set BC
    T1=20;
    T2=100;

    %% calculate element stiffness matrix and assemble
    global stiff. mat.
    if coordtype==1
        A=1; % m^2
        Ke = A*k/dx*[1,-1;-1,1];
        K = zeros(N);
        for i = 1:N-1
            K(i,i) = K(i,i)+ Ke(1,1);
            K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
            K(i,i+1) = Ke(1,2);
            K(i+1,i) = Ke(2,1);
        end
    elseif coordtype==2
        K = zeros(N);
        for i = 1:N-1
            Ke = 2*pi*k*(xfea(i)+xfea(i+1))/(2*dx)*[1,-1;-1,1];
            K(i,i) = K(i,i)+ Ke(1,1);
            K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
            K(i,i+1) = Ke(1,2);
            K(i+1,i) = Ke(2,1);
        end
    else
        K = zeros(N);
        for i = 1:N-1
            Ke=4*pi*k*(xfea(i)^2+xfea(i)*xfea(i+1)+xfea(i+1)^2)/ ...
            (3*dx)*[1,-1;-1,1];
            K(i,i) = K(i,i)+ Ke(1,1);
            K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
            K(i,i+1) = Ke(1,2);
            K(i+1,i) = Ke(2,1);
        end
    end
end
%% set temperature BCs solve equations
```

```

F=zeros(N-2,1);
F(1)=-K(2,1)*T1;
F(N-2)=F(N-2)-K(N-1,N)*T2;
Kred=K(2:N-1,2:N-1);
Tred=Kred\F;
Tfea=[T1;Tred;T2];
K*Tfea;
%% compare to exact
xexact=linspace(x1,x2,50);
if coordtype==1
    Texact=T1+(T2-T1)*(xexact-x1)/L;
elseif coordtype==2
    Texact=T1+(T2-T1)*log(xexact/x1)/log(x2/x1);
else
    Texact=T1+(T2-T1)*(x2./xexact).*(xexact-x1)/L;
end
%
h=figure;
plot(xfea,Tfea,'*',xexact, Texact, '-')
xlabel('Position (m)')
ylabel('Temperature (C)')
axis([x1-.01 x2+.01 T1-5 T2+5])
legend('FEA','Exact','Location','NorthWest')
if coordtype==1
    filename='conduction_1D_cartesian';
    title('Cartesian Coordinates')
elseif coordtype==2
    filename='conduction_1D_cylindrical';
    title('Cylindrical Coordinates')
else
    filename='conduction_1D_spherical';
    title('Spherical Coordinates')
end
saveas(h,filename,'png');
end

% 1-D conduction with outer wall convection
clc; clear all; close all; format compact
set(groot,'defaulttextinterpreter','latex');
set(groot,'defaultAxesTickLabelInterpreter','latex');
set(groot,'defaultLegendInterpreter','latex');
for coordtype=1:3 % (1- Cartesian, 2-Cylindrical, 3- Spherical)
    clear T
    %% set constants
    if coordtype==1
        T0 = 20; % deg C
        Tinf = 100; % deg C
        h = 40; % W/m^2 K
        rho = 2600; % kg/m^3
        c = 800; % J/kg K
        k = 1; % W/m K
    elseif coordtype==2
        T0 = 20; % deg C
        Tinf = 100; % deg C
        h = 40; % W/m^2 K
        rho = 2600; % kg/m^3
        c = 800; % J/kg K
        k = 1; % W/m K
    else
        T0 = 5; % deg C
        Tinf = 95; % deg C
        h = 1200; % W/m^2 K
        rho = 993; % kg/m^3
        c = 4178; % J/kg K
        k = 0.627; % W/m K
    end
end

```



```

end
%% define mesh
if coordtype==1
    % for Cartesian, use Mills problem
    x1=0; % left node coordinate(m)
    x2=.08; % right node coordinate (m)
    L = x2-x1; % mesh length (m)
    N=5; % number of nodes;
    dx=L/(N-1); % element length (m)
    xfea=x1:dx:x2;
    %
elseif coordtype==2
    x1=0.05; % left node coordinate(m)
    x2=.1; % right node coordinate (m)
    dz=1; % unit height in z-direction (m)
    L = x2-x1; % m
    N=51; %21; % number of nodes;
    dx=L/(N-1); % element length (m)
    xfea=x1:dx:x2;
else
    % for Spherical, use boiling egg problem
    x1=0; % left node coordinate(m)
    x2=.025; % right node coordinate (m)
    L = x2-x1; % m
    N=21; % number of nodes;
    dx=L/(N-1);
    xfea=x1:dx:x2;
end

%% set Initial condition
if coordtype==1
    T(1,:) = T0*ones(N,1);
elseif coordtype==2
    T(1,:) = T0*ones(N,1);
else
    T(1,:) = T0*ones(N,1);
end

%% calculate element stiffness matrix and
% assemble global stiff. mat.
if coordtype==1
    A=1; % m^2
    Ke = A*k/dx*[1,-1;-1,1];
    Kh = h*A*[0 0; 0 1];
    K = zeros(N);
    % first, add K for last element
    K(N-1:N,N-1:N)=Kh;
    for i = 1:N-1
        K(i,i) = K(i,i)+ Ke(1,1);
        K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
        K(i,i+1) = Ke(1,2);
        K(i+1,i) = Ke(2,1);
    end
    m = c*rho*A*dx/6 * [2,1;1,2];
    M = zeros(N);
    for i = 1:N-1
        M(i,i) = M(i,i)+ m(1,1);
        M(i+1,i+1) = M(i+1,i+1) + m(2,2);
        M(i,i+1) = m(1,2);
        M(i+1,i) = m(2,1);
    end
elseif coordtype==2
    K = zeros(N);
    A=2*pi*x2*dz;
    % first, add K for last element
    % (terms are per unit height, dz)

```

```

Kh = 2*pi*x2*h*[0 0; 0 1];
K(N-1:N,N-1:N)=Kh;
for i = 1:N-1
    Ke = 2*pi*k*(xfea(i)+xfea(i+1))/(2*dx)*[1,-1;-1,1];
    K(i,i) = K(i,i) + Ke(1,1);
    K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
    K(i,i+1) = Ke(1,2);
    K(i+1,i) = Ke(2,1);
end
M = zeros(N);
for i = 1:N-1
    r1=xfea(i);
    r2=xfea(i+1);
    m(1,1) = 2*pi*c*rho*(r2-r1)*(r1/4+r2/12);
    m(1,2) = 2*pi*c*rho*(r2-r1)*(r1/12+r2/12);
    m(2,1) = m(1,2);
    m(2,2) = 2*pi*c*rho*(r2-r1)*(r1/12+r2/4);
    M(i,i) = M(i,i) + m(1,1);

    m(1,1) = 2*pi*c*rho*(r2-r1)^3*(r1/4+r2/12);
    m(1,2) = 2*pi*c*rho*(r2-r1)^3*(r1/12+r2/12);
    m(2,1) = m(1,2);
    m(2,2) = 2*pi*c*rho*(r2-r1)^3*(r1/12+r2/4);
    M(i,i) = M(i,i) + m(1,1);
    M(i+1,i+1) = M(i+1,i+1) + m(2,2);
    M(i,i+1) = M(i,i+1) + m(1,2);
    M(i+1,i) = M(i+1,i) + m(2,1);
end
else
    K = zeros(N);
    % first, add K for last element
    Kh = 4*pi*x2^2*h*[0 0; 0 1];
    K(N-1:N,N-1:N)=Kh;
    for i = 1:N-1
        Ke=4*pi*k*(xfea(i)^2+xfea(i)*xfea(i+1)+xfea(i+1)^2)/ ...
            (3*dx)*[1,-1;-1,1];
        K(i,i) = K(i,i) + Ke(1,1);
        K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
        K(i,i+1) = K(i,i+1) + Ke(1,2);
        K(i+1,i) = K(i+1,i) + Ke(2,1);
    end
    K;
    M = zeros(N);
    for i = 1:N-1
        r1=xfea(i);
        r2=xfea(i+1);
        m(1,1) = 4*pi*c*rho*(r2-r1)*(r1^2/5+r1*r2/10+r2^2/30);
        m(1,2) = 4*pi*c*rho*(-3*r1^5+5*r1^4*r2-5*r1*r2^4+...
            3*r2^5)/(60*(r2-r1)^2);
        m(2,1) = m(1,2);
        m(2,2) = 4*pi*c*rho*(r2-r1)*(r1^2/30+r1*r2/10+r2^2/5);
        M(i,i) = M(i,i) + m(1,1);
        M(i+1,i+1) = M(i+1,i+1) + m(2,2);
        M(i,i+1) = M(i,i+1) + m(1,2);
        M(i+1,i) = M(i+1,i) + m(2,1);
    end
    M;
end

%% calculate element force vector
% and assemble global force vector
if coord.type==1
    f = [0,0];
    F = zeros(N,1);
    F(N) = A*h*Tinf;
elseif coord.type==2

```

```

%           % Temp BC at inner and outer radius
%           T1=20;
%           T2=100;
%           F=zeros(N-2,1);
%           F(1)=-K(2,1)*T1;
%           F(N-2)=F(N-2)-K(N-1,N)*T2;
%           Kred=K(2:N-1,2:N-1);
%           Tred=Kred\F;
%           Tfea=[T1;Tred;T2];
f = [0,0];
F = zeros(N,1);
F(N) = A*h*Tinf;
else
    f = [0,0];
    F = zeros(N,1);
    F(N) = 4*pi*x2^2*h*Tinf;
end

%% calculate matrices for iteration time stepping
if coordtype==1
    dt=60;           % time step increment (s)
    % set beta (parameter for weighting explicit
    % and implicit calculation
    beta = .5;      % Crank-Nicholson: 0.5
    A1 = M/dt + beta*K;
    B = M/dt - (1-beta)*K; % same as A for Crank-Nicholson
    % solve for t_i (stored in matrix T(t,i)
    % with t timesteps and i nodes
    tp=zeros(20,1);
    tp(1)=0;
    for t = 1:(70*60)/dt-1
        tp(t+1)=tp(t)+dt;
        T(t+1,:) = A1\ (B * T(t,:) + F); % '
    end
elseif coordtype==2
    dt=1;           % time step increment (s)
    tmax=3600;      % final time (s)
    % set beta (parameter for weighting explicit
    % and implicit calculation
    beta = .5;      % Crank-Nicholson: 0.5
    A1 = M/dt + beta*K;
    B = M/dt - (1-beta)*K; % same as A
    % for Crank-Nicholson
    % solve for t_i (stored in matrix T(t,i)
    % with t timesteps and i nodes
    %
    tp=zeros(ceil(tmax/dt),1);
    tp(1)=0;
    for t = 1:tmax/dt
        tp(t+1)=tp(t)+dt;
        T(t+1,:) = A1\ (B * T(t,:) + F);
        disp(['Time. T1, T2 = ' num2str(tp(t)),...
' num2str(T(t+1,1)) ', ' num2str(T(t+1,end)) ])
    end

else
    dt=1;           % time step increment (s)
    % set beta (parameter for weighting explicit
    % and implicit calculation
    beta = .5;      % Crank-Nicholson: 0.5
    A1 = M/dt + beta*K;
    B = M/dt - (1-beta)*K; % same as A for Crank-Nicholson
    % solve for t_i (stored in matrix T(t,i)
    % with t timesteps and i nodes
    tp=zeros(1000/dt,1);
    tp(1)=0;

```

```

        for t = 1:1000/dt
            tp(t+1)=tp(t)+dt;
            T(t+1,:) = A1\ (B * T(t,:) + F); %'
        end
    end
end
T
%%
%% compare to exact
if coordtype==1
    exact=[0 20
            3.47 46.32
            6.93 53.30
            10.4 57.68
            13.87 60.85
            17.33 63.32
            20.80 65.33
            24.27 67.01
            27.72 68.45
            31.20 69.71
            34.67 70.82
            38.13 71.81
            41.60 72.72
            45.07 73.54
            48.53 74.31
            52.00 75.02
            55.47 75.69
            58.93 76.32
            62.40 76.92
            65.87 77.50
            69.33 78.05];
    t_exact=60*exact(:,1);
    T_exact=exact(:,2);
    h=figure;
    plot(tp,T(:,end),'.',t_exact,T_exact,'-')
    xlabel('Time (s)')
    ylabel('Temperature (C)')
    legend('FEA','Exact','Location','NorthWest')
    axis([0 4500 10 90])
elseif coordtype==2
    h=figure;
    exact=[0.          20.          20.
            100.         20.          40.4818
            200.         20.0093    46.8965
            300.         20.1234    51.2019
            400.         20.4915    54.4783
            500.         21.1787    57.1297
            600.         22.1691    59.3574
            700.         23.4109    61.2787
            800.         24.8466    62.9686
            900.         26.4244    64.4777
            1.E+03      28.0996    65.8445
            1.1E+03     29.8374    67.0965
            1.2E+03     31.6109    68.2544
            1.3E+03     33.3991    69.3345
            1.4E+03     35.1863    70.3492
            1.5E+03     36.9607    71.3082
            1.6E+03     38.7135    72.2192
            1.7E+03     40.4383    73.0881
            1.8E+03     42.1305    73.9196
            1.9E+03     43.787    74.7176
            2.E+03      45.4054    75.4851
            2.1E+03     46.9846    76.2246
            2.2E+03     48.5236    76.9383
            2.3E+03     50.0223    77.6278
            2.4E+03     51.4804    78.2943
            2.5E+03     52.8986    78.9394
            2.6E+03     54.2772    79.5641
            2.7E+03     55.617    80.1693
    ]
end

```

```

                2.8E+03          56.9187          80.7558
                2.9E+03          58.183          81.3242
                3.E+03           59.4108          81.8755
                3.1E+03          60.6031          82.4101
                3.2E+03          61.7608          82.9287
                3.3E+03          62.8848          83.4318
                3.4E+03          63.9758          83.9199
                3.5E+03          65.035          84.3934
                3.6E+03          66.0631          84.853    ];
t_exact=exact(:,1);
T_exact_inner=exact(:,2);
T_exact_outer=exact(:,3);
plot(tp,T(:,1),'b.',t_exact,T_exact_inner,'b-',...
      tp,T(:,end),'r.',t_exact,T_exact_outer,'r-')
xlabel('Time (s)')
ylabel('Temperature (C)')
legend('FEA Inner Center','Exact Inner Center',...
       'FEA Outer Surface','Exact Outer Surface',...
       'Location','NorthWest')
axis([0 3600 10 110])
else
h=figure;
for i=2:size(tp,1)
    if T(i-1,1)<70 && T(i,1)>=70
        t70=tp(i);
    end
end
disp([tp T(:,1)])
tp;
T;
plot(tp,T(:,1),'b.',tp,T(:,end),'r.')
xlabel('Time (s)')
ylabel('Temperature (C)')
legend('Center','Surface','Location','NorthWest')
text(500,20,['time step = ' num2str(dt)])
text(500,15,['time to reach 70 deg = ' num2str(t70) ' sec'])
axis([0 1000 0 110])
end
if coordtype==1
    filename='conduction_1D_convection_cartesian';
    title('Cartesian Coordinates - Mill''s problem')
elseif coordtype==2
    filename='conduction_1D_convection_cylindrical';
    title('Cylindrical Coordinates - Convection BC''s')
else
    filename='conduction_1D_convection_spherical';
    title('Spherical Coordinates - Boiling egg problem')
end
saveas(h,filename,'png');
end

% 1-D conduction with outer wall convection
clc; clear all; close all; format compact
set(groot,'defaulttextinterpreter','latex');
set(groot,'defaultAxesTickLabelInterpreter','latex');
set(groot,'defaultLegendInterpreter','latex');
for coordtype=1:3 % (1- Cartesian, 2-Cylindrical, 3- Spherical)
    clear T
    %% set constants
    if coordtype==1
        % PLA
        qA=5.; % Watt
        T0 = 20; % deg C
        k = 0.195; % W/m K
        c = 2060; % cp = J/kg K
    end
end

```

```

    rho = 1200; % kg/m^3
elseif coordtype==2
    qA=100000*(2*pi*.05*1.); % Watt (unit height in z-direction)
    T0 = 20; % deg C
    rho = 2600; % kg/m^3
    c = 800; % J/kg K
    k = 100; % W/m K
else
    qA=100000*(4*pi*.05^2); % Watt (unit height in z-direction)
    T0 = 20; % deg C
    rho = 2600; % kg/m^3
    c = 800; % J/kg K
    k = 100; % W/m K
end
%% define mesh
if coordtype==1
    % PLA "peg" geometry
    x1=0; % left node coordinate(m)
    x2=.006; % right node coordinate (m)
    L = x2-x1; % mesh length (m)
    N=31; % number of nodes;
    dx=L/(N-1); % element length (m)
    xfea=x1:dx:x2;
elseif coordtype==2
    x1=0.05; % left node coordinate(m)
    x2=.1; % right node coordinate (m)
    dz=1; % unit height in z-direction (m)
    L = x2-x1; % m
    N=21; % number of nodes;
    dx=L/(N-1); % element length (m)
    xfea=x1:dx:x2;
else
    %
    x1=0.05; % left node coordinate(m)
    x2=.1; % right node coordinate (m)
    L = x2-x1; % m
    N=21; % number of nodes;
    dx=L/(N-1); % element length (m)
    xfea=x1:dx:x2;
end

%% set Initial condition
if coordtype==1
    T(1,:) = T0*ones(N,1);
elseif coordtype==2
    T(1,:) = T0*ones(N,1);
else
    T(1,:) = T0*ones(N,1);
end

%% calculate element stiffness matrix
% and assemble global stiff. mat.
if coordtype==1
    A=pi*.001^2; % m^2
    Ke = A*k/dx*[1,-1;-1,1];
    K = zeros(N);
    for i = 1:N-1
        K(i,i) = K(i,i)+ Ke(1,1);
        K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
        K(i,i+1) = K(i,i+1) + Ke(1,2);
        K(i+1,i) = K(i+1,i) + Ke(2,1);
    end
    K;
    m = c*rho*A*dx/6 * [2,1;1,2];
    M = zeros(N);
    for i = 1:N-1

```

```

        M(i,i) = M(i,i)+ m(1,1);
        M(i+1,i+1) = M(i+1,i+1) + m(2,2);
        M(i,i+1) = M(i,i+1) + m(1,2);
        M(i+1,i) = M(i+1,i) + m(2,1);
    end
    M;
elseif coordtype==2
    K = zeros(N);
    A=2*pi*x2*dz;
    for i = 1:N-1
        Ke = 2*pi*k*(xfea(i)+xfea(i+1))/(2*dx)*[1,-1;-1,1];
        K(i,i) = K(i,i)+ Ke(1,1);
        K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
        K(i,i+1) = Ke(1,2);
        K(i+1,i) = Ke(2,1);
    end
    M = zeros(N);
    for i = 1:N-1
        r1=xfea(i);
        r2=xfea(i+1);
        m(1,1) = 2*pi*c*rho*(r2-r1)*(r1/4+r2/12);
        m(1,2) = 2*pi*c*rho*(r2-r1)*(r1/12+r2/12);
        m(2,1) = m(1,2);
        m(2,2) = 2*pi*c*rho*(r2-r1)*(r1/12+r2/4);
        M(i,i) = M(i,i)+ m(1,1);
        M(i+1,i+1) = M(i+1,i+1) + m(2,2);
        M(i,i+1) = M(i,i+1) + m(1,2);
        M(i+1,i) = M(i+1,i) + m(2,1);
    end
else
    K = zeros(N);
    for i = 1:N-1
        Ke=4*pi*k*(xfea(i)^2+xfea(i)*xfea(i+1)+...
        xfea(i+1)^2)/(3*dx)*[1,-1;-1,1];
        K(i,i) = K(i,i)+ Ke(1,1);
        K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
        K(i,i+1) = K(i,i+1) + Ke(1,2);
        K(i+1,i) = K(i+1,i) + Ke(2,1);
    end
    K;
    M = zeros(N);
    for i = 1:N-1
        r1=xfea(i);
        r2=xfea(i+1);
        m(1,1) = 4*pi*c*rho*(r2-r1)*(r1^2/5+r1*r2/10+r2^2/30);
        m(1,2) = 4*pi*c*rho*(-3*r1^5+5*r1^4*r2-5*r1*r2^4+...
        3*r2^5)/(60*(r2-r1)^2);
        m(2,1) = m(1,2);
        m(2,2) = 4*pi*c*rho*(r2-r1)*(r1^2/30+r1*r2/10+r2^2/5);
        M(i,i) = M(i,i)+ m(1,1);
        M(i+1,i+1) = M(i+1,i+1) + m(2,2);
        M(i,i+1) = M(i,i+1) + m(1,2);
        M(i+1,i) = M(i+1,i) + m(2,1);
    end
    M;
end

%% calculate element force vector and
assemble global force vector
if coordtype==1
    f = [0,0];
    F = zeros(N,1);
    F(1) = qA; % flux = (power (W) / area (m^2)) * area (m^2)
elseif coordtype==2
    f = [0,0];
    F = zeros(N,1);

```

```

    F(1) = qA;
else
    f = [0,0];
    F = zeros(N,1);
    F(1) = qA;
end

%% calculate matrices for iteration time stepping
if coordtype==1

    %% set temperature BCs solve equations
    dt=.02;      % time step increment (s)
    tmax=2;      % final time (s)
    % set beta (parameter for weighting explicit
    and implicit calculation
    beta = .5; % Crank-Nicholson: 0.5
    A1 = M/dt + beta*K;
    B = M/dt - (1-beta)*K; % same as A for Crank-Nicholson
    % solve for t_i (stored in matrix T(t,i)
    with t timesteps and i nodes
    tp=zeros(floor(tmax/dt),1);
    tp(1)=0;
    for t = 1:floor(tmax/dt)
        tp(t+1)=tp(t)+dt;
        T(t+1,:) = A1\ (B * T(t,:) + F); %'
    end
elseif coordtype==2
    dt=.02;      % time step increment (s)
    tmax=10;     % final time (s)
    % set beta (parameter for weighting
    explicit and implicit calculation
    beta = .5; % Crank-Nicholson: 0.5
    A1 = M/dt + beta*K;
    B = M/dt - (1-beta)*K; % same as A for Crank-Nicholson
    % solve for t_i (stored in matrix T(t,i)
    with t timesteps and i nodes
    tp=zeros(floor(tmax/dt),1);
    tp(1)=0;
    for t = 1:floor(tmax/dt)
        tp(t+1)=tp(t)+dt;
        T(t+1,:) = A1\ (B * T(t,:) + F); %'
    end
else
    dt=.01;      % time step increment (s)
    tmax=10;     % final time (s)
    % set beta (parameter for weighting
    explicit and implicit calculation
    beta = .5; % Crank-Nicholson: 0.5
    A1 = M/dt + beta*K;
    B = M/dt - (1-beta)*K; % same as A for Crank-Nicholson
    % solve for t_i (stored in matrix T(t,i)
    with t timesteps and i nodes
    tp=zeros(floor(tmax/dt),1);
    tp(1)=0;
    for t = 1:floor(tmax/dt)
        tp(t+1)=tp(t)+dt;
        T(t+1,:) = A1\ (B * T(t,:) + F); %'
    end
end
T;
%% compare to exact
if coordtype==1
    % exact (Abaqus FEA)
    exact=[0.          20.          20.

```


10.E-03	20.	138.526
20.E-03	20.	241.211
30.E-03	20.	331.23
40.E-03	20.	411.05
50.E-03	20.	482.598
60.E-03	20.	547.382
70.E-03	20.	606.594
80.E-03	20.	661.174
90.E-03	20.	711.873
100.E-03	20.	759.291
110.E-03	20.	803.91
120.E-03	20.	846.124
130.E-03	20.	886.252
140.E-03	20.	924.555
150.E-03	20.	961.253
160.E-03	20.	996.524
170.E-03	20.	1.03052E+03
180.E-03	20.	1.06337E+03
190.E-03	20.	1.09519E+03
200.E-03	20.	1.12606E+03
210.E-03	20.	1.15607E+03
220.E-03	20.	1.18528E+03
230.E-03	20.	1.21376E+03
240.E-03	20.	1.24157E+03
250.E-03	20.	1.26874E+03
260.E-03	20.	1.29532E+03
270.E-03	20.	1.32135E+03
280.E-03	20.	1.34687E+03
290.E-03	20.	1.37189E+03
300.E-03	20.	1.39646E+03
310.E-03	20.	1.42058E+03
320.E-03	20.	1.4443E+03
330.E-03	20.	1.46762E+03
340.E-03	20.	1.49057E+03
350.E-03	20.	1.51317E+03
360.E-03	20.	1.53543E+03
370.E-03	20.	1.55736E+03
380.E-03	20.	1.57898E+03
390.E-03	20.	1.6003E+03
400.E-03	20.	1.62134E+03
410.E-03	20.	1.6421E+03
420.E-03	20.	1.6626E+03
430.E-03	20.	1.68285E+03
440.E-03	20.	1.70285E+03
450.E-03	20.	1.72262E+03
460.E-03	20.	1.74216E+03
470.E-03	20.	1.76148E+03
480.E-03	20.	1.78058E+03
490.E-03	20.	1.79948E+03
500.E-03	20.	1.81818E+03
510.E-03	20.	1.83669E+03
520.E-03	20.	1.85501E+03
530.E-03	20.	1.87315E+03
540.E-03	20.	1.89111E+03
550.E-03	20.	1.9089E+03
560.E-03	20.	1.92653E+03
570.E-03	20.	1.94399E+03
580.E-03	20.	1.9613E+03
590.E-03	20.	1.97845E+03
600.E-03	20.	1.99545E+03
610.E-03	20.	2.01231E+03
620.E-03	20.	2.02903E+03
630.E-03	20.	2.0456E+03
640.E-03	20.	2.06205E+03
650.E-03	20.	2.07836E+03
660.E-03	20.	2.09454E+03
670.E-03	20.	2.1106E+03
680.E-03	20.	2.12654E+03

690.E-03	20.	2.14235E+03
700.E-03	20.	2.15805E+03
710.E-03	20.	2.17363E+03
720.E-03	20.	2.18911E+03
730.E-03	20.	2.20447E+03
740.E-03	20.	2.21972E+03
750.E-03	20.	2.23487E+03
760.E-03	20.	2.24992E+03
770.E-03	20.	2.26486E+03
780.E-03	20.	2.27971E+03
790.E-03	20.	2.29446E+03
800.E-03	20.	2.30911E+03
810.E-03	20.	2.32367E+03
820.E-03	20.	2.33814E+03
830.E-03	20.	2.35252E+03
840.E-03	20.	2.36681E+03
850.E-03	20.	2.38102E+03
860.E-03	20.	2.39514E+03
870.E-03	20.	2.40918E+03
880.E-03	20.	2.42313E+03
890.E-03	20.	2.437E+03
900.E-03	20.	2.4508E+03
910.E-03	20.	2.46451E+03
920.E-03	20.	2.47815E+03
930.E-03	20.	2.49172E+03
940.E-03	20.	2.50521E+03
950.E-03	20.	2.51863E+03
960.E-03	20.	2.53197E+03
970.E-03	20.	2.54525E+03
980.E-03	20.	2.55845E+03
990.E-03	20.	2.57159E+03
1.	20.	2.58466E+03
1.01	20.	2.59766E+03
1.02	20.	2.6106E+03
1.03	20.	2.62348E+03
1.04	20.	2.63629E+03
1.05	20.	2.64904E+03
1.06	20.	2.66172E+03
1.07	20.	2.67435E+03
1.08	20.	2.68692E+03
1.09	20.	2.69942E+03
1.1	20.	2.71187E+03
1.11	20.	2.72426E+03
1.12	20.	2.7366E+03
1.13	20.	2.74888E+03
1.14	20.	2.7611E+03
1.15	20.	2.77327E+03
1.16	20.	2.78539E+03
1.17	20.	2.79745E+03
1.18	20.	2.80946E+03
1.19	20.	2.82142E+03
1.2	20.	2.83333E+03
1.21	20.	2.84519E+03
1.22	20.	2.857E+03
1.23	20.	2.86876E+03
1.24	20.	2.88047E+03
1.25	20.	2.89214E+03
1.26	20.	2.90376E+03
1.27	20.	2.91533E+03
1.28	20.	2.92685E+03
1.29	20.	2.93833E+03
1.3	20.	2.94976E+03
1.31	20.	2.96115E+03
1.32	20.	2.9725E+03
1.33	20.	2.9838E+03
1.34	20.	2.99506E+03
1.35	20.	3.00627E+03
1.36	20.	3.01745E+03

1.37	20.	3.02858E+03
1.38	20.	3.03967E+03
1.39	20.	3.05073E+03
1.4	20.	3.06174E+03
1.41	20.	3.07271E+03
1.42	20.	3.08364E+03
1.43	20.	3.09453E+03
1.44	20.	3.10539E+03
1.45	20.	3.1162E+03
1.46	20.	3.12698E+03
1.47	20.	3.13773E+03
1.48	20.	3.14843E+03
1.49	20.	3.1591E+03
1.5	20.	3.16973E+03
1.51	20.	3.18033E+03
1.52	20.	3.19089E+03
1.53	20.	3.20141E+03
1.54	20.	3.21191E+03
1.55	20.	3.22236E+03
1.56	20.	3.23279E+03
1.57	20.	3.24317E+03
1.58	20.	3.25353E+03
1.59	20.	3.26385E+03
1.6	20.	3.27414E+03
1.61	20.	3.2844E+03
1.62	20.	3.29463E+03
1.63	20.	3.30482E+03
1.64	20.	3.31498E+03
1.65	20.	3.32511E+03
1.66	20.	3.33521E+03
1.67	20.	3.34528E+03
1.68	20.	3.35532E+03
1.69	20.	3.36533E+03
1.7	20.	3.37531E+03
1.71	20.	3.38526E+03
1.72	20.	3.39518E+03
1.73	20.	3.40507E+03
1.74	20.	3.41493E+03
1.75	20.	3.42476E+03
1.76	20.	3.43457E+03
1.77	20.	3.44434E+03
1.78	20.	3.45409E+03
1.79	20.	3.46381E+03
1.8	20.	3.47351E+03
1.81	20.	3.48317E+03
1.82	20.	3.49281E+03
1.83	20.	3.50243E+03
1.84	20.	3.51201E+03
1.85	20.	3.52158E+03
1.86	20.	3.53111E+03
1.87	20.	3.54062E+03
1.88	20.	3.5501E+03
1.89	20.	3.55956E+03
1.9	20.	3.56899E+03
1.91	20.	3.5784E+03
1.92	20.	3.58778E+03
1.93	20.	3.59714E+03
1.94	20.	3.60647E+03
1.95	20.	3.61578E+03
1.96	20.	3.62507E+03
1.97	20.	3.63433E+03
1.98	20.	3.64357E+03
1.99	20.	3.65278E+03
2.	20.	3.66197E+03];

t_exact=exact(:,1);
T1_exact=exact(:,2);
T2_exact=exact(:,3);

```

h=figure;
plot(tp,T(:,1),'.',t_exact,T2_exact,'-')
xlabel('Time (s)')
ylabel('Temperature (C)')
legend('FEA (x=0)', 'Exact (x=0)', 'Location', 'NorthWest')
axis([0 2 0 4000])
%
h=figure;
plot(tp,T(:,end),'.')
xlabel('Time (s)')
ylabel('Temperature (C)')
text(2,500,['left/top final temp = ...
' num2str(T(end,1),'%s')])
legend('FEA right/bottom edge',...
'Location', 'NorthWest')
elseif coordtype==2
h=figure;
% exact (Abaqus FEA)
exact=[
500.E-03      0.      25.2754      20.      20.
1.      27.357      20.
1.5      28.9064      20.0002
2.      30.1827      20.0017
2.5      31.2857      20.0079
3.      32.2661      20.023
3.5      33.1541      20.0511
4.      33.9694      20.0952
4.5      34.7253      20.1571
5.      35.432      20.2374
5.5      36.0967      20.3363
6.      36.7253      20.4532
6.5      37.3224      20.5873
7.      37.8918      20.7375
7.5      38.4368      20.9027
8.      38.9599      21.0819
8.5      39.4635      21.2738
9.      39.9496      21.4775
9.5      40.4199      21.6919
10.      40.8761      21.9162 ];

t_exact=exact(:,1);
T_exact_inner=exact(:,2);
T_exact_outer=exact(:,3);
plot(tp,T(:,1),'b.',t_exact,T_exact_inner,'b-', ...
tp,T(:,end),'r.',t_exact,T_exact_outer,'r-')
xlabel('Time (s)')
ylabel('Temperature (C)')
legend('FEA Inner Surface', 'Exact Inner Surface', ...
'FEA Outer Surface', ...
'Exact Outer Surface', 'Location', 'NorthWest')
%
else
h=figure;
% exact (Abaqus FEA)
exact=[ 0.      20.
100.E-03      21.4997      20.
200.E-03      22.5778      20.
300.E-03      23.4033      20.
400.E-03      24.0698      20.
500.E-03      24.6311      20.
600.E-03      25.1191      20.
700.E-03      25.5537      20.
800.E-03      25.9476      20.
900.E-03      26.3093      20.
1.      26.6448      20.
1.1      26.9585      20.
1.2      27.2536      20.0001
1.3      27.5328      20.0001

```

1.4	27.7979	20.0002
1.5	28.0507	20.0003
1.6	28.2924	20.0005
1.7	28.5241	20.0007
1.8	28.7468	20.001
1.9	28.9613	20.0014
2.	29.1683	20.0019
2.1	29.3683	20.0026
2.2	29.562	20.0034
2.3	29.7497	20.0044
2.4	29.9318	20.0057
2.5	30.1088	20.0071
2.6	30.281	20.0088
2.7	30.4486	20.0108
2.8	30.6119	20.0131
2.9	30.7712	20.0156
3.	30.9267	20.0185
3.1	31.0786	20.0218
3.2	31.227	20.0254
3.3	31.3722	20.0294
3.4	31.5143	20.0339
3.5	31.6535	20.0387
3.6	31.7898	20.0439
3.7	31.9235	20.0496
3.8	32.0545	20.0557
3.9	32.1831	20.0623
4.	32.3093	20.0694
4.1	32.4333	20.0769
4.2	32.5551	20.0849
4.3	32.6748	20.0933
4.4	32.7924	20.1023
4.5	32.9081	20.1117
4.6	33.0219	20.1216
4.7	33.134	20.132
4.8	33.2442	20.1429
4.9	33.3528	20.1543
5.	33.4598	20.1661
5.1	33.5651	20.1785
5.2	33.669	20.1913
5.3	33.7713	20.2046
5.4	33.8722	20.2184
5.5	33.9717	20.2326
5.6	34.0699	20.2474
5.7	34.1668	20.2626
5.8	34.2623	20.2782
5.9	34.3567	20.2943
6.	34.4498	20.3109
6.1	34.5418	20.3279
6.2	34.6326	20.3454
6.3	34.7224	20.3633
6.4	34.811	20.3816
6.5	34.8986	20.4004
6.6	34.9852	20.4195
6.7	35.0708	20.4391
6.8	35.1554	20.4591
6.9	35.2391	20.4795
7.	35.3218	20.5003
7.1	35.4037	20.5215
7.2	35.4846	20.5431
7.3	35.5648	20.565
7.4	35.644	20.5873
7.5	35.7225	20.61
7.6	35.8002	20.6331
7.7	35.8771	20.6565
7.8	35.9532	20.6802
7.9	36.0286	20.7043
8.	36.1033	20.7287
8.1	36.1773	20.7535

8.2	36.2506	20.7785
8.3	36.3232	20.8039
8.4	36.3951	20.8296
8.5	36.4665	20.8557
8.6	36.5371	20.882
8.7	36.6072	20.9086
8.8	36.6767	20.9355
8.9	36.7455	20.9627
9.	36.8138	20.9902
9.1	36.8816	21.0179
9.2	36.9487	21.0459
9.3	37.0154	21.0742
9.4	37.0815	21.1027
9.5	37.1471	21.1315
9.6	37.2122	21.1605
9.7	37.2768	21.1898
9.8	37.3409	21.2194
9.9	37.4046	21.2491
10.	37.4677	21.2791

```

];
t_exact=exact(:,1);
T_exact_inner=exact(:,2);
T_exact_outer=exact(:,3);
plot(tp,T(:,1),'b.',t_exact,T_exact_inner,'b-', ...
      tp,T(:,end),'r.',t_exact,T_exact_outer,'r-')
xlabel('Time (s)')
ylabel('Temperature (C)')
legend('FEA Inner Surface',...
       'Exact Inner Surface','FEA Outer Surface',...
       'Exact Outer Surface','Location','NorthWest')
axis([0 10 18 38])
end
if coordtype==1
    filename='conduction_1D_heat_flux_cartesian';
    title('Cartesian Coordinates - Heat Flux BC''s')
elseif coordtype==2
    filename='conduction_1D_heat_flux_cylindrical';
    title('Cylindrical Coordinates - Heat Flux BC''s')
else
    filename='conduction_1D_heat_flux_spherical';
    title('Spherical Coordinates - Heat Flux BC''s')
end
saveas(h,filename,'png');
end

```

APPENDIX D

Matlab script for finite difference transient convection problem

```
clc; clear; %close all; format compact
%
h=40;
k=1;
c=800;
rho=2600;
alpha=k/(rho*c);
L=.08; % 8 cm
%
nnode=41;
dx=L/(nnode-1);
Bi=h*dx/k
Fo_max=1/(2*(1+Bi))
Fo=.4
%
% Fo=0.25;
% Bi=0.8;
%
Te=100;
dt=Fo*dx^2/alpha
%
t=0;
T=20*ones(1,nnode);
while t<3600
    t=t+dt;
    Tnew(1)=2*Fo*(T(2)+Bi*Te)+(1-2*Fo-2*Fo*Bi)*T(1);
    for i=2:nnode-1
        Tnew(i)=(1-2*Fo)*T(i)+Fo*(T(i-1)+T(i+1));
    end
    Tnew(nnode)=2*Fo*T(nnode-1)+(1-2*Fo)*T(nnode);
    T=Tnew;
    disp(['t_min, T = ' num2str(t/60,3) ' ' num2str(T,4)])
end
%
x=linspace(0,L,nnode);
figure
plot(x,T,'-')
xlabel('x')
ylabel('T')
%
% Abaqus FEA
%
fea=[    0.                76.2645
      2.E-03             74.3786
      4.E-03             72.5206
      6.E-03             70.6926
      8.E-03             68.8963
     10.E-03             67.1337
     12.E-03             65.4064
     14.E-03             63.7162
     16.E-03             62.0646
     18.E-03             60.4532
     20.E-03             58.8832
     22.E-03             57.3561
     24.E-03             55.8731
     26.E-03             54.4352
     28.E-03             53.0437
     30.E-03             51.6994
```

```

32.E-03          50.4033
34.E-03          49.1561
36.E-03          47.9586
38.E-03          46.8114
40.E-03          45.7152
42.E-03          44.6705
44.E-03          43.6776
46.E-03          42.7371
48.E-03          41.8492
50.E-03          41.0143
52.E-03          40.2325
54.E-03          39.5042
56.E-03          38.8294
58.E-03          38.2083
60.E-03          37.641
62.E-03          37.1276
64.E-03          36.6681
66.E-03          36.2627
68.E-03          35.9113
70.E-03          35.6139
72.E-03          35.3706
74.E-03          35.1813
76.E-03          35.0461
78.E-03          34.965
80.E-03          34.938] ;
x_fea=fea(:,1);
T_fea=fea(:,2);
hold on
plot(x_fea,T_fea,'r*')
legend('Finite Diff','Kaosi ist der Beste', 'Abaqus FEA')
title('Temperature distribution after 1 hour')

```


APPENDIX E

Matlab script for finite element transient convection problem

```
clc
clear all
format compact
close all

%% set constants
Tinf = 100; %deg C
h = 40; %W/m^2 K
T0 = 20; %deg C
rho = 2600; %kg/m^3
c = 800; %J/kg K
k = 1; %W/m K
% dx = 0.02; %m
L = 0.08; %m
Nnode=5; % 51;
dx=L/(Nnode-1)

%% calculate therm. diffus., Biot and Fourier nr.
% a = k / (rho * c); %thermal diffusivity
%
% Bi = h * dx / k %Biot number
% FoMax = 1 / (2 + 2*Bi) %Maximum Fourier number for stability
%
% Fo = 0.25; %set to .25 arbitrarily
% if Fo > FoMax
%     disp("Choose a lower Fourier number")
% end

%% determine time step
dt=60;

% dt = Fo * dx^2 / a;

%% calculate element stiffness matrix and assemble global stiff. mat.
A = 1; %area of slab similar to ex. 13.3
% in logans textbook for 1d problem
h*A*[1 0; 0 0]

K1 = A*k/dx*[1,-1;-1,1]+h*A*[1 0; 0 0]
K2 = A*k/dx*[1,-1;-1,1]
K = zeros(Nnode);
K(1:2,1:2)=K1;
for i = 2:Nnode-1
    K(i,i) = K(i,i)+ K2(1,1);
    K(i+1,i+1) = K(i+1,i+1) + K2(2,2);
    K(i,i+1) = K2(1,2);
    K(i+1,i) = K2(2,1);
end
K;

%% calculate element force vector and assemble global force vector
f = [0,0];
F = zeros(Nnode,1);
% for i = 1:4
```

```

%      F(i) = F(i) + f(1);
%      F(i+1) = F(i+1) +f(2);
% end

F(1) = A*h*Tinf;

F
%% calculate element mass capacitance matrix
% and assemble capac. matrix

% m = c*rho*A*L/6 * [2,1;1,2];
m = c*rho*A*dx/6 * [2,1;1,2];

M = zeros(Nnode);
for i = 1:Nnode-1
    M(i,i) = M(i,i)+ m(1,1);
    M(i+1,i+1) = M(i+1,i+1) + m(2,2);
    M(i,i+1) = m(1,2);
    M(i+1,i) = m(2,1);
end
M

%% calculate matrices for iteration

% set beta (parameter for weighting explicit and implicit calculation
beta = .5 % Crank-Nicholson: 0.5

A1 = M/dt + beta*K
B = M/dt - (1-beta)*K % same as A for Crank-Nicholson

% %solve for t_i (stored in matrix T(t,i)
with t timesteps and i nodes

% T(1,:) = A1\ (B * T0*ones(Nnode,1) + F);
T(1,:) = T0*ones(Nnode,1);

tp=zeros(20,1);
tp(1)=0;
for t = 1:(70*60)/dt-1
    tp(t+1)=tp(t)+dt;
    T(t+1,:) = A1\ (B * T(t,:) + F);
end

% T(1,:) = A1\B * T0*[1;1;1;1;1] + F;
%
% for t = 1:10
%     T(t+1,:) = A1\B * T(t,:) + F;
% end

[tp T(:,1:5)]

exact=[0 20
3.47 46.32
6.93 53.30
10.4 57.68
13.87 60.85
17.33 63.32
20.80 65.33
24.27 67.01
27.72 68.45
31.20 69.71
34.67 70.82
38.13 71.81
41.60 72.72
45.07 73.54

```

```
48.53 74.31
52.00 75.02
55.47 75.69
58.93 76.32
62.40 76.92
65.87 77.50
69.33 78.05];

t_exact=60*exact(:,1);
T_exact=exact(:,2);

plot(tp,T(:,1),'.',t_exact,T_exact,'*')
xlabel('Time (s)')
ylabel('Temperature (C)')
legend('FEA','Exact','Location','NorthWest')
```

APPENDIX F

Matlab scripts for chapter 5 heat transfer problems

F.1 Matlab script for 1-dimensional finite element analysis of insulated rod cooling

```
clc
clear all
%% define const.

Tinf = 10; %deg C
T0 = 100; %deg C
h = 40; %W/m^2 K
Kxx = 0.195; %W/m K

%% calculate element stiffness matrix and assemble global stiff. mat.
A = pi/144; %area in m^2
L = 10/12; %length m
K1 = A*Kxx/L*[1,-1;-1,1];
K = zeros(5);
for i = 1:4
    K(i,i) = K(i,i)+ K1(1,1);
    K(i+1,i+1) = K(i+1,i+1) + K1(2,2);
    K(i,i+1) = K1(1,2);
    K(i+1,i) = K1(2,1);
end

K(5,5) = K(5,5) + h*A

%% calculate element force vector and assemble global force vector
f = [0,0];
F = zeros(5,1);
for i = 1:4
    F(i) = F(i) + f(1);
    F(i+1) = F(i+1) +f(2);
end

F(5) = A*h*Tinf;

%% solve system of equations K*t = F using boundary conditions
K(1,1) = 1;
F(1) = 100;
F(2) = -K(1,2) * F(1);
K(1,2) = 0;
K(2,1) = 0;

t = K \ F
```

F.2 Matlab script for 1-dimensional finite element analysis of rod cooling with free convection

```
clc
clear all
%% define const.

Tinf = 20; %deg F
T0 = 200; %deg F
h = 1; %Btu / (h ft^2 deg F)
Kxx = 3; %Btu / (h ft^2 deg F)
r = 2; %in
%% calculate element stiffness matrix and assemble global stiff. mat.
A = r^2*pi; %area in in^2
P = 2*pi*r; %perimeter in in
L = 3;
K1 = A*Kxx/L*[1,-1;-1,1] + h*P*L/6*[2,1;1,2];
K = zeros(4);
for i = 1:3
    K(i,i) = K(i,i) + K1(1,1);
    K(i+1,i+1) = K(i+1,i+1) + K1(2,2);
    K(i,i+1) = K1(1,2);
    K(i+1,i) = K1(2,1);
end
K(4,4) = K(4,4) + h*A

%% calculate element force vector and assemble global force vector
f = h*Tinf*P*L/2*[1,1];
F = zeros(4,1);
for i = 1:3
    F(i) = F(i) + f(1);
    F(i+1) = F(i+1) + f(2);
end
F(4) = F(4) + h*Tinf*A;

%% solve system of equations K*t = F for t_2 to t_4
F(2) = 160*4*pi;
K(2:end,2:end) \ F(2:end)
```

F.3 Matlab script for 1-dimensional finite element analysis of transient fin

```
clc
clear all

%% set constants

Tinf = 25; %deg C
h = 150; %W/m^2 K
T0 = 25; %deg C
rho = 8900; %kg/m^3
c = 375; %J/kg K
k = 400; %W/m K
L = 0.02; %m
dx = L/2; %m
T1=85; % deg C

% Tinf = 100; %deg C
% h = 40; %W/m^2 K
% T0 = 20; %deg C
% rho = 2600; %kg/m^3
% c = 800; %J/kg K
```

```

% k = 1; %W/m K
% dx = 0.02; %m
% L = 0.08; %m

%% calculate therm. diffus., Biot and Fourier nr.

% a = k / (rho * c); %thermal diffusivity
%
% Bi = h * dx / k %Biot number
% FoMax = 1 / (2 + 2*Bi) %Maximum Fourier number for stability
%
% Fo = 0.25; %set to .25 arbitrarily
% if Fo > FoMax
%     disp("Choose a lower Fourier number")
% end

%% determine time step

% dt = Fo * dx^2 / a;

%% calculate element stiffness matrix and assemble global stiff. mat.
A = pi*.002^2; %area of slab similar to
% ex. 13.3 in logans textbook for 1d problem
P=2*pi*.002; % perimeter

K1 = A*k/dx*[1,-1;-1,1]+(h*P*dx/6)*[2 1; 1 2];
K = zeros(3);
for i = 1:2
    K(i,i) = K(i,i)+ K1(1,1);
    K(i+1,i+1) = K(i+1,i+1) + K1(2,2);
    K(i,i+1) = K1(1,2);
    K(i+1,i) = K1(2,1);
end
K

% A = 1; %area of slab similar to ex. 13.3
% in logans textbook for 1d problem
%
% K1 = A*k/dx*[1,-1;-1,1];
% K = zeros(5);
% for i = 1:4
%     K(i,i) = K(i,i)+ K1(1,1);
%     K(i+1,i+1) = K(i+1,i+1) + K1(2,2);
%     K(i,i+1) = K1(1,2);
%     K(i+1,i) = K1(2,1);
% end
% K

%% calculate element force vector and assemble global force vector

f=(h*Tinf*P*dx/2)*[1;1];
F = zeros(3,1);
for i = 1:2
    F(i) = F(i) + f(1);
    F(i+1) = F(i+1) +f(2);
end
F

% f = [0,0];
%
% F = zeros(5,1);
% for i = 1:4
%     F(i) = F(i) + f(1);
%     F(i+1) = F(i+1) +f(2);
% end
%
% F(1) = A*h*Tinf

```

```

%% calculate element mass capacitance
% matrix and assemble capac. matrix

m = c*rho*A*dx/6 * [2,1;1,2];
M = zeros(3);
for i = 1:2
    M(i,i) = M(i,i) + m(1,1);
    M(i+1,i+1) = M(i+1,i+1) + m(2,2);
    M(i,i+1) = m(1,2);
    M(i+1,i) = m(2,1);
end
M

% m = c*rho*A*L/6 * [2,1;1,2];
% M = zeros(5);
% for i = 1:4
%     M(i,i) = M(i,i) + m(1,1);
%     M(i+1,i+1) = M(i+1,i+1) + m(2,2);
%     M(i,i+1) = m(1,2);
%     M(i+1,i) = m(2,1);
% end
% M

%% calculate matrices for iteration

dt=0.1;

% set beta (parameter for weighting explicit and implicit calculation
beta=2/3;

A1 = M/dt + beta*K
B = M/dt - (1-beta)*K % same as A for Crank-Nicholson

Alp=A1(2:3,2:3)
Bp=B(2:3,2:3)
% solve for t_i (stored in matrix T(t,i)
% with t timesteps and i nodes

Alp\Bp * T0*[1;1]
Fp=[F(2);F(3)]
[B(2,1);B(3,1)]*T1
[A1(2,1);A1(3,1)]*T1
T(1,:) = Alp\(Bp * T0*[1;1] + Fp + ...
[B(2,1);B(3,1)]*T0 - [A1(2,1);A1(3,1)]*T1)
tp=zeros(20,1)
tp(1)=dt

for t = 1:29
    tp(t+1)=tp(t)+dt
    T(t+1,:) = Alp\(Bp * T(t,:) + Fp + ...
+ Fp + [B(2,1);B(3,1)]*T1 - [A1(2,1);A1(3,1)]*T1);
end

[tp T]

plot(tp,T(:,1),'-',tp,T(:,2),'-')
xlabel('time')
ylabel('temperature')
legend('Node 2','Node 3')

% % set beta (parameter for weighting
% explicit and implicit calculation
%
% beta = 0.7; % Crank-Nicholson: 0.5
%
% A1 = M/dt + beta*K

```

```

% B = M/dt - (1-beta)*K % same as A for Crank-Nicholson
%
% %solve for t_i (stored in matrix T(t,i)
%with t timesteps and i nodes
% T(1,:) = A1\B * T0*[1;1;1;1;1] + F;
%
% for t = 1:10
%     T(t+1,:) = A1\B * T(t,:) + F;
% end
%
```


APPENDIX G

Matlab script for 1-dimensional transient finite element problem with phase change

```
function melting
% temperature BC (200 C) at x=0
clc; clear all; close all
%% set constants

T0 = 20; % deg C (initial condition)
T1 = 200; % deg C (left end BC)
k = 0.195; %W/m K
c = 2060; % = cp J/kg K
rho = 1200; %kg/m^3
hfs =3e6*rho/10; % latent heat of melting per deg C
% (J/kg)*(kg/m^3)(1/s) = W/m^3

dt=.01; % time step increment (s)
tmax=100; % final time (s)

r = 1e-3; %radius of probe in m
A = pi*r^2; %area of top of pin
L = 6e-3; % height of probe in m
Nnode = 101; %
dx = L/(Nnode-1);
x=linspace(0,L,Nnode);

TL = 160;
TS = 150;

%% calculate element stiffness matrix and assemble global stiff. mat.
K2 = A*k/dx*[1,-1;-1,1];
K = zeros(Nnode);
% for i = 2:Nnode-1
for i = 1:Nnode-1
    K(i,i) = K(i,i)+ K2(1,1);
    K(i+1,i+1) = K(i+1,i+1) + K2(2,2);
    K(i,i+1) = K2(1,2);
    K(i+1,i) = K2(2,1);
end
K;

%% set beta (parameter for weighting explicit and implicit calculation
beta = .5;

%% calculate element mass capacitance matrix and assemble capac. matrix
m = c*rho*A*dx/6 *[2,1;1,2];
M = zeros(Nnode);
for i = 1:Nnode-1
    M(i,i) = M(i,i)+ m(1,1);
    M(i+1,i+1) = M(i+1,i+1) + m(2,2);
    M(i,i+1) = m(1,2);
    M(i+1,i) = m(2,1);
end
M;

%% calculate matrices for iteration
A1 = M/dt + beta*K;
```

```

% size(A1)
B = M/dt - (1-beta)*K; % same as A1 for Crank-Nicholson
% size(B)

%% iterate for each timestep while updating F
T(1,:) = T0*ones(Nnode,1);

tp=zeros(tmax/dt,1);
tp(1)=0;

for time_step=1:tmax/dt % t = dt:dt:tmax
    % disp(['t, step = ' num2str([t,time_step])]);
    F = zeros(Nnode,1);
    f_type=zeros(Nnode-1,1);
    tp(time_step+1)=tp(time_step)+dt;

    for i = 1:Nnode-1
        [fnew,ftype] = fMelting(TL,TS,T(time_step,i),...
            T(time_step,i+1),dx,dt,A,hfs,rho);
        % fnew=[0;0]; % for testing no melting
        f_type(i)=ftype;
        F(i) = F(i)+fnew(1);
        F(i+1) = F(i+1)+fnew(2);
    end
    % modify equations to impose BC at x=0
    Fred=zeros(Nnode-1,1);
    Fred(1)=Fred(1)+B(2,1)*T1-A1(2,1)*T1;
    Fred(2:Nnode-1)=F(3:Nnode);
    Alred=A1(2:Nnode,2:Nnode);
    Bred=B(2:Nnode,2:Nnode);
    Tred_prev=T(time_step,2:Nnode);

    Tred=Alred\ (Bred * Tred_prev' + Fred);
    T(time_step+1,1) = T1;
    T(time_step+1,2:Nnode) = Tred;

    t_plot=tp(time_step+1);

    if abs(t_plot-10)<dt/10
        figure(1)
        t_plot;
        min_T=min(T(time_step+1,:));
        disp(['tplot, min-T= ' num2str([t_plot,min-T])]);
        plot(x,T(time_step+1,:), 'r*-')
        hold on
    elseif abs(t_plot-50)<dt/10
        figure(1)
        t_plot;
        min_T=min(T(time_step+1,:));
        disp(['tplot, min-T= ' num2str([t_plot,min-T])]);
        plot(x,T(time_step+1,:), 'g*-')
    elseif abs(t_plot-100)<dt/10
        figure(1)
        t_plot;
        min_T=min(T(time_step+1,:));
        disp(['tplot, min-T= ' num2str([t_plot,min-T])]);
        plot(x,T(time_step+1,:), 'b*-')
    end
end
end
hold on
plot_exact_soln

% Compaare to Abaqus solutions

function plot_exact_soln
%
```

```

% Abaqus case with melting (LH=3e6) - Table labels:
%   x, T(10 sec), T(50 sec), T(100 sec)
%

```

```

a=[  0.          200.          200.          200.
60.E-06      184.634      192.964      194.972
120.E-06      169.29       185.931      189.945
180.E-06      153.99       178.903      184.919
240.E-06      148.216      171.882      179.896
300.E-06      142.517      164.871      174.877
360.E-06      136.9        157.872      169.861
420.E-06      131.376      153.013      164.851
480.E-06      125.953      150.054      159.846
540.E-06      120.639      147.548      155.809
600.E-06      115.443      145.047      152.716
660.E-06      110.37       142.553      150.404
720.E-06      105.429      140.067      148.692
780.E-06      100.627      137.592      146.985
840.E-06       95.9677      135.129      145.283
900.E-06       91.4576      132.681      143.586
960.E-06       87.101      130.248      141.894
1.02E-03      82.9018      127.832      140.21
1.08E-03      78.8631      125.435      138.532
1.14E-03      74.9871      123.058      136.861
1.2E-03       71.2756      120.702      135.198
1.26E-03      67.7295      118.368      133.543
1.32E-03      64.349      116.057      131.896
1.38E-03      61.1336      113.77       130.259
1.44E-03      58.0821      111.508      128.632
1.5E-03       55.1927      109.272      127.015
1.56E-03      52.4629      107.062      125.408
1.62E-03      49.8898      104.879      123.812
1.68E-03      47.4698      102.724      122.228
1.74E-03      45.199      100.597      120.656
1.8E-03       43.073      98.499      119.096
1.86E-03      41.087      96.4302     117.549
1.92E-03      39.236      94.3912     116.015
1.98E-03      37.5146     92.3825     114.495
2.04E-03      35.9175     90.4045     112.99
2.1E-03       34.4388     88.4576     111.499
2.16E-03      33.0729     86.5423     110.022
2.22E-03      31.814      84.6588     108.562
2.28E-03      30.6562     82.8076     107.117
2.34E-03      29.5939     80.9888     105.688
2.4E-03       28.6211     79.2029     104.276
2.46E-03      27.7324     77.4499     102.881
2.52E-03      26.9223     75.7302     101.503
2.58E-03      26.1854     74.0439     100.142
2.64E-03      25.5165     72.3912     98.7999
2.7E-03       24.9107     70.7722     97.4758
2.76E-03      24.3632     69.1871     96.1703
2.82E-03      23.8694     67.6359     94.8837
2.88E-03      23.4251     66.1186     93.6163
2.94E-03      23.0261     64.6354     92.3684
3.E-03        22.6685     63.1863     91.1404
3.06E-03      22.3488     61.7711     89.9324
3.12E-03      22.0636     60.3899     88.7449
3.18E-03      21.8096     59.0426     87.5779
3.24E-03      21.5839     57.7291     86.4318
3.3E-03       21.3837     56.4494     85.3069
3.36E-03      21.2066     55.2032     84.2033
3.42E-03      21.0502     53.9905     83.1214
3.48E-03      20.9124     52.811      82.0613
3.54E-03      20.7912     51.6647     81.0233
3.6E-03       20.6848     50.5512     80.0075
3.66E-03      20.5917     49.4704     79.0143
3.72E-03      20.5103     48.4221     78.0437
3.78E-03      20.4392     47.4059     77.0961
3.84E-03      20.3774     46.4218     76.1715

```

3.9E-03	20.3237	45.4693	75.2703
3.96E-03	20.2771	44.5482	74.3924
4.02E-03	20.2368	43.6583	73.5382
4.08E-03	20.202	42.7992	72.7078
4.14E-03	20.172	41.9707	71.9014
4.2E-03	20.1462	41.1725	71.119
4.26E-03	20.124	40.4042	70.3609
4.32E-03	20.105	39.6655	69.6273
4.38E-03	20.0888	38.9562	68.9181
4.44E-03	20.0749	38.2759	68.2336
4.5E-03	20.0631	37.6244	67.574
4.56E-03	20.0531	37.0012	66.9392
4.62E-03	20.0445	36.4062	66.3295
4.68E-03	20.0373	35.839	65.7449
4.74E-03	20.0312	35.2993	65.1856
4.8E-03	20.0261	34.7869	64.6517
4.86E-03	20.0217	34.3014	64.1432
4.92E-03	20.0181	33.8426	63.6602
4.98E-03	20.015	33.4102	63.2029
5.04E-03	20.0125	33.004	62.7713
5.1E-03	20.0103	32.6238	62.3654
5.16E-03	20.0085	32.2692	61.9855
5.22E-03	20.007	31.94	61.6314
5.28E-03	20.0058	31.6362	61.3033
5.34E-03	20.0048	31.3574	61.0013
5.4E-03	20.004	31.1034	60.7254
5.46E-03	20.0033	30.8742	60.4756
5.52E-03	20.0027	30.6695	60.2519
5.58E-03	20.0022	30.4893	60.0545
5.64E-03	20.0019	30.3333	59.8834
5.7E-03	20.0016	30.2015	59.7385
5.76E-03	20.0014	30.0938	59.62
5.82E-03	20.0012	30.0101	59.5277
5.88E-03	20.0011	29.9504	59.4618
5.94E-03	20.001	29.9146	59.4223
6.E-03	20.001	29.9026	59.4091

```

] ;

x=a(:,1);
t10=a(:,2);
t50=a(:,3);
t100=a(:,4);
plot(x,t10,'r-')
plot(x,t50,'g-')
plot(x,t100,'b-')
% plot(x,t1,x,t5,x,t10,x,t20,x,t30,x,t40,x,t50)
xlabel('Distance (m)')
ylabel('Temperature (C)')
legend('Matlab t = 10 s','Matlab t = 50 s','Matlab t = 100 s',...
'Abaqus t = 10 s','Abaqus t = 50 s','Abaqus t = 100 s')
title('Temperature Profile, h_{fs}=3e6')
% axis([ 0 .006 0 6000])

```

APPENDIX H

Function to compute force vector for 1-D melting problem

```

function [f,type] = fMelting(TL,TS,T1,T2,dx,dt,A,hfs,rho)
% local force vector for melting phenomena

% Consider four cases when T1 is always greater than T2
% (dT/dx<0 everywhere)
% Note: TL>TS
% - type 1: T1>=T2, T1 and T2 both <= TS (all solid)
% - type 2: T1>=T2, T1>TS, T1<TL and T2<TS (part solid, part melting)
% - type 3: T1>=T2, T1>TS, T1<TL, T2>TS, T2<TL
% (all melting)
% - type 4: T1>=T2, T1>TL and T2<TS (part liquid,
% part melting, part solid)
% - type 5: T1>=T2, T1>TL, T2>TS, T2<TL (part liquid, part melting)
% - type 6: T1>=T2, T1>TL and T2>TL (all liquid)
% - type 7: T2>T1, T1 and T2 both <= TS (all solid)
% - type 8: T2>T1, T2>TS, T2<TL and T1<TS (part solid, part melting)
% - type 9: T2>T1, T1>TS, T1<TL, T2>TS, T2<TL
% (all melting)
% - type 10: T2>T1, T2>TL and T1<TS (part liquid,
% part melting, part solid)
% - type 11: T2>T1, T2>TL, T1>TS, T1<TL (part liquid, part melting)
% - type 12: T2>T1, T1>TL and T2>TL (all liquid)
%
[T1 T2 TS TL];
if (T1 >= T2) && (T1 <= TS) && (T2 <= TS) % f=[[0;0]
    type=1;
    f=[0;0];
elseif (T1 > TS) && (T1 <= TL) && (T2 <= TS)
    type=2;
    f = [-(hfs*A*dx)*(T1 - TS)*(T1 - 2*T2 + TS)/(2*(T1 - T2)^2);
        -(hfs*A*dx)*(T1 - TS)^2/(2*(T1 - T2)^2)];
elseif (T1 >= T2) && (T1 > TS) && (T1 <= TL) &&...
    (T2 > TS) && (T2 <= TL)
    type=3;
    f = -(hfs*A*dx)/2*[1;1];
elseif (T1 >= T2) && (T1>TL) && (T2<TS)
    type=4;
    f = -[(hfs*A*dx)*(TL - TS)*(TL - 2*T2 + TS)/(2*(T1 - T2)^2);
        (hfs*A*dx)*(TL - TS)*(TL - 2*T1 + TS)/(2*(T1 - T2)^2)];
elseif (T1 >= T2) && (T1 > TL) && (T2 > TS) && (T2 <= TL)
    type=5;
    f = -[(hfs*A*dx)*(T2 - TL)^2/(2*(T1 - T2)^2);
        (hfs*A*dx)*(1/2 - (T1 - TL)^2/(2*(T1 - T2)^2))];
elseif (T1 >= T2) && (T1>TL) && (T2>TL)
    type=6;
    f=[0;0];
elseif (T2 > T1) && (T1 <= TS) && (T2 <= TS)
    type=7;
    f=[0;0];
elseif (T2 > T1) && (T2 > TS) && (T2 <= TL) && (T1 <= TS)
    type=8;
    f = -[(hfs*A*dx)*(T2 - TS)^2/(2*(T1 - T2)^2); ...
        (hfs*A*dx)*(1/2 - (T1 - TS)^2/...
        (2*(T1 - T2)^2))];
elseif (T2 > T1) && (T1 > TS) && (T1 <= TL) &&...
    (T2 > TS) && (T2 <= TL)
    type=9;

```

```

    f = -(hfs*A*dx)/2*[1;1];
elseif (T2 > T1) && (T2 > TL) && (T1 <= TS)
    type=10;
    f = -[-(hfs*A*dx)*(TL - TS)*(TL - 2*T2 + TS)/(2*(T1 - T2)^2);
          (hfs*A*dx)*(TL - TS)*(TL - 2*T1 + TS)/(2*(T1 - T2)^2)];
elseif (T2 > T1) && (T2 > TL) && (T1 > TS) && (T1 <= TL)
    type=11;
    f = -[(hfs*A*dx)*(T1 - TL)*(T1 - 2*T2 + TL)/(2*(T1 - T2)^2);
          (hfs*A*dx)*(T1 - TL)^2/(2*(T1 - T2)^2)];
elseif (T2 > T1) && (T1 > TL) && (T2 > TL)
    type=12;
    f=[0;0];
end

```

APPENDIX I

Function to compute 1-dimensional phase change using variable specific heat

```
function melting
% 1-D conduction with melting
clc; clear all; close all; format compact
set(groot, 'defaulttextinterpreter', 'latex');
set(groot, 'defaultAxesTickLabelInterpreter', 'latex');
set(groot, 'defaultLegendInterpreter', 'latex');
% set constants
T0 = 20; % deg C (initial condition)
k = 0.195; % W/m K
c = 2060; % J/kg K
rho = 1200; % kg/m^3
% melting parameters
TL = 160; % liquidus temperature (C)
TS = 150; % solidus temperature (C)
c_melting=3e6/(TL-TS); % J/kg K (latent heat / temperature range)
%
% mesh and time step parameters
%
% coarse: (OK for temperature distribution)
% Nnode=101; % number of nodes;
% nstep=1000; % number of time steps
%
% fine: (better for melt pool growth)
Nnode=1001; % number of nodes;
nstep=10000; % number of time steps
for coordtype=1:3 % (1- Cartesian, 2-Cylindrical, 3- Spherical)
tic
figure(coordtype)
% calculate element stiffness matrix and assemble global stiff. mat.
if coordtype==1
    T1 = 200; % deg C (left end BC)
    % time step parameters
    tmax=100; % final time (s)
    dt=tmax/nstep; % time step increment (s)
    beta=.5; % set beta (for weighting explicit vs. implicit)
    % geometric parameters
    r = 1e-3; % radius (m)
    A = pi*r^2; % area (m)
    L = 6e-3; % length (m)
    % define mesh
    x1=0; % left node coordinate (m)
    x2=L; % right node coordinate (m)
    dx=L/(Nnode-1);
    x=x1:dx:x2;
    Ke = A*k/dx*[1,-1;-1,1];
    K = zeros(Nnode);
    for i = 1:Nnode-1
        K(i,i) = K(i,i)+ Ke(1,1);
        K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
        K(i,i+1) = Ke(1,2);
        K(i+1,i) = Ke(2,1);
    end
elseif coordtype==2
    T1 = 200; % deg C (left end BC)
    % time step parameters
```

```

tmax=100; % final time (s)
dt=tmax/nstep; % time step increment (s)
beta=.5; % set beta (for weighting explicit vs. implicit)
% geometric parameters
L = 1e-2; % length (m)
% define mesh
x1=L/2; % left node coordinate (m)
x2=L; % right node coordinate (m)
dx=(x2-x1)/(Nnode-1);
x=x1:dx:x2;
K = zeros(Nnode);
for i = 1:Nnode-1
    Ke = 2*pi*k*(x(i)+x(i+1))/(2*dx)*[1,-1;-1,1];
    K(i,i) = K(i,i)+ Ke(1,1);
    K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
    K(i,i+1) = Ke(1,2);
    K(i+1,i) = Ke(2,1);
end
else
T1 = 200; % deg C (left end BC)
% time step parameters
tmax=100; % final time (s)
dt=tmax/nstep; % time step increment (s)
beta=.5; % set beta (for weighting explicit vs. implicit)
% geometric parameters
L = 1e-2; % length (m)
% define mesh
x1=L/2; % left node coordinate (m)
x2=L; % right node coordinate (m)
dx=(x2-x1)/(Nnode-1);
x=x1:dx:x2;
K = zeros(Nnode);
for i = 1:Nnode-1
    Ke=4*pi*k*(x(i)^2+x(i)*x(i+1)+x(i+1)^2)/ ...
        (3*dx)*[1,-1;-1,1];
    K(i,i) = K(i,i)+ Ke(1,1);
    K(i+1,i+1) = K(i+1,i+1) + Ke(2,2);
    K(i,i+1) = Ke(1,2);
    K(i+1,i) = Ke(2,1);
end
end
% iterate for each timestep while adjusting heat capacity
clear T
T=zeros(nstep,Nnode);
T(1,:) = T0*ones(1,Nnode);
tp=zeros(nstep,1);
tp(1)=0;
for time_step=1:tmax/dt % t = dt:dt:tmax
    F = zeros(Nnode,1);
    tp(time_step+1)=tp(time_step)+dt;
    % compute M matrix based on previous step temperature
    M = zeros(Nnode);
    A1 = zeros(Nnode);
    B = zeros(Nnode);
    for i = 1:Nnode-1
        T_previous=(T(time_step,i+1)+T(time_step,i))/2;
        if T_previous<=TS || T_previous>TL
            c_element=c;
        else
            c_element=c_melting;
        end
        if coordtype==1
            m = c_element*rho*A*dx/6 * [2,1;1,2];
        elseif coordtype==2
            r1=x(i);

```



```

        r2=x(i+1);
        m(1,1) = 2*pi*c_element*rho*(r2-r1)*(r1/4+r2/12);
        m(1,2) = 2*pi*c_element*rho*(r2-r1)*(r1/12+r2/12);
        m(2,1) = m(1,2);
        m(2,2) = 2*pi*c_element*rho*(r2-r1)*(r1/12+r2/4);
    else
        r1=x(i);
        r2=x(i+1);
        m(1,1) = 4*pi*c_element*rho*(r2-r1)*(r1^2/5+r1*r2/10+r2^2/30);
        m(1,2) = 4*pi*c_element*rho*(-3*r1^5+5*r1^4*r2-5*r1*r2^4+...
            3*r2^5)/(60*(r2-r1)^2);
        m(2,1) = m(1,2);
        m(2,2) = 4*pi*c_element*rho*(r2-r1)*(r1^2/30+r1*r2/10+r2^2/5);
    end
    M(i,i) = M(i,i)+ m(1,1);
    M(i+1,i+1) = M(i+1,i+1) + m(2,2);
    M(i,i+1) = m(1,2);
    M(i+1,i) = m(2,1);
end
% compute A1 and B matrices
A1 = M/dt + beta*K;
B = M/dt - (1-beta)*K; % same as A1 for Crank-Nicholson
% compute force vector
Fred=zeros(Nnode-1,1);
Fred(1)=Fred(1)+B(2,1)*T1-A1(2,1)*T1;
Fred(2:Nnode-1)=F(3:Nnode);
Alred=A1(2:Nnode,2:Nnode);
Bred=B(2:Nnode,2:Nnode);
Tred_prev=T(time_step,2:Nnode);
Tred=Alred\(Bred * Tred_prev' + Fred);
T(time_step+1,1) = T1;
T(time_step+1,2:Nnode) = Tred;
t_plot=tp(time_step+1);
if abs(t_plot-tmax/10)<dt/10
    t_plot;
    min_T=min(T(time_step+1,:));
    disp(['tplot, min_T= ' num2str([t_plot,min_T])])
    plot(x,T(time_step+1:), 'r*')
    hold on
elseif abs(t_plot-tmax/2)<dt/10
    t_plot;
    min_T=min(T(time_step+1,:));
    disp(['tplot, min_T= ' num2str([t_plot,min_T])])
    plot(x,T(time_step+1:), 'g*')
    hold on
elseif abs(t_plot-tmax)<dt/10
    t_plot;
    min_T=min(T(time_step+1,:));
    disp(['tplot, min_T= ' num2str([t_plot,min_T])])
    plot(x,T(time_step+1:), 'b*')
    hold on
end
end
plot_exact_soln(coordtype,x1)
if coordtype==1
    legend('Matlab t = 10 s', 'Matlab t = 50 s', ...
        'Matlab t = 100 s','Abaqus t = 10 s', ...
        'Abaqus t = 50 s', 'Abaqus t = 100 s')
    title('Cartesian Coordinates')
elseif coordtype==2
    legend('Matlab t = 10 s', 'Matlab t = 50 s', ...
        'Matlab t = 100 s','Abaqus t = 10 s', ...
        'Abaqus t = 50 s', 'Abaqus t = 100 s')
    title('Cylindrical Coordinates')
else

```

```

        legend('Matlab t = 10 s', 'Matlab t = 50 s', 'Matlab t = 100 s')
        % legend('Matlab t = 10 s', 'Matlab t = 50 s', ...
        % 'Matlab t = 100 s', 'Abaqus t = 10 s', ...
        % 'Abaqus t = 50 s', 'Abaqus t = 100 s')
        title('Spherical Coordinates')
    end
    set(groot, 'defaulttextinterpreter', 'latex');
    set(groot, 'defaultAxesTickLabelInterpreter', 'latex');
    set(groot, 'defaultLegendInterpreter', 'latex');
    xlabel('Distance (m)')
    ylabel('Temperature ( $^{\circ}$ C)')
    %
    % plot melt front
    figure(4)
    xm=melt_front(nstep, TS, TL, x, tp, T);
    tm=tp(1:nstep);
    if coordtype==1
        plot(tm, xm, 'r-')
    elseif coordtype==2
        plot(tm, xm, 'g-')
    else
        plot(tm, xm, 'b-')
    end
    hold on

    toc
end
xlabel('time (s)')
ylabel('melt front (m)')
title('Melt Pool Growth')
legend('Cartesian', 'Cylindrical', 'Spherical', 'Location', 'Northwest')
%
% -----
%
function xm=melt_front(nstep, TS, TL, x, tp, T)
%
% tm=zeros(1, nstep);
% xm=zeros(nstep, 1);
for i=1:nstep
    % f=abs((TL+TS)/2-T(i, :));
    % [fmin, imin]=min(f);
    % xm(i)=x(imin)-x(1);
    %
    temps=T(i, :);
    if max(temps)<(TL+TS)/2
        xm(i)=0;
    elseif min(temps)>=(TL+TS)/2
        xm(i)=x(end);
    else
        clear temps2 x2
        % il=find(temps>=((TL+TS)/2)-4.9)&temps<=((TL+TS)/2)+4.9);
        il=find(temps>=(TS+.1)&temps<=(TL-.1));
        il=size(il);
        if il_size(2)==0
            [min_dT, imin]=min(abs(temps-(TS+TL)/2));
            xm(i)=x(imin)-x(1);
            continue
        elseif il_size(2)==1
            xm(i)=x(il)-x(1);
            continue
        end
        temps2=temps(il);
        x2=x(il)-x(1);
        xm(i) =interp1(temps2, x2', (TL+TS)/2);
    end
end
end

```

```

%
% -----
%
function plot_exact_soln(coord_type,x1)
% Plot temperature vs. position
if coord_type==1
    %
    % Cartesian coordinates (LH=3e6) - Table labels:
    %   x, T(10 sec), T(50 sec), T(100 sec)
    %
    a=[ 0.          200.          200.          200.
194.972 60.E-06    184.634    192.964
189.945 120.E-06    169.29     185.931
184.919 180.E-06    153.99     178.903
179.896 240.E-06    148.216    171.882
174.877 300.E-06    142.517    164.871
169.861 360.E-06    136.9      157.872
164.851 420.E-06    131.376    153.013
159.846 480.E-06    125.953    150.054
155.809 540.E-06    120.639    147.548
152.716 600.E-06    115.443    145.047
150.404 660.E-06    110.37     142.553
148.692 720.E-06    105.429    140.067
146.985 780.E-06    100.627    137.592
145.283 840.E-06     95.9677    135.129
143.586 900.E-06     91.4576    132.681
141.894 960.E-06     87.101     130.248
138.532 1.02E-03    82.9018    127.832    140.21
136.861 1.08E-03    78.8631    125.435
135.198 1.14E-03    74.9871    123.058
133.543 1.2E-03     71.2756    120.702
131.896 1.26E-03    67.7295    118.368
130.259 1.32E-03    64.349     116.057
128.632 1.38E-03    61.1336    113.77
127.015 1.44E-03    58.0821    111.508
125.408 1.5E-03     55.1927    109.272
123.812 1.56E-03    52.4629    107.062
122.228 1.62E-03    49.8898    104.879
         1.68E-03    47.4698    102.724
         1.74E-03    45.199     100.597

```

120.656				
	1.8E-03	43.073	98.499	
119.096				
	1.86E-03	41.087	96.4302	
117.549				
	1.92E-03	39.236	94.3912	
116.015				
	1.98E-03	37.5146	92.3825	
114.495				
	2.04E-03	35.9175	90.4045	112.99
	2.1E-03	34.4388	88.4576	
111.499				
	2.16E-03	33.0729	86.5423	
110.022				
	2.22E-03	31.814	84.6588	
108.562				
	2.28E-03	30.6562	82.8076	
107.117				
	2.34E-03	29.5939	80.9888	
105.688				
	2.4E-03	28.6211	79.2029	
104.276				
	2.46E-03	27.7324	77.4499	
102.881				
	2.52E-03	26.9223	75.7302	
101.503				
	2.58E-03	26.1854	74.0439	
100.142				
	2.64E-03	25.5165	72.3912	
98.7999				
	2.7E-03	24.9107	70.7722	
97.4758				
	2.76E-03	24.3632	69.1871	
96.1703				
	2.82E-03	23.8694	67.6359	
94.8837				
	2.88E-03	23.4251	66.1186	
93.6163				
	2.94E-03	23.0261	64.6354	
92.3684				
	3.E-03	22.6685	63.1863	
91.1404				
	3.06E-03	22.3488	61.7711	
89.9324				
	3.12E-03	22.0636	60.3899	
88.7449				
	3.18E-03	21.8096	59.0426	
87.5779				
	3.24E-03	21.5839	57.7291	
86.4318				
	3.3E-03	21.3837	56.4494	
85.3069				
	3.36E-03	21.2066	55.2032	
84.2033				
	3.42E-03	21.0502	53.9905	
83.1214				
	3.48E-03	20.9124	52.811	
82.0613				
	3.54E-03	20.7912	51.6647	
81.0233				
	3.6E-03	20.6848	50.5512	
80.0075				
	3.66E-03	20.5917	49.4704	
79.0143				
	3.72E-03	20.5103	48.4221	
78.0437				
	3.78E-03	20.4392	47.4059	
77.0961				

76.1715	3.84E-03	20.3774	46.4218	
75.2703	3.9E-03	20.3237	45.4693	
74.3924	3.96E-03	20.2771	44.5482	
73.5382	4.02E-03	20.2368	43.6583	
72.7078	4.08E-03	20.202	42.7992	
71.9014	4.14E-03	20.172	41.9707	
71.119	4.2E-03	20.1462	41.1725	
70.3609	4.26E-03	20.124	40.4042	
69.6273	4.32E-03	20.105	39.6655	
68.9181	4.38E-03	20.0888	38.9562	
68.2336	4.44E-03	20.0749	38.2759	
67.574	4.5E-03	20.0631	37.6244	
66.9392	4.56E-03	20.0531	37.0012	
66.3295	4.62E-03	20.0445	36.4062	
65.7449	4.68E-03	20.0373	35.839	
65.1856	4.74E-03	20.0312	35.2993	
64.6517	4.8E-03	20.0261	34.7869	
64.1432	4.86E-03	20.0217	34.3014	
63.6602	4.92E-03	20.0181	33.8426	
63.2029	4.98E-03	20.015	33.4102	
62.7713	5.04E-03	20.0125	33.004	
62.3654	5.1E-03	20.0103	32.6238	
61.9855	5.16E-03	20.0085	32.2692	
61.6314	5.22E-03	20.007	31.94	
61.3033	5.28E-03	20.0058	31.6362	
61.0013	5.34E-03	20.0048	31.3574	
60.7254	5.4E-03	20.004	31.1034	
60.4756	5.46E-03	20.0033	30.8742	
60.2519	5.52E-03	20.0027	30.6695	
60.0545	5.58E-03	20.0022	30.4893	
59.8834	5.64E-03	20.0019	30.3333	
59.7385	5.7E-03	20.0016	30.2015	
59.5277	5.76E-03	20.0014	30.0938	59.62
	5.82E-03	20.0012	30.0101	
	5.88E-03	20.0011	29.9504	

```

59.4618      5.94E-03      20.001      29.9146
59.4223      6.E-03      20.001      29.9026
59.4091 ] ;
%
x=a(:,1);
t10=a(:,2);
t50=a(:,3);
t100=a(:,4);
plot(x+x1,t10,'r-')
plot(x+x1,t50,'g-')
plot(x+x1,t100,'b-')
elseif coordtype==2
%
% Cylindrical coordinates (LH=3e6) - Table labels:
% x, T(10 sec), T(50 sec), T(100 sec)
%
a=[          0.          200.
200.          49.9999E-06      185.98      193.63
195.307      100.E-06      172.111      187.324
190.66      150.E-06      158.404      181.084
186.06      200.E-06      150.558      174.908
181.506      250.E-06      145.385      168.798
176.998      300.E-06      140.286      162.754
172.535      350.E-06      135.267      156.775
168.117      400.E-06      130.334      152.464
163.744      450.E-06      125.492      149.766
159.415      500.E-06      120.748      147.104
155.791      550.E-06      116.106      144.478
152.854      600.E-06      111.572      141.887
150.52      650.E-06      107.15      139.331
148.719      700.E-06      102.844      136.81
146.938      750.E-06      98.6577      134.324
145.176      800.E-06      94.5948      131.872
143.434      850.E-06      90.6577      129.455
141.712      900.E-06      86.8485      127.072
140.009      950.E-06      83.169      124.723
138.327      1.E-03      79.6203      122.408
136.664      1.05E-03      76.2032      120.127
135.021      1.1E-03      72.9179      117.88
133.398      1.15E-03      69.7641      115.667
131.795      1.2E-03      66.7412      113.487

```

130.212				
	1.25E-03	63.8482	111.341	
128.649				
	1.3E-03	61.0837	109.229	
127.107				
	1.35E-03	58.4461	107.15	
125.584				
	1.4E-03	55.9331	105.105	
124.082				
	1.45E-03	53.5426	103.092	
122.601				
	1.5E-03	51.2719	101.113	121.14
	1.55E-03	49.1183	99.1673	
119.699				
	1.6E-03	47.0787	97.2545	
118.279				
	1.65E-03	45.15	95.3748	
116.879				
	1.7E-03	43.3289	93.528	115.5
	1.75E-03	41.6118	91.7141	
114.142				
	1.8E-03	39.9954	89.933	
112.804				
	1.85E-03	38.476	88.1846	
111.488				
	1.9E-03	37.0498	86.4689	
110.192				
	1.95E-03	35.7131	84.7857	
108.917				
	2.E-03	34.4623	83.135	
107.663				
	2.05E-03	33.2935	81.5166	
106.431				
	2.1E-03	32.203	79.9305	
105.219				
	2.15E-03	31.1871	78.3765	
104.028				
	2.2E-03	30.2421	76.8546	
102.859				
	2.25E-03	29.3644	75.3645	
101.711				
	2.3E-03	28.5504	73.9063	
100.584				
	2.35E-03	27.7967	72.4797	
99.4777				
	2.4E-03	27.0998	71.0846	
98.3931				
	2.45E-03	26.4565	69.7209	
97.3298				
	2.5E-03	25.8634	68.3884	
96.2877				
	2.55E-03	25.3176	67.087	
95.267				
	2.6E-03	24.816	65.8165	
94.2675				
	2.65E-03	24.3558	64.5768	
93.2894				
	2.7E-03	23.9341	63.3677	
92.3326				
	2.75E-03	23.5484	62.1889	
91.3972				
	2.8E-03	23.1961	61.0404	
90.4831				
	2.85E-03	22.8748	59.922	
89.5903				
	2.9E-03	22.5822	58.8334	
88.7188				
	2.95E-03	22.3161	57.7745	

87.8687			
87.0398	3.E-03	22.0746	56.7451
86.2323	3.05E-03	21.8557	55.7449
85.446	3.1E-03	21.6576	54.7739
84.6811	3.15E-03	21.4785	53.8317
83.9373	3.2E-03	21.317	52.9183
83.2148	3.25E-03	21.1715	52.0333
82.5135	3.3E-03	21.0405	51.1765
81.8334	3.35E-03	20.923	50.3479
81.1744	3.4E-03	20.8175	49.5471
80.5365	3.45E-03	20.7231	48.7739
79.9197	3.5E-03	20.6387	48.0282
79.324	3.55E-03	20.5633	47.3097
78.7492	3.6E-03	20.4962	46.6182
78.1955	3.65E-03	20.4364	45.9536
77.6627	3.7E-03	20.3833	45.3155
77.1507	3.75E-03	20.3362	44.7038
76.6597	3.8E-03	20.2945	44.1183
76.1894	3.85E-03	20.2575	43.5588
75.7398	3.9E-03	20.225	43.0251
75.311	3.95E-03	20.1962	42.5169
74.9028	4.E-03	20.1709	42.0342
74.5152	4.05E-03	20.1487	41.5766
74.1481	4.1E-03	20.1292	41.144
73.8015	4.15E-03	20.1122	40.7363
73.4753	4.2E-03	20.0973	40.3531
73.1694	4.25E-03	20.0843	39.9944
72.8839	4.3E-03	20.073	39.66
72.6185	4.35E-03	20.0631	39.3497
72.3733	4.4E-03	20.0547	39.0633
72.1482	4.45E-03	20.0473	38.8006
71.9431	4.5E-03	20.0411	38.5615
71.7579	4.55E-03	20.0357	38.3459
71.5925	4.6E-03	20.0312	38.1536
	4.65E-03	20.0273	37.9844


```

71.447      4.7E-03      20.0242      37.8381
71.3211    4.75E-03    20.0216    37.7148
71.2148    4.8E-03      20.0196    37.6141
71.1281    4.85E-03    20.018     37.536
71.0607    4.9E-03      20.017     37.4804
71.0128    4.95E-03    20.0163    37.4472
70.9841    5.E-03      20.0161    37.4361
70.9745];
    x=a(:,1);
    t10=a(:,2);
    t50=a(:,3);
    t100=a(:,4);
    plot(x+x1,t10,'r-')
    plot(x+x1,t50,'g-')
    plot(x+x1,t100,'b-')
else
    %
    % Spherical coordinates (LH=3e6) - Table labels:
    %   x, T(10 sec), T(50 sec), T(100 sec)
    %
    a=[
200.          0.          200.
    49.9999E-06      185.576      192.892
194.635      100.E-06      171.448      185.925
189.376      150.E-06      157.623      179.096
184.219      200.E-06      150.16      172.402
179.164      250.E-06      144.348      165.841
174.207      300.E-06      138.664      159.411
169.346      350.E-06      133.115      154.286
164.579      400.E-06      127.706      150.294
159.904      450.E-06      122.441      147.047
155.916      500.E-06      117.325      143.864
152.645      550.E-06      112.362      140.744
150.021      600.E-06      107.555      137.686
147.604      650.E-06      102.906      134.69
145.231      700.E-06      98.4162      131.754
142.903      750.E-06      94.0876      128.877
140.618      800.E-06      89.9202      126.059
138.376      850.E-06      85.9137      123.299
136.177      900.E-06      82.0674      120.596
134.02      950.E-06      78.38      117.949
131.905

```

129.831	1.E-03	74.8497	115.358	
	1.05E-03	71.4745	112.821	
127.797	1.1E-03	68.2518	110.339	
125.804	1.15E-03	65.179	107.909	123.85
	1.2E-03	62.2528	105.533	
121.936	1.25E-03	59.47	103.208	120.06
	1.3E-03	56.8272	100.935	
118.223	1.35E-03	54.3206	98.7117	
116.423	1.4E-03	51.9465	96.5386	114.66
	1.45E-03	49.7008	94.4146	
112.934	1.5E-03	47.5796	92.3392	
111.243	1.55E-03	45.5786	90.3115	
109.588	1.6E-03	43.6937	88.331	
107.969	1.65E-03	41.9206	86.3969	
106.383	1.7E-03	40.255	84.5086	
104.832	1.75E-03	38.6925	82.6654	
103.314	1.8E-03	37.2288	80.8667	
101.829	1.85E-03	35.8597	79.1118	
100.377	1.9E-03	34.5808	77.4	
98.9574	1.95E-03	33.388	75.7307	
97.5691	2.E-03	32.2769	74.1032	
96.2122	2.05E-03	31.2435	72.517	
94.8861	2.1E-03	30.2837	70.9713	
93.5905	2.15E-03	29.3937	69.4657	
92.3249	2.2E-03	28.5694	67.9993	
91.0891	2.25E-03	27.8073	66.5717	
89.8825	2.3E-03	27.1035	65.1822	
88.7049	2.35E-03	26.4547	63.8303	
87.5559	2.4E-03	25.8574	62.5153	
86.4351	2.45E-03	25.3082	61.2366	
85.3422	2.5E-03	24.8042	59.9938	
84.2768	2.55E-03	24.3421	58.7861	
83.2387	2.6E-03	23.9193	57.6132	
82.2274	2.65E-03	23.5329	56.4744	
81.2428	2.7E-03	23.1802	55.3691	
80.2844	2.75E-03	22.8589	54.2969	

79.352			
78.4452	2.8E-03	22.5666	53.2572
77.5639	2.85E-03	22.301	52.2495
76.7076	2.9E-03	22.0602	51.2733
75.8762	2.95E-03	21.842	50.3281
75.0693	3.E-03	21.6446	49.4133
74.2867	3.05E-03	21.4664	48.5286
73.5281	3.1E-03	21.3057	47.6734
72.7932	3.15E-03	21.161	46.8473
72.0819	3.2E-03	21.031	46.0497
71.3937	3.25E-03	20.9142	45.2803
70.7286	3.3E-03	20.8096	44.5386
70.0863	3.35E-03	20.7159	43.8242
69.4664	3.4E-03	20.6322	43.1365
68.8688	3.45E-03	20.5575	42.4753
68.2933	3.5E-03	20.4909	41.84
67.7396	3.55E-03	20.4317	41.2304
67.2074	3.6E-03	20.3791	40.6459
66.6967	3.65E-03	20.3325	40.0862
66.2071	3.7E-03	20.2912	39.5509
65.7384	3.75E-03	20.2546	39.0397
65.2905	3.8E-03	20.2224	38.5521
64.863	3.85E-03	20.194	38.0878
64.4559	3.9E-03	20.1689	37.6465
64.0689	3.95E-03	20.1469	37.2278
63.7018	4.E-03	20.1277	36.8314
63.3543	4.05E-03	20.1108	36.4569
63.0264	4.1E-03	20.096	36.1041
62.7178	4.15E-03	20.0831	35.7726
62.4283	4.2E-03	20.0718	35.4622
62.1578	4.25E-03	20.0621	35.1724
61.9059	4.3E-03	20.0536	34.9032
61.6727	4.35E-03	20.0463	34.6541
61.4578	4.4E-03	20.0399	34.4249
	4.45E-03	20.0345	34.2154

61.2611	4.5E-03	20.0299	34.0252
61.0824	4.55E-03	20.0259	33.8542
60.9215	4.6E-03	20.0226	33.7021
60.7783	4.65E-03	20.0198	33.5687
60.6526	4.7E-03	20.0174	33.4537
60.5442	4.75E-03	20.0156	33.357
60.4529	4.8E-03	20.0141	33.2782
60.3786	4.85E-03	20.013	33.2174
60.3211	4.9E-03	20.0122	33.1741
60.2803	4.95E-03	20.0117	33.1483
60.2559	5.E-03	20.0116	33.1397

```

60.2478 ];
      x=a(:,1);
      t10=a(:,2);
      t50=a(:,3);
      t100=a(:,4);
      plot(x+x1,t10,'r-')
      plot(x+x1,t50,'g-')
      plot(x+x1,t100,'b-')
end

```

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